

Teaser documents for the proposed power plant in UAE

| Heads | Details |
|---|---|
| Land Area required in sq mtr. As per law of land build up area is 60% of the total area | [B] |
| Expected Land Rent to be paid to the government | [C] |
| Desired Land Levelling (As it will be sand) | [B] |
| Estimated Distance desirable between the land and the sea shore | [B] |
| Estimated Distance desirable between the land and the power grid | [B] |
| Power & Water requirement during the construction phase | [B] |
| Draught of the Sea | [B] |
| Proposed Movement of Fuel from Sea to Plant | [B] |
| | |
| Nature of Fuel | LNG |
| Source of Fuel | QATAR or OMAN |
| Transportation of Fuel | [B] SHIP |
| | |
| Brief Configuration of the Power plant | Appendix A |
| Brief Configuration of the Cooling Tower | Appendix A |
| Brief configuration of the Desalination Plant | Appendix C |
| Envisaged Output of the Power Plant | [C] |
| Total estimated Capital Cost of the power project | [C] |
| Total estimated Operational Cost of the power project | Appendix D |
| Approximate Cost of Production of Power | Appendix D |
| | |
| Brief Background of the Promoters or Consortium | [A] |
| Brief Background of the Technology Supplier | Appendix A, C |
| Brief Background of the Equipment Supplier | Appendix A |
| Source of Fund CAPEX & OPEX for the project | Appendix D |
| Background reference of the operational power plants in the other parts of the world | Appendix A |
| | |
| PPA Agreement at what rate is expected from the government | Appendix D |
| | |
| Release of the produced power will be for grid completely or also to sale to end users | Optional |
| | |
| Expected Man Power required for EPC & running the power plant | ALNG storage & Regas; Pipeline(s); Power Plant; LT-MED plant --<100 |
| | |
| Waste & Effluent Disposal arrangements and treatment | In accordance with local regulations |

INFORMATION MEMORANDUM:

PROPOSED UAE RLNG CCGT POWER SYSTEM -- ENERGY GIANT HKSAR LLC

PROPOSER: [A]

Energy Giant LLC HKSAR acts as a system integrator that:

- (1) integrates best-of-breed technologies which it funds through Special Purpose Vehicles to beneficiate high value products from local resources [such as in India & Mozambique]; and
 - (2) develops and funds high-reliability power generation projects for ‘green fields’ locations at the best possible cost efficiency.
- EG is working with EMEM Mozambique to build a coal-to-diesel and agro-chemical Program in northern MZQ: \$4.5 billion
 - EG is working with Indian Oil Corp. Ltd. to build a coal-to-diesel and agro-chemical Program at three India ports [Hazira, Ennore, and Kirtania Subarnarekha]: \$4.5 billion.
 - EG is working with Indian Oil Corp. Ltd. and PetroBangla to build a 2,500 mmscfd LNG storage and regas facility [using CDTS tanks] on the mouth of the Subarnarekha River at the India Bay of Bengal coast that will pipe gas to West Bengal and eastern Bangladesh markets for the first time: \$3.9 billion.

EG has organized a specialized aero derivative EPC in Morocco to ‘de-conflict’ all CCGT projects in ‘green fields’ markets. All personnel are trained and certified by Siemens in the installation, operation, and maintenance of Siemens/ Rolls-Royce SGT A65 aeroderivative gas turbines and assorted support sub-system described herein.

Many emerging markets have been approached to build over-sized gas turbine power plants where there is no supporting industrial infrastructure for handling, operations or repair. In addition, some emerging markets have no gas grids. EG’s solution is to derive a modular and scalable CCGT configuration with its proprietary ‘flow acceleration’ heat exchanger with a competitive heat rate.

- EG is working with Bright Trade to build out a 2,000 MW CCGT-based power system for the government on the Mediterranean coast of Syria.
- EG is working with the Myanmar government to build out a 3 berth site at Dala port on the Yangon River to receive and regas LNG that will feed three 386MW CCGT systems situated across the river in the MPE refinery premises at Thanlyin to send power to Hlaingeharyar Grid.
- EG is working with the Government of Bangladesh for the distribution of 386 MW CCGT power generation stations along the new gas pipeline to be built in eastern Bangladesh.

A. Land area we will require for all Power Plant sub-systems and in what condition: [B]

CCGT Power Plant:

We propose a 386 MW-rated 3 on 1 SGT A65 Wet Low Emissions (WLE - The injection of water reduces emissions and boosts performance); Inlet Spray Inter-cooling (ISI reduces ambient inlet temperature and decreases the energy required for compression) and 3 on 1 Pressured Fired configuration. Our proposed proprietary ‘flow acceleration heat exchanger’ will increase output of the 386 MW.

Attached please find Appendix A. “SGT A65 CCGT Reference Layout with Horizontal-HRSG”. On page one you will note:

Projected Width: 459 ft.

INFORMATION MEMORANDUM:

PROPOSED UAE RLNG CCGT POWER SYSTEM -- ENERGY GIANT HKSAR LLC

Projected Length: 388 ft.
Total Area: 178,092 ft²
In square meters: 16,545.29 m²

Projected Result / MW Configuration: 17,100 m²

[3] Gas Turbine Package Weight: 238,600 kg

[1] Overall Steam Turbine &
Generator Weight: 396,050 kg

We will build an entire floor for the full layout from reinforced concrete capable of sustaining both equipment weights and all the necessary servicing vehicles.

We will implement additional 3 on 1 CCGT systems as power requirements expand.

LNG Storage and Regasification:

In our work with Indian Oil on the 2,500 mmscfd LNG storage and regasification facility at “LNG Kirtania”, we expect IOCL to obtain an mmBTU of LNG at about 12.5% of the price of a barrel of Brent Crude, plus about \$25 per ton for freight from Qatar / Singapore to India. This LNG will be stored in sixteen CDTS 40,000 m³ LNG storage modules until regasified. The RLNG will be piped to West Bengal Indian markets, and markets in Bangladesh.

The UAE project will procure LNG from Oman or Qatar – which is virtually next door. However, we will have to receive, store, then regasify the LNG for CCGT use. Our 386 MW 3-on-1 CCGT will require about 42.21 mt of LNG per hour or about 24,652 mt of LNG for 80% availability over 1 month of CCGT Operation.

As in India, we will utilize a Cubic Donut Tanking Modular Storage System (CDTS of Altair Engineering) – two 40,000 m³ tanks, constructed from 9% Ni Steel. We have standardized on the 40,000 m³ module, and are building the units off-shore for welding and assembly on site. This allows us to obtain safe LNG storage within the CCGT system construction time frame. Attached please find Appendix B. “31Aug2018_AltairCDTS_Solution_Land Storage”.

Two 40,000 m³ tanks will require 140.5 X 232 = 32,596 m³

Optimal risk factored design of LNG Tank Farm layout by China Petroleum University, the required land for the CDTS modules is 67% of the land use required for conventional circular concrete full containment tanks of similar capacity.

Our Indian LNG storage facility, at LNG Kirtania, working with Indian Oil Corp. Ltd., **obtained approval** from the Indian Ministry of Petroleum and Natural Gas- Oil Industry Safety Directorate [“OSID”], for this modular, single containment tank because the OISD-194 section 6.1.3 covering double integrity is fully covered by Altair’s CDTS design.

Low-draught [6-8 meters] 22,000 mt LNG carriers will make deliveries about every three weeks for the two CDTS tanks to off-take and store. Best case is to co-locate the CDTS tank facility at a deep-water port. However, if necessary a dolphin can be anchored at sufficient sea depth so a 6-8 m draught 22,000 mt LNG carrier can connect and pipe LNG to the CDTS tanks close by on the beach.

Although a 386 MW 3 to 1 CCGT system burns about 49.34mmscfd -- to achieve operational simplicity expanding power capacity, a single 1100 kW Wartsila 250mmscfd regas train will be

INFORMATION MEMORANDUM:

PROPOSED UAE RLNG CCGT POWER SYSTEM -- ENERGY GIANT HKSAR LLC

deployed. The train weighs about 175 mt. *Its dimensions: 26 m long X 14.5 m wide X 8 m high. The train is placed on a 4,000 m³ tract, reinforced to bear 175mt, at sufficient distance (>100 meters) from the CDTS tanks & CCGT power system to satisfy local safety regulations.*

It is more economical & timely to ramp up additional CDTS tanks to feed additional CCGT power systems – five of which can be supplied with RLNG via one 250mmscfd regas train.

Fog technology inlet cooling increases output by up to 20%, improves heat rate up to 5%. Substantial water [28 gal./minute per inlet fogging sub-system] must be demineralized [less than 5 parts per million of Total Dissolved Solids]. The proposed three SGT A65 GT inlet fogging systems utilize 120,960 gallons [458 cubic meters] per day to keep inlet air temperate in 35° C high humidity weather prevalent at UAE beaches. The three wet compression combustion systems can evaporate 70 gallons per minute each [0.798 cubic meters/minute, 1,149 m³ per day].

We use Low-Temperature Multi-Effect Distillation [MED] to desalinate seawater because the primary energy required is free: A 386 MW 3 to 1 CCGT system generates greater than 400° C. exhaust heat, far more than the 70° C. a MED unit's 'effects' use to generate 100,000 m³ /day of water with 5 ppm TDS [parts per million of Total Dissolved Solids]. Note: The 'fresh' water consumed by humans is ~1,000 ppm TDS. An LT-MED system makes guaranteed Boiler Feed Water at <5ppm TDS for ~\$0.13 /m³. *An LT-MED system requires 25 acres [100,000 m²] at the shore.*

Indicative Budget [c]

| | |
|--|---------------|
| LNG Storage and Re-gas plant | \$ 78,444,215 |
| If Dolphin Required vice existing Port | \$ 25,000,000 |
| 386 MW CCGT with flow acceleration | \$309,994,347 |
| 25,000 m ³ /day LT-MED System | \$ 27,500,000 |
| Land @ \$13 per m ² [153,696 m ²] | \$ 1,998,048 |

Each additional 386 MW CCGT Capacity Expansion

| | |
|---|---------------|
| LNG Storage Expansion | \$ 51,400,000 |
| CCGT with Flow Acceleration | \$297,750,000 |
| Land [49,696 m ²] @ \$13/m ² | \$ 646,048 |



Appendix A.

Resilient Power Plants

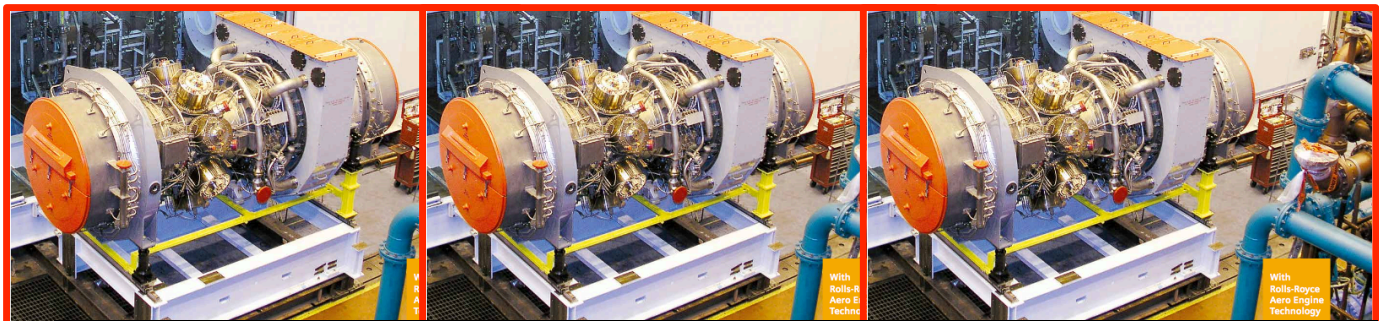
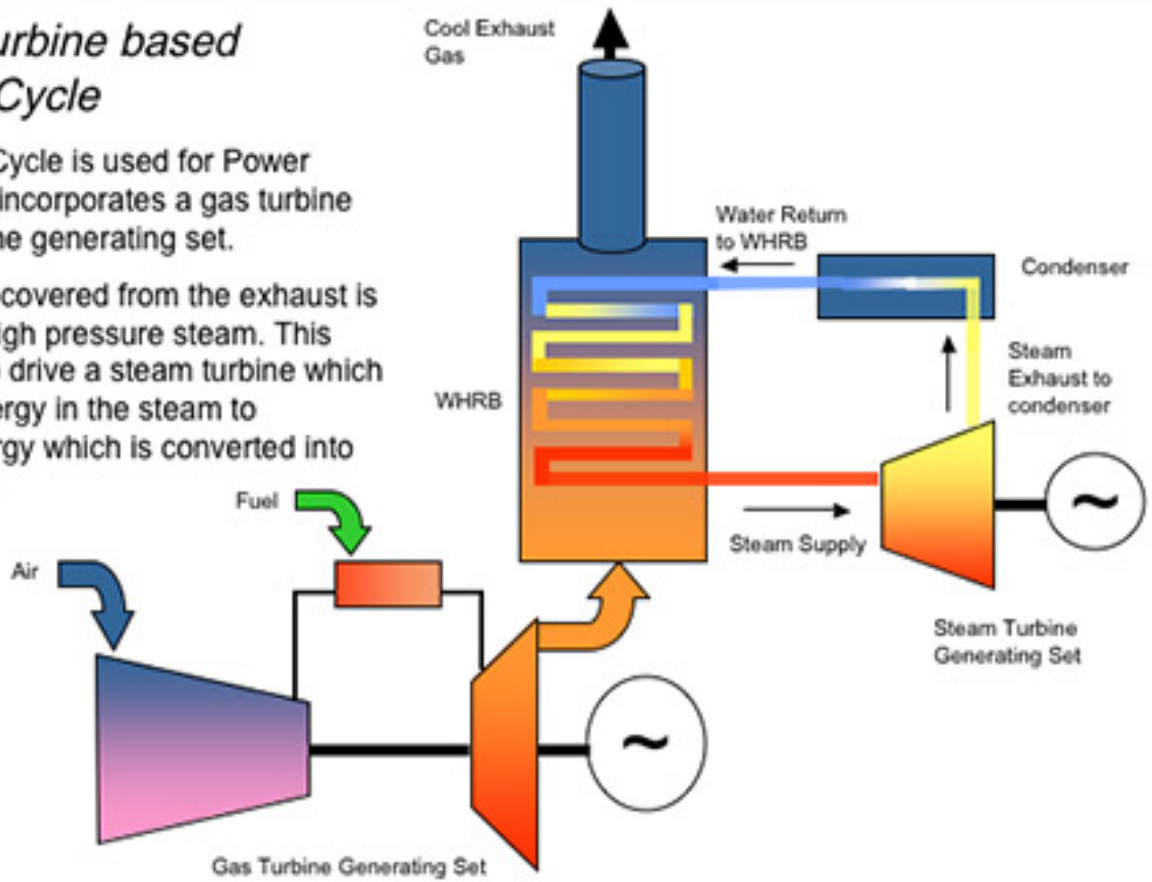
Custom-Tailored Power Solution

- We are developing a versatile engineering capability in Morocco to purchase, integrate, install, and operate modular power plants
- These modular power plants will be standardized on the Siemens 321.9 MW *SGT A65 WLE ISI 3 on 1 One Pressure Fired* combined cycle system
- We will purchase standardized 321.9 MW power modules based on the *SGT A65 WLE ISI* from Siemens, implement them in Morocco, then pack them up and ship them to our developing country client sites where we will install, operate and maintain them.
- As the power requirements inevitably expand, we will continue to purchase and implement additional Siemens 321.9 MW power modules at our developing country client sites.
- All power plants will be configured similarly to assure singular expertise, availability of spares and parts, and the highest efficiency of operation.
- All 321.9 MW power modules can be trucked into the interior of a developing country client from the port of access. Right-sized component handling equipment will be a standard feature of each configuration. We will bring everything with us that we will need to build, operate, and maintain our power plant modules.
- We will supply all funding, and will contract for a service charge per kWh of electricity generated. The natural gas fuel will remain the responsibility of the power purchasing utility.

The Gas Turbine based Combined Cycle

The Combined Cycle is used for Power Generation and incorporates a gas turbine and steam turbine generating set.

All of the heat recovered from the exhaust is converted into high pressure steam. This steam is used to drive a steam turbine which converts the energy in the steam to mechanical energy which is converted into electrical power.



2. Site Specific Gas Turbine Performance Data (per unit)

| | | |
|---|----------|----------|
| Generator Output | 66002 | kW |
| LHV Heat Rate @ Generator Terminals | 8661 | kJ/kWh |
| LHV Efficiency @ Generator Terminals | 41.57 | % |
| Compressor Inlet Airflow | 170.2 | kg/s |
| Exhaust Temperature | 422.6 | C |
| Site Performance Data Computed Burning | Gas Fuel | |
| Site Performance Data Computed with Inlet Loss | 7.938 | millibar |
| Site Performance Data Computed with Exhaust Loss | 21.97 | millibar |
| Site Performance Data Computed with Water Injection | 4.016 | kg/s |

High power and efficiency: Due to an independent 3 shaft design, this turbine is flexible, offering high power out and fuel efficiency with minimal drop-off at reduced speed conditions

For power generation: One of the most efficient gas turbines on the market, the SGT-A65 provides up to 71 MW in simple cycle service at 43.8% efficiency

Modular design for quick installation and easy on-site maintenance: The SGT-A65 consists of 8 engine modules for easy maintenance. Each module is pre-balanced to make it completely interchangeable.

What's the value of an Aero ?

| | | |
|--|---|--|
| High Simple Cycle Efficiency Typically 3~5%pts better than Industrials High pressure ratio EQUALS high fuel efficiency (downside; requires a higher skid edge fuel pressure). | High Power Density Typically 30% size and 50% weight reduction Extensive application of Titanium and high Nickel alloys, which reduces weight. | High Cycle Capability No penalty for starting and stopping Hollow shafts eliminate rotor bow and high Nickel casings eliminate stress. |
| Fast First & Restart Capability 5' ~ 8' starts and with NO lockout timers after a shutdown Combined benefit of Nickel alloys and design. | Low Black start requirement <500kW electrical start-up equates to smaller site back-up generation Multi-shaft core requires starting only on the smallest, lightest rotor. | High Grid Frequency Change Lightweight rotors allows to respond quickly Nickel alloys and hollow design allow rapid rate of change. |
| Experience – mission critical Customers demand operational experience – aero hours prove technology when applied to industrial applications FAA approval and flight hours creates natural experience list. | “NO” EOH Material within an aero GT capable of more extreme operating conditions which leads to longer life and lower OPEX cost Combined benefit of Nickel alloys and design. | Bearings Anti-friction bearings require less lubrication which reduces OPEX Ball bearing design is lightweight and low oil flow / consumption. |

A SGT-A65 is

- Direct derivative of the aero Trent 800 engine, because
- Proven technology.
- Low cost solution.
- 3 shaft gas turbine (HP, IP & LP) – see next slide.
 - Each shaft rotating independently of each other.
 - Excellent future growth.
- 36:1 Rp gas turbine (50Hz).
- Environmentally friendly, having both DLE & WLE options.
- Hot end drive machine.
- **NO** gearbox required for both 50Hz & 60Hz applications.
- Normal start capability; <7mins, from cold metal to full load on either GAS or LIQUID fuel; Ramp rates of 21~40MW/min.
- High cycling capability, w/limited maintenance cost impact, **NO** EOH, immediate restarting and **NO** lockout period.

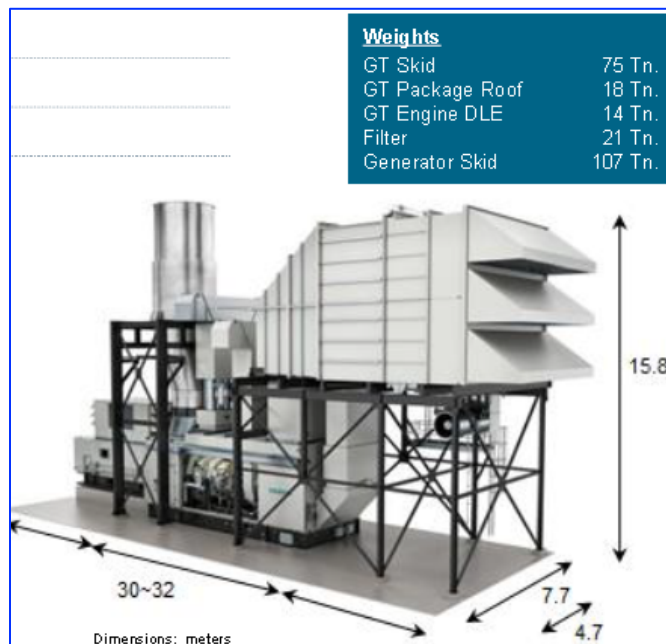
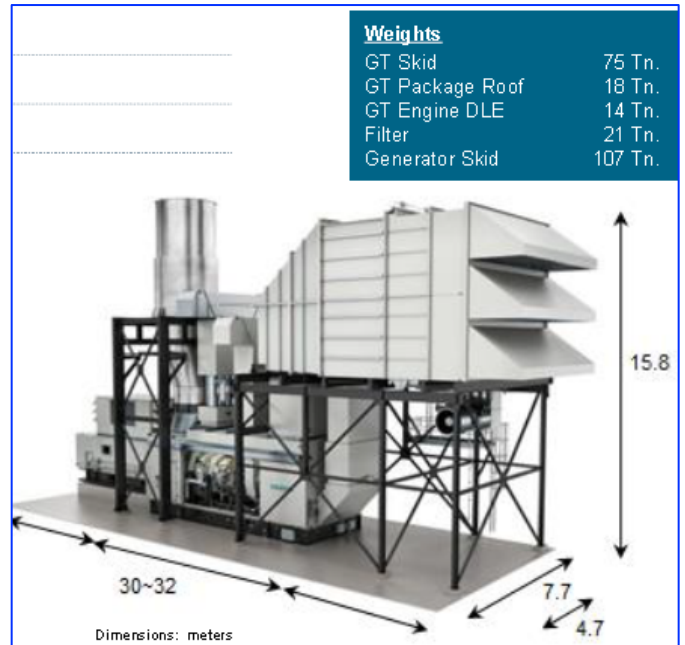
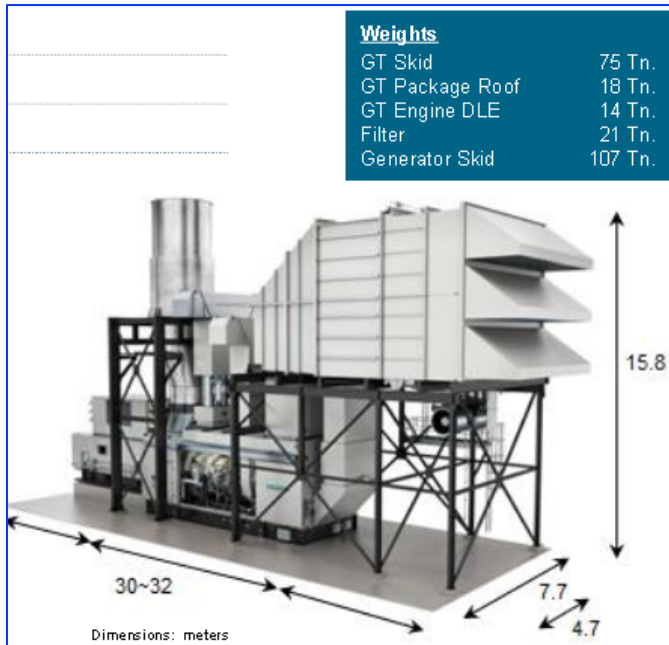
Power Output Analysis of SGT A65 WLE ISI 3 on 1 One Pressure Fired CCGT System

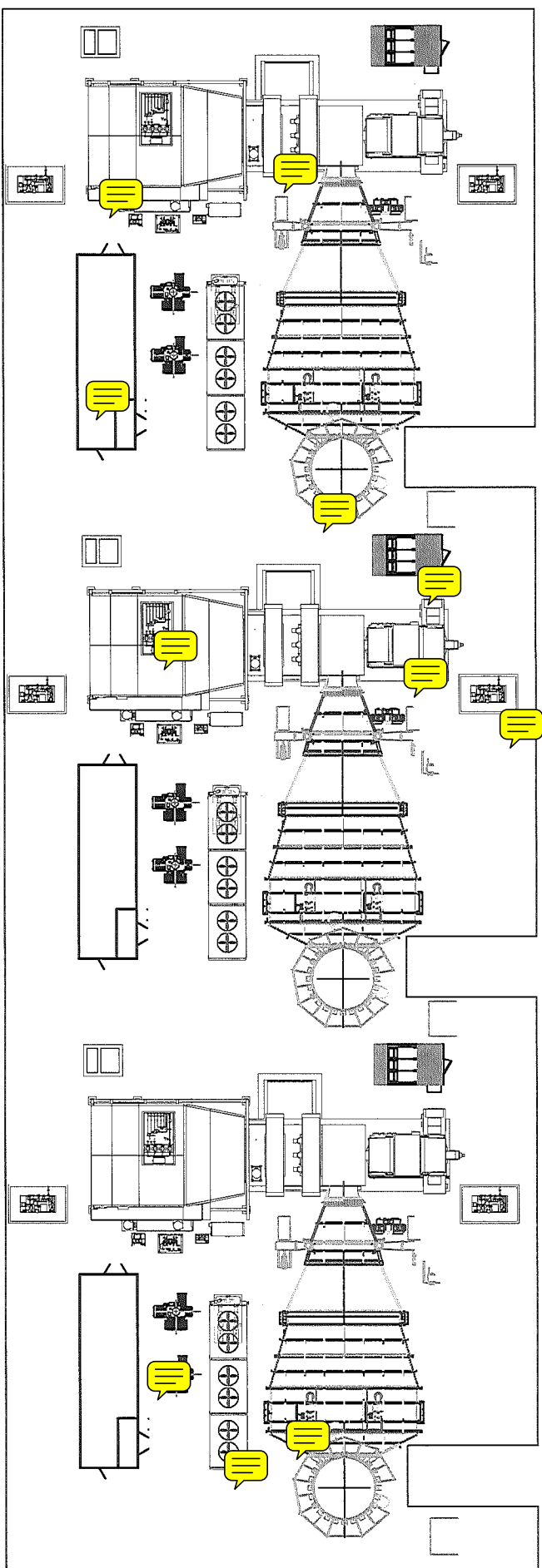
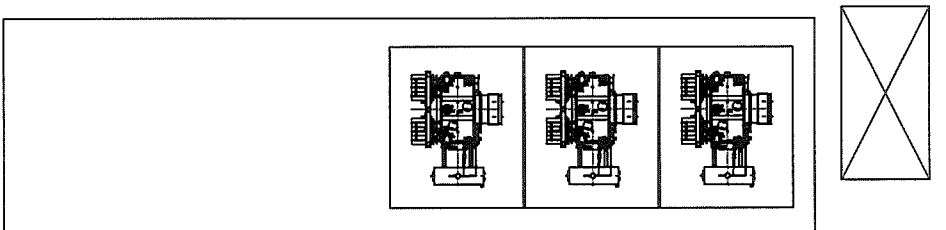
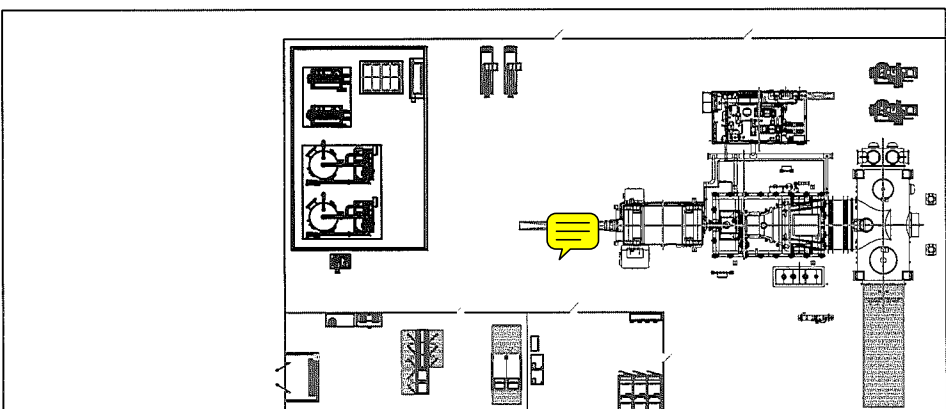
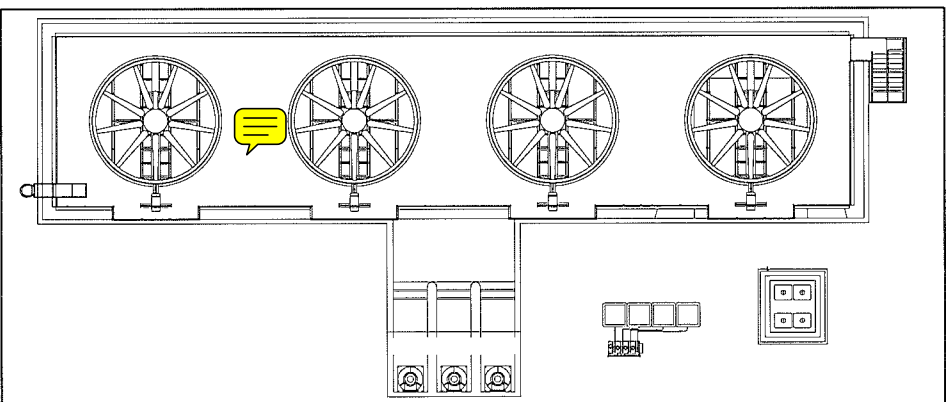
SGT A65 WLE ISI No. 1
 SGT A65 WLE ISI No. 2
 SGT A65 WLE ISI No. 3
 Steam Turbine
Total Output

Generator Output

66,002 kiloWATTs
 66,002 kiloWATTs
 66,002 kiloWATTs
 123,894 kiloWATTs

321,900 KiloWATTs



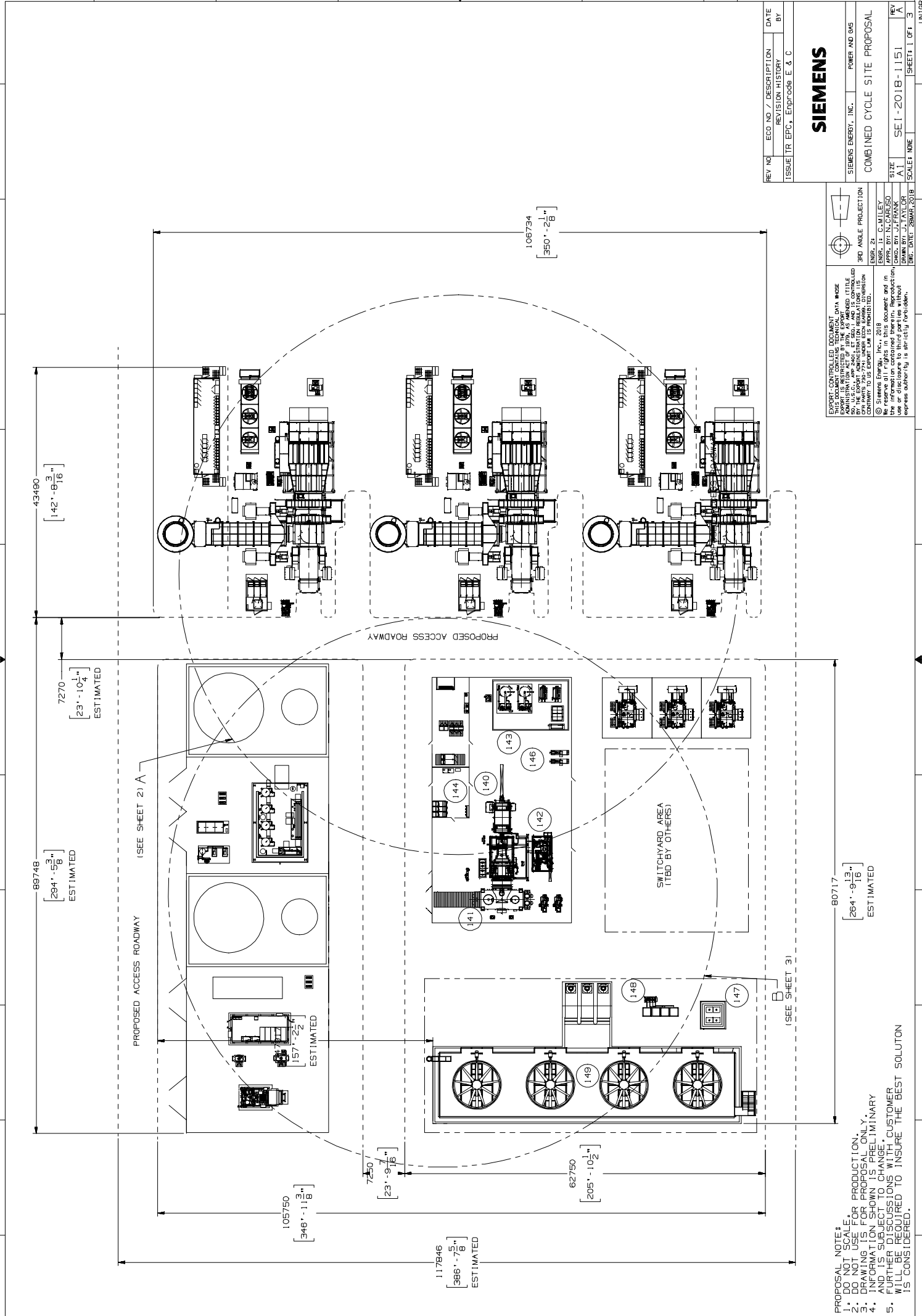


| REV NO | ECO NO / DESCRIPTION | DATE |
|--------|-------------------------------|------|
| 1 | ISSUE TR EPC, Enbridge E. & C | |

| SIEMENS ENERGY, INC. | POWER AND GAS |
|-------------------------------------|---------------|
| COMBINED CYCLE SITE PROPOSAL | |
| SIZE: A1 | REV: A |
| SCALE: NONE | SHEET: 1 OF 3 |

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ENGR. BY: N. CARLISO
 CHECKED BY: J. FRANK
 DRAWN BY: J. TAYLOR
 DATE: 02/28/2018



89748
 [294' - 5 3/8"]
 ESTIMATED

105750
 [346' - 11 3/8"]

117846
 [386' - 7 5/8"]
 ESTIMATED

62750
 [205' - 10 1/2"]

7250
 [23' - 9 7/16"]

7270
 [23' - 10 1/4"]
 ESTIMATED

43490
 [142' - 8 3/16"]

106734
 [350' - 2 1/8"]

80717
 [264' - 9 13/16"]
 ESTIMATED

(SEE SHEET 21) A

(SEE SHEET 31)

SWITCHYARD AREA
 (1160 BY OTHERS)

PROPOSED ACCESS ROADWAY

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 2. DO NOT USE FOR PRODUCTION.
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 4. INFORMATION SHOWN IS PRELIMINARY
 5. FURTHER DISCUSSIONS WITH CUSTOMER
 IS REQUIRED TO INSURE THE BEST SOLUTION
 IS CONSIDERED.

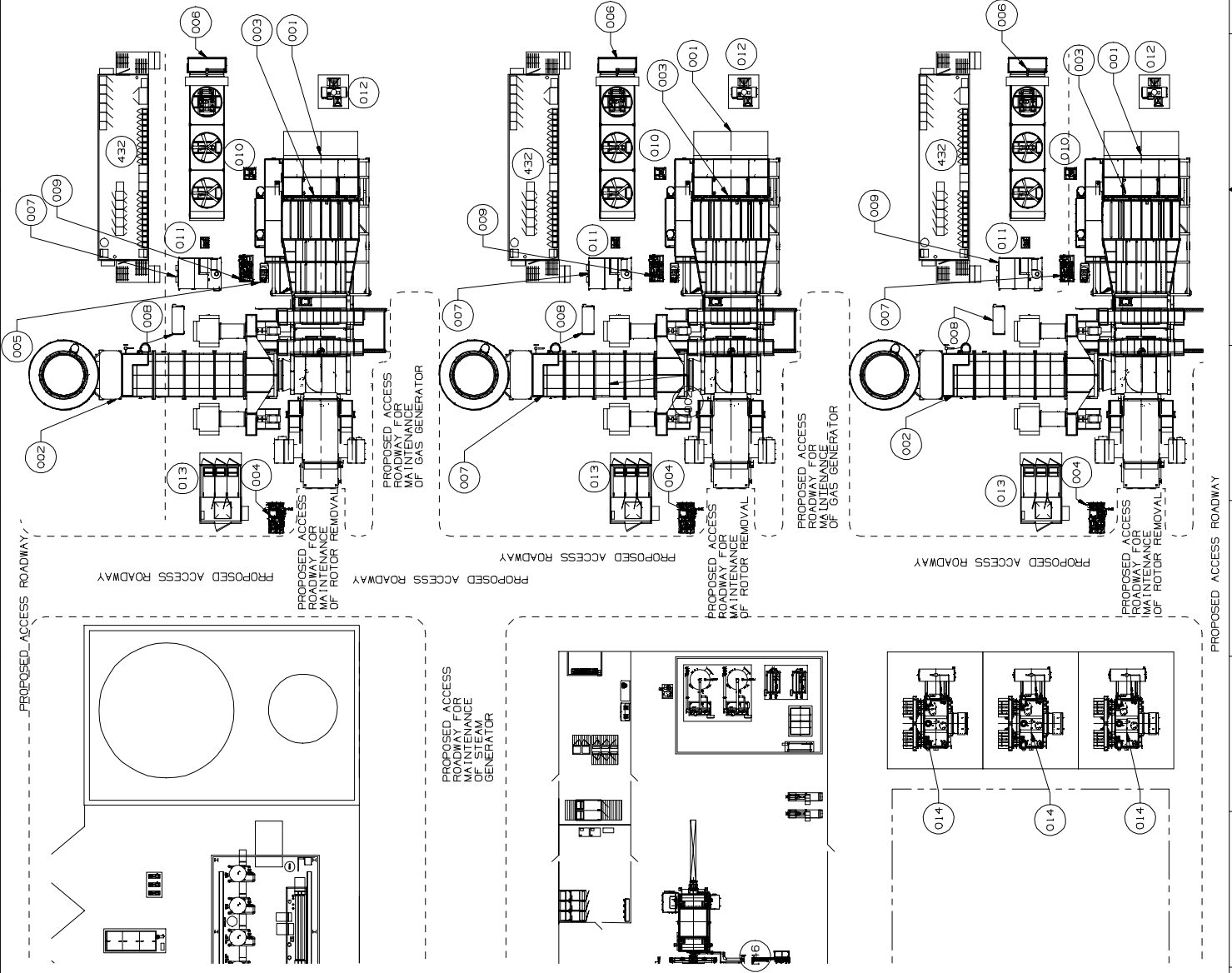
EQUIPMENT LIST MAJOR COMPONENTS

| PINS | DESCRIPTION | QTY | NOTES |
|------|--|-----|----------------------|
| 001 | GAS TURBINE GENERATOR | 3 | |
| 002 | HRSG HEAT RECOVERY STEAM GENERATOR VERTICAL | 3 | |
| 003 | ISI AUXILIARY SKID | 3 | |
| 004 | MINERAL LUBE OIL SKID | 3 | |
| 005 | MOBILE WATER WASH | 2 | SHARED BETWEEN UNITS |
| 006 | FIN FAN COOLING SKID | 3 | |
| 007 | WATER INJECTION SKID | 3 | |
| 008 | GT CO2 FIRE PROTECTION SYSTEM | 3 | |
| 009 | LIQUID FUEL FORWARDING PUMP | 3 | |
| 010 | FUEL FILTER SKID | 3 | |
| 011 | DEMINERALIZED WATER FILTER SKID | 3 | |
| 012 | AUXILIARY TRANSFORMER | 3 | |
| 013 | CIRCUIT BREAKER | 3 | |
| 014 | MAIN TRANSFORMER | 3 | |
| 015 | LV SWITCHGEAR BOP (TO BE SUPPLIED BY OTHERS) | 3 | |
| 140 | STEAM TURBINE GENERATOR (STG) | 1 | |
| 141 | CONDENSER | 1 | |
| 142 | CONDENSATE VACUUM PUMP | 2 | |
| 143 | BOILER FEED WATER PUMPS | 2 | |
| 144 | WATER POLISHING SYSTEM | 1 | |
| 145 | CONTROL SYSTEM MODULE | 1 | |
| 146 | BATTERY (125VDC) SET UP | 1 | |
| 147 | CHEMICAL INJECTION SKID | 1 | |
| 148 | CHEMICAL TOTE FOUNDATION | 1 | |
| 149 | MAIN COOLING TOWER | 1 | |

**EQUIPMENT LIST LOCATED INSIDE CONTROL HOUSE (PIN #432)
QUANTITY REPRESENTS ONE UNIT**

| PINS | DESCRIPTION | QTY | NOTES |
|------|--------------------------------------|-------|------------|
| 016 | UNIT CONTROL PANEL | 1 LOT | INSIDE 432 |
| 018 | TURBINE STARTER PANEL | | INSIDE 432 |
| 018A | ULTRA PROTECTION PANEL | | INSIDE 432 |
| 326 | 480V SWITCH GEAR | 1 LOT | INSIDE 432 |
| 327 | MOTOR CONTROL CENTER (MCC) | 1 LOT | INSIDE 432 |
| 337 | LIGHTING DISTRIBUTION TRANSFORMER | 2 | INSIDE 432 |
| 338 | LIGHTING AND DISTRIBUTION PANEL | 2 | INSIDE 432 |
| 354 | VARIABLE FREQUENCY DRIVE (VFD) | 1 LOT | INSIDE 432 |
| 360 | UPS 3-125VDC/120VAC-UCP | 1 LOT | INSIDE 432 |
| 362 | UPS 2-24VDC FIRE AND GAS | 1 LOT | INSIDE 432 |
| 364 | UPS 1-24VDC DC LUBE OIL PUMP STARTER | 1 LOT | INSIDE 432 |
| 454 | SCS PANEL | | INSIDE 432 |

DETAIL A
SCALE: 1:200 (FROM SHEET 1)
SIEMENS TRUCK CYCLE PROPOSAL
COMBINED CYCLE PROPOSAL



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SCALE: 1:200
DATE: 08/14/2018
BY: J. CARLOS
APPR. BY: J. CARLOS
DRAWN BY: J. CARLOS
PART: 28001-0218

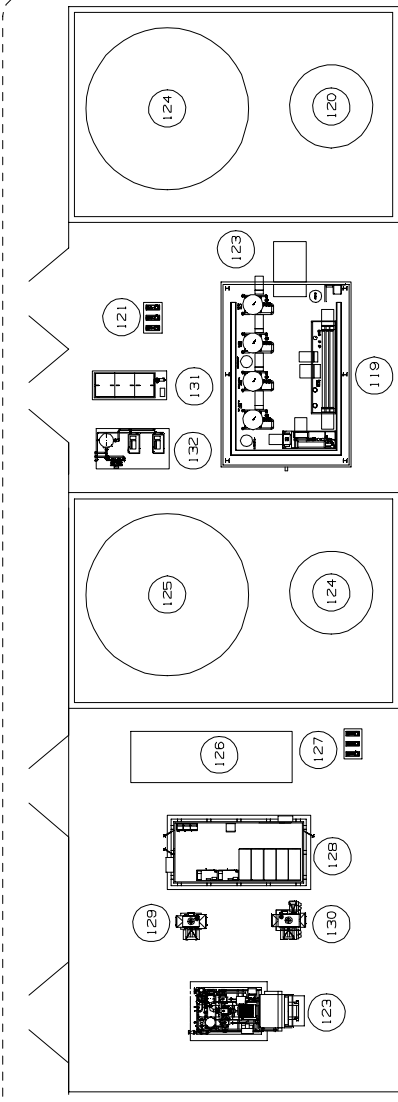
3RD ANGLE PROJECTION
ENGR. 31

SIEMENS ENERGY, INC. POWER AND GAS
COMBINED CYCLE SITE PROPOSAL

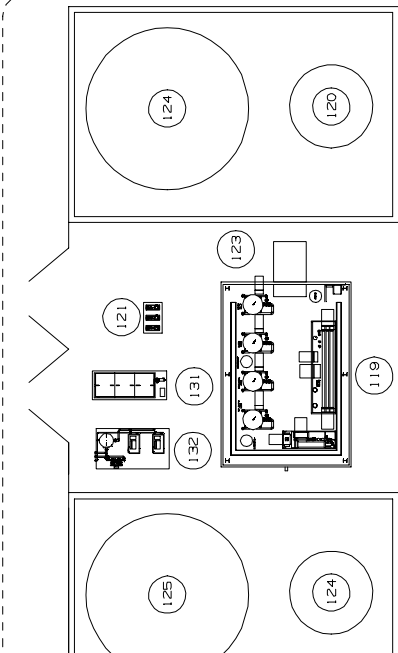
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SHEET: 2 OF 3
REV: 3
DATE: 08/14/2018

EQUIPMENT LIST MAJOR COMPONENTS

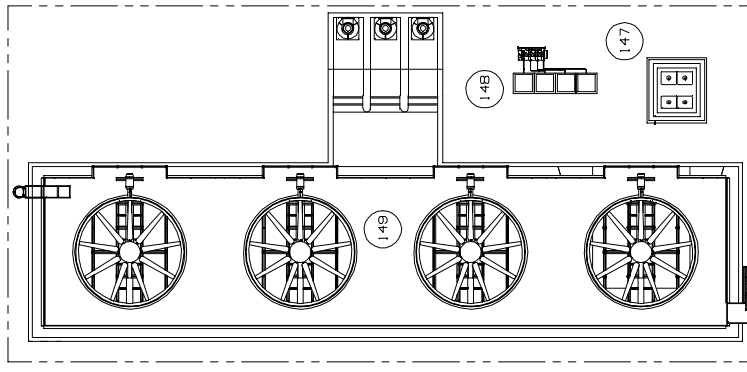
| PINS | DESCRIPTION | QTY | NOTES |
|------|----------------------------------|-------|-------|
| 119 | WATER TREATMENT SYSTEM | 1 LOT | |
| 120 | DEMIN WATER STORAGE TANK | 1 | |
| 121 | DEMIN FORWARDING PUMPS | 1 | |
| 123 | RAW WATER FORWARDING PUMPS | 1 | |
| 124 | RAW WATER STORAGE TANK | 1 | |
| 125 | RAW DIESEL TANK | 1 | |
| 126 | DIESEL FUEL TREATMENT | 1 | |
| 127 | DIESEL FORWARDING PUMPS | 1 | |
| 128 | MEDIUM VOLTAGE GENERATOR BREAKER | 1 | |
| 129 | AUX TRANSFORMER 13.8KV/4.16KV | 1 | |
| 130 | AUX TRANSFORMER 4.16KV/460V | 1 | |
| 131 | OIL/WATER SEPARATOR | 1 | |
| 132 | AIR COMPRESSOR | 1 | |
| 140 | STEAM TURBINE GENERATOR (STG) | 1 | |
| 141 | CONDENSER | 1 | |
| 142 | CONDENSATE VACUUM PUMP | 2 | |
| 143 | BOILER FEED WATER PUMPS | 2 | |
| 144 | WATER POLISHING SYSTEM | 1 | |
| 145 | CONTROL SYSTEM MODULE | 1 | |
| 146 | BATTERY (125VDC) SET UP | 1 | |
| 147 | CHEMICAL INJECTION SKID | 1 | |
| 148 | CHEMICAL TOTE FOUNDATION | 1 | |
| 149 | MAIN COOLING TOWER | 1 | |



DIESEL GAS (FUEL) TREATMENT PROPOSED SYSTEM



WATER TREATMENT PROPOSED SYSTEM



DETAIL B
 SCALE 1:200 (FROM SHEET 1)
 DIESEL GAS (FUEL) & WATER TREATMENT PROPOSED SYSTEMS

| REV NO | ECO NO / DESCRIPTION | DATE |
|--------|------------------------------|------|
| 1 | ISSUE TR EPC, Enbridge E & C | |

SIEMENS
 SIEMENS ENERGY, INC. POWER AND GAS
 COMBINED CYCLE SITE PROPOSAL

EXPORT-CONTROLLED DOCUMENT
 THIS DOCUMENT CONTAINS TECHNICAL DATA WHOSE UNLAWFUL EXPORTATION IS PROHIBITED BY THE EXPORT ADMINISTRATION REGULATIONS (EAR) OF THE U.S. DEPARTMENT OF COMMERCE. IT IS THE RESPONSIBILITY OF THE USER TO OBTAIN NECESSARY EXPORT PERMITS. UNLAWFUL EXPORTATION IS STRICTLY PROHIBITED.
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ENR: 21
 ENR: 13 G. MILEY
 APPR: BY N. CARUSO
 DRAWN BY: J. FRANK
 CHECKED BY: J. TAYLOR
 PART: DIESEL_2500V_0318

3RD ANGLE PROJECTION



Appendix B.

UAE Power System Requirements:

LNG Storage

Shiva Egambaram
Ban-Wee Eng
Regu Ramoo
Prof. Emeritus Thomas Lamb (U. Mich.)

Senior Process Engineer, Altair Malaysia
Principal Naval Architect, Altair Taiwan
VP of Engineering, Altair Engineering, Inc., Troy, Michigan, USA
Technical Consultant, IMPD, Seattle, Washington, USA



Cubic Donut Tank System (CDTS) for Land Storage



Altair

July, 2018



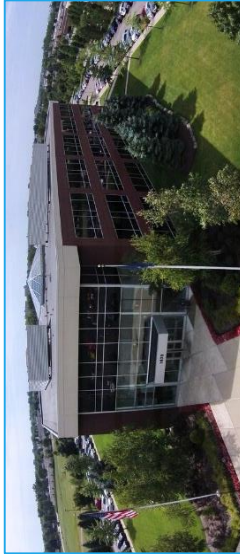


Altair

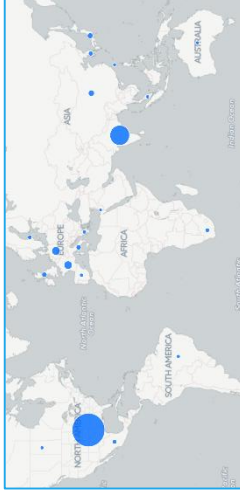
Corporate Overview



ALTAIR AT A GLANCE



Founded **1985**
Headquartered in Troy, MI US



69 offices
in 24 countries



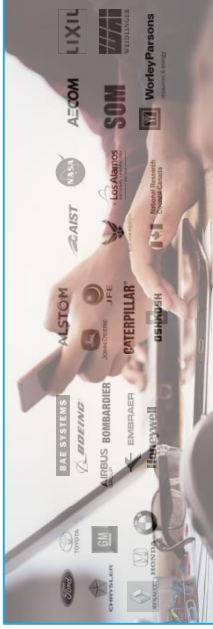
\$313M
2016 Revenue



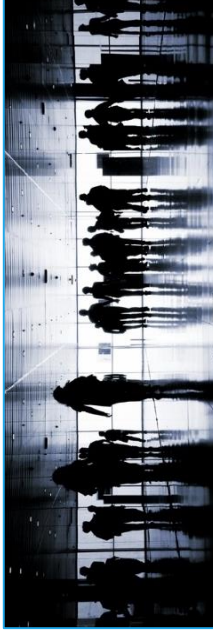
50+
ISV partners under our unique,
patented licensing model



2000+
Engineers, scientists and creative thinkers

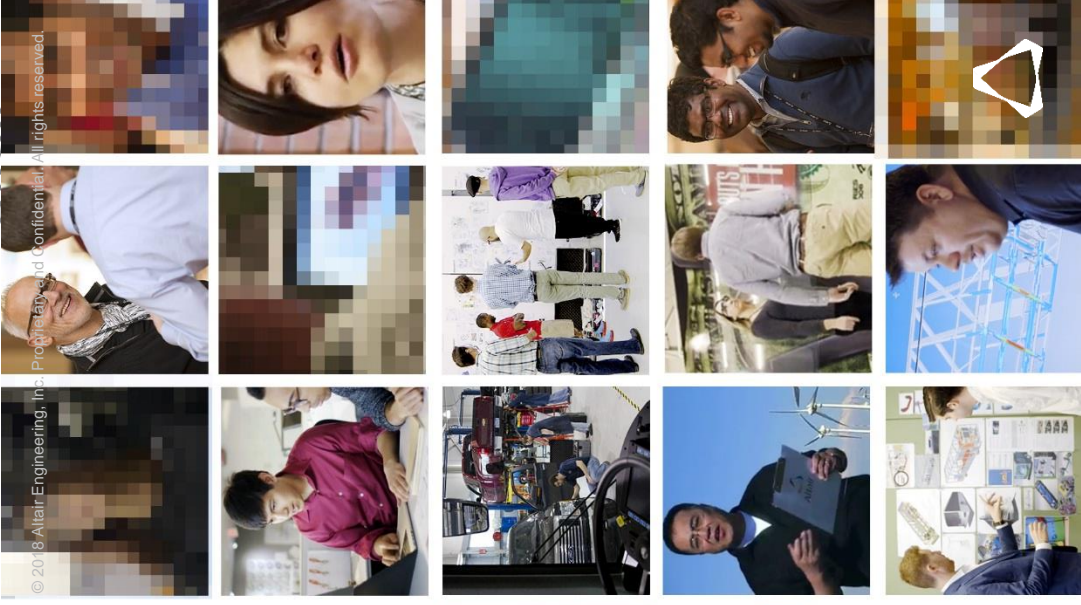


5000+
Customer installations globally



60,000+
Users

NASDAQ: ALTR



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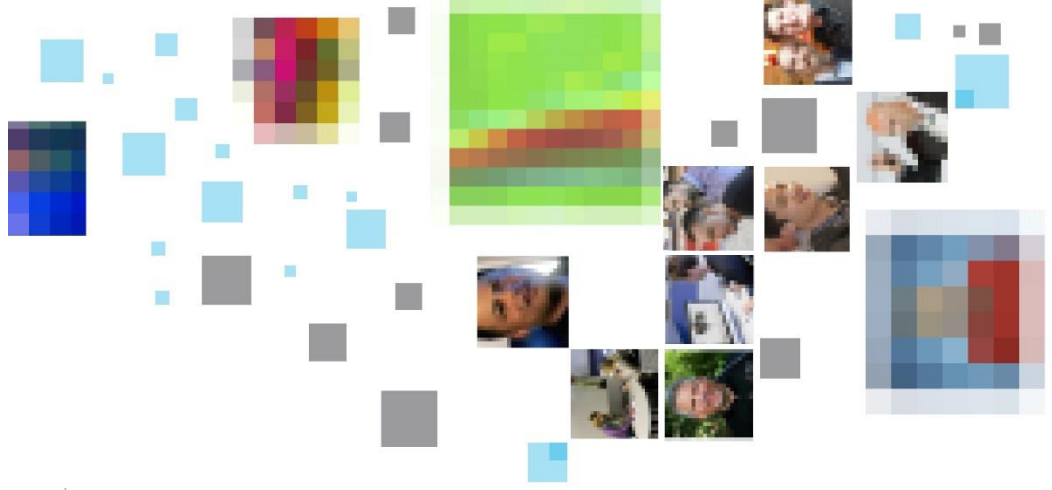
CULTURE & VALUES

Envision the future

Communicate honestly and broadly

Seek technology and business firsts

Embrace diversity and risk taking



OUR VISION



**Altair transforms design and decision making
by applying simulation, machine learning and optimization
throughout product lifecycles.**



Services – Not Just Another Software Developer

Altair has grown to become a global product development consultancy of 700+ designers, engineers, scientists and creative thinkers. The knowledge of real world product design and manufacturing has never been lost.

- Product Engineering
- Industrial Design
- Technical Staffing
- HyperWorks Solutions
- Analytics Solutions





We Work with Some of the Best

| Automotive | Aerospace | Heavy Equipment | Government |
|---------------------|--------------------------------|-----------------|--------------|
| | | | |
| Life/Earth Sciences | Electronics/ Consumer Goods | Energy | Architecture |
| | | | |

5,000 customers worldwide



Altair

**Engagements in the Marine
Industry**

Altair Marine Customers



HYUNDAI
HEAVY INDUSTRIES CO., LTD.

SAMSUNG

DAEWOO

Sea Ray

WÄRTSILÄ

Mitsui Engineering & Shipbuilding Co., Ltd.

ibm
Mitsubishi Heavy Industries Group

CARDEROCK DIVISION
NAVSEA
WARFARE CENTERS

NAVSEA
WARFARE CENTERS

NORTHROP GRUMMAN MISSION SYSTEMS

GENERAL DYNAMICS
Electric Boat

MARTEC™
Smart Solutions for Engineering, Science & Computing

CHORYO ENGINEERING
Mitsubishi Heavy Industries Group

CARDEROCK DIVISION
NAVSEA
WARFARE CENTERS

NAVSEA
WARFARE CENTERS

NORTHROP GRUMMAN
DEFINING THE FUTURE

ATLAS ELEKTRONIK
A joint company of ThyssenKrupp and EADS

BAE SYSTEMS

THALES

Bath Iron Works
A GENERAL DYNAMICS COMPANY

babcock

WEIDLINGER ASSOCIATES® INC
CONSULTING ENGINEERS

MARIC

SWAN HUNTER

KAWASAKI

MANI

IHI MARINE UNITED

YAMAHA

NAV AIR
NAVAL AIR SYSTEMS COMMAND

GERMANY

STX Shipbuilding

LURSSEN

VT Group

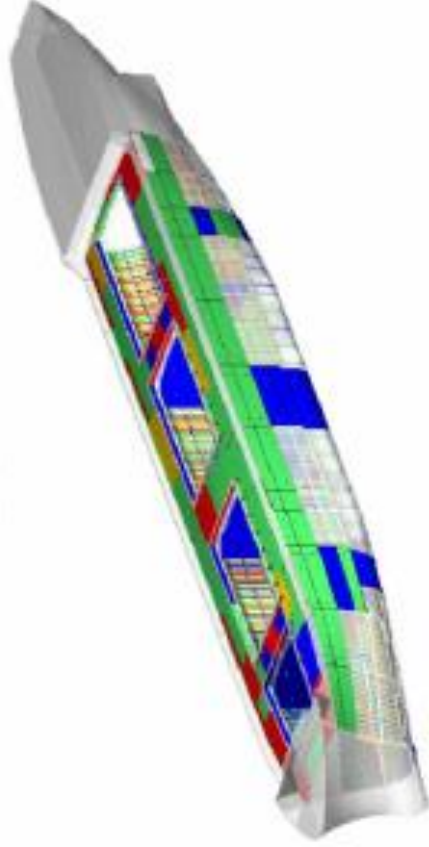
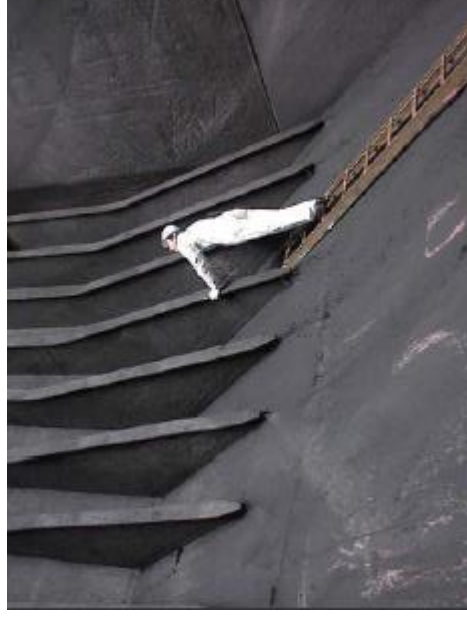
Altair Marine Customers

- Altair's HyperWorks software suite is recognized by the marine industry as best-in-class for Computer Aided Engineering (CAE)
- Leading shipyards and maritime classification societies including Hyundai Heavy Industry, STX, Sumitomo, Tsuneishi, Jiangnan, BAE Systems, General Dynamics Electric Boat, Lloyd's, ClassNK, and ABS have adopted HyperWorks as a next-generation simulation technology for ensuring structural performance and constructability while meeting cost targets.
- Altair's technologies have been applied to vessels ranging from racing yachts and leisure craft, to naval and commercial ships covering hull form drag, dynamic control, underwater explosions, wave response, composite materials usage, electromagnetic compatibility, and manufacturing process assessment,

PrimeShip Hull

- HyperWorks chosen as platform after extensive evaluation.
- Altair Product Design has been awarded to develop the new hull design system

ClassNK
PrimeShip-HULL



Altair - Structures Design Solution Partner for CVF

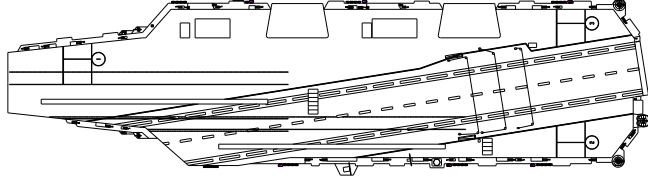
- The Royal Navy's two new aircraft carriers (CVF) are expected to enter service in late 2015 and 2018
- The CVF programme is being managed by Aircraft Carrier Alliance (ACA). The Alliance Partners are:
 - Thales Naval Ltd
 - BVT Surface Fleet Limited (JV VT Shipbuilding & BAE Systems)
 - Babcock Marine
 - The UK MOD

• **The ship structure is being designed to meet the standards of Lloyd's Register Rules and Regulations for the Classification of Naval Ships and upon completion the vessels will be entered into Lloyd's Class**

- **"Aircraft Carrier Alliance select Altair as Structures Design Solution Partners"** (design compliance with 'Lloyds Register Rules & Regulations for the Classification of Naval Ships')
- Altair team work closely with LR on the CVF program



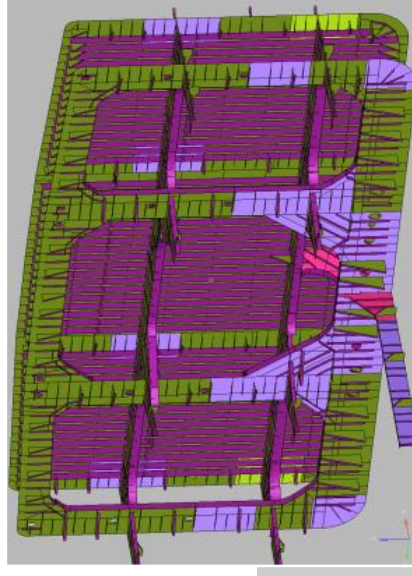
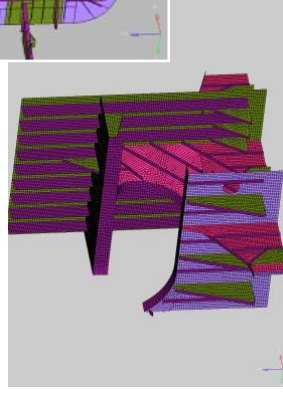
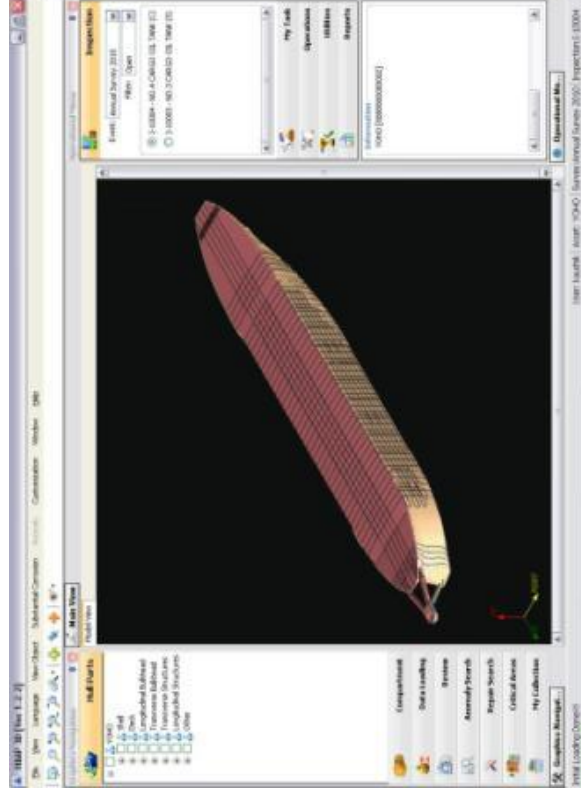
CVF (CV) – UK ~ 65,000 tonnes



Hull Inspection Maintenance Program 3D (HIMP3D)

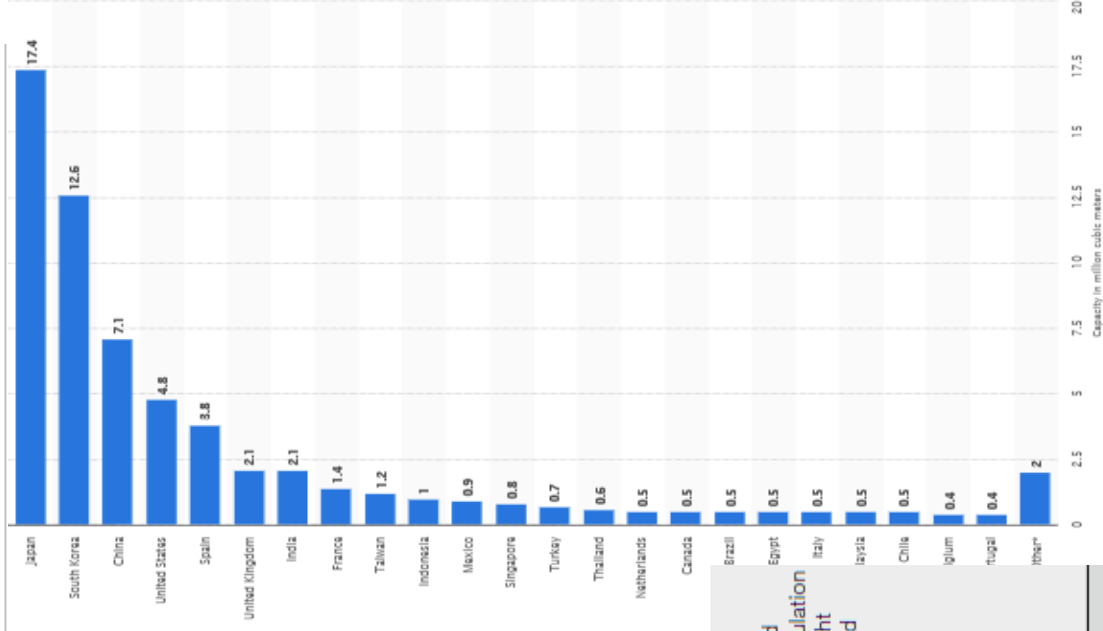
Project Objective

Standardize across ABS and its customers a solution for Marine Systems Classification, Inspection and Repair, to include ABS Classification rules build in + an interface to CAE system for the purpose of validating and optimize the repair operations



Land Storage LNG Tanks

Storage tank capacity for liquefied natural gas worldwide in 1st quarter 2018, by country (in million cubic meters)

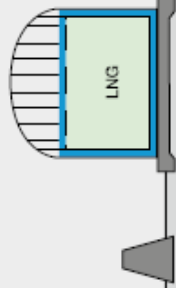


The approximate number of field erected LNG tanks operating worldwide is summarized in the following list¹:

- Single Containment Type 320
- Double Containment Type 15
- Full Containment Type 110
- Membrane Containment Type 30
- Membrane In-ground Containment Type 50

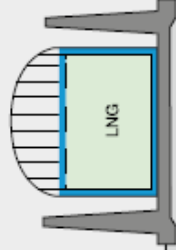
Single containment tank

- Primary container contains liquid and vapour
- Outer shell retains insulation
- Bund around the tanks retains liquid (not vapour) if primary container fails.



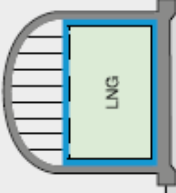
Double containment tank

- Primary container contains liquid and vapour
- Outer shell retains insulation
- Secondary container is an open top tank that retains liquid (not vapour) if primary container fails.



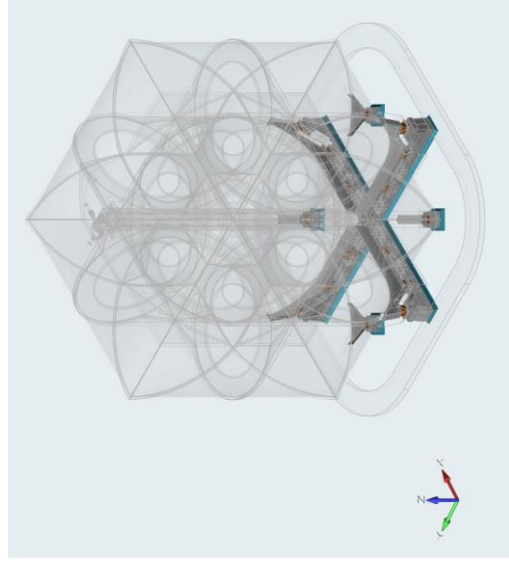
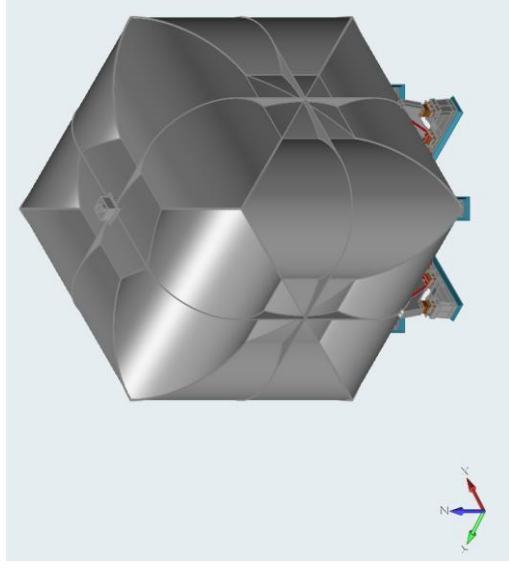
Full containment tank

- Primary container contains liquid
- Secondary container retains insulation and is also liquid and vapour tight
- Smallest foot print since no bund around the tanks is required.




CDTS for Land Storage

- LNG Kitania has sent us an Expression of Interest Letter to Tank EPC and Altair to Supply 16 40K CDTs Tanks
- The Tank EPC will fabricate and erect the CDTs modules. **Altair is the licensor of the CDTs Technology and is responsible for all Design Drawings and Approvals.**
- The Delivery timeline is 24 months after signing agreement to supply the first tranche of ~4 of 40K tanks and the remaining over a 3-year period thereafter
- The tank team is here today at IOCL in New Delhi to introduce and explain the CDTs Technology
- Wartsila is the EPC for the Port, Plat prep., Gas Systems & Engineering for tank and Gasification system




9Ni Single Containment CDTs

LNG Kirtania Ownership, Development & Operation Structure




EnergyGiant Limited

Consortium Lead & Project Developer




CREATIVE PORT

Port Owner & Operator



WÄRTSILÄ

LNG Terminal Operator, Re-Gasification Infrastructure, Gas Engineering for storage tanks, BoG Handling, Plant Controls, Electronics, Safety, Firefighting Package, metering, Instrumentation, controls & Powerplant



KOMAC
KOREA MARITIME CONSULTANTS CO., LTD.

EPC for berths
EPC for Civil Works related to ReGas & Gas Storage

LNG Storage Tank Team



*Licensor of the CDTs Technology

*Overseeing PE



KOMAC
KOREA MARITIME CONSULTANTS CO., LTD.

CDTS* Storage Tanks Supplier
CDTS* Environmental Cover Supplier



WÄRTSILÄ

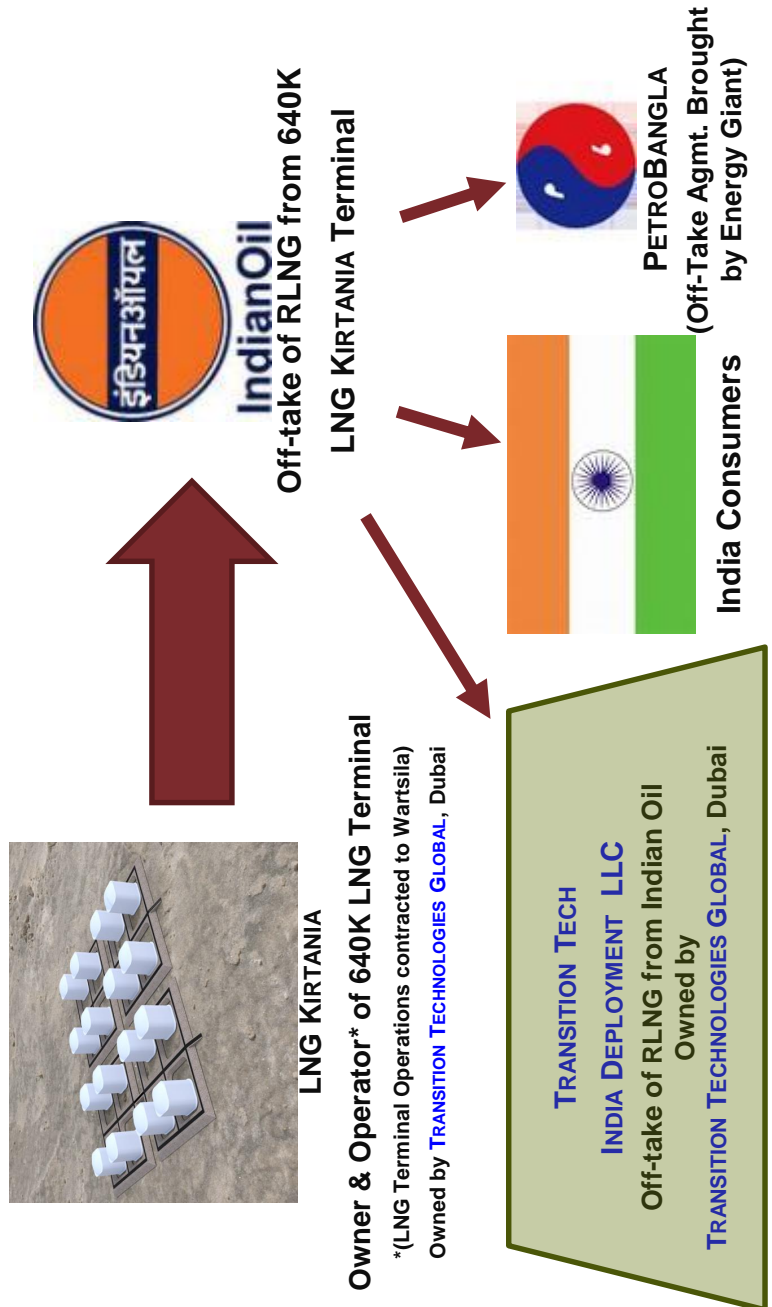


CALLENBERG
TECHNOLOGY GROUP



TRIDENT
Maritime Systems

CDTS* Tank Insulation & Gas System Suppliers up to tie-up point of Wärtsilä Gasification Unit



Role and Responsibilities as the CDTs Tank Technology Licensor CDTs

- **Altair will deliver the 40K net 3-D CDTs Tank Shell Design which meets or exceeds API 620/625 and NFPA59A standards**
- We will appoint a local India based Tankage Engineering PE-Civil to secure API620/625 & NFPA59A or equivalent from local regulators
- Our team will work closely with the tank fabricator(s) who will be responsible for fabricating the CDTs tank modules and the erection of the modules on-site. **Our tank fabricator will provide warranties against tank leakage due to material & weld quality**
- **Our Gas Engineering partner will use our basic Gas Engineering layout to develop the detailed Gas Engineering package, secure relevant approvals, and provide operational and Gas engineering related warranties.**
- **Our Insulation Partner who would use our basic insulation space requirements to develop and install the insulation system and provide LNG Kirtania with the BoG rate warranties.**

Understanding Shape Influence on Structural Efficiencies for Hydrostatic Containment



For self-standing Independent tanks, structural compliance provides a measure of structural efficiency

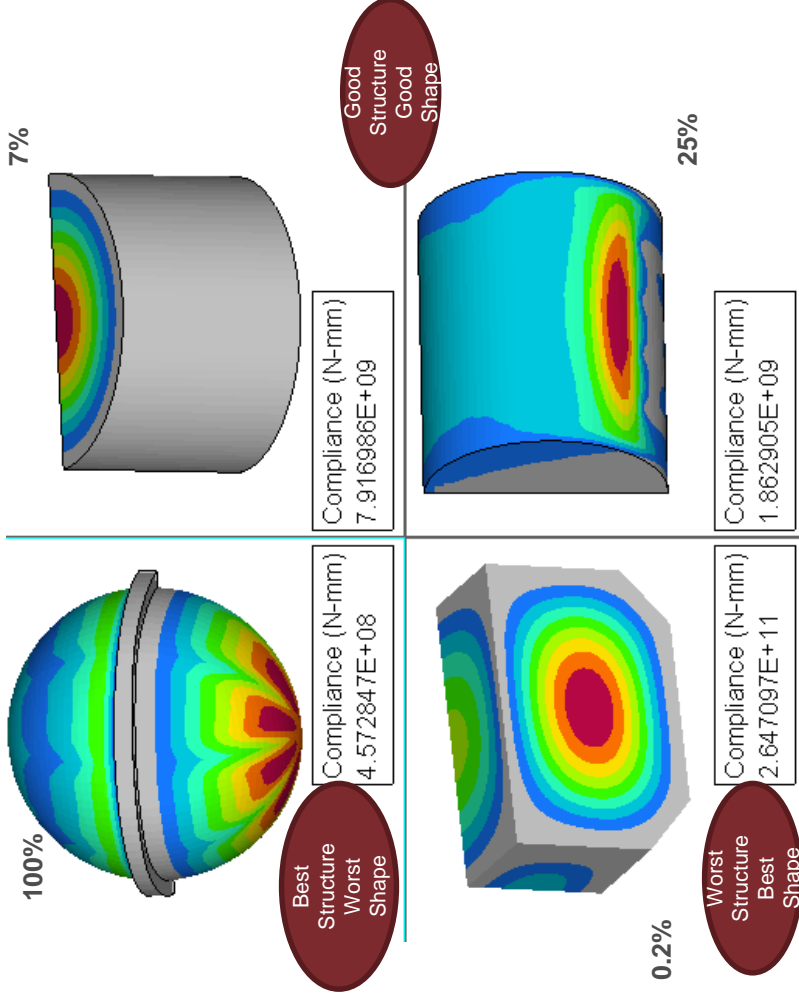
- Spherical Shapes have the highest structural efficiency
- Cylindrical Shapes have good structural efficiency
- Prismatic shapes have the worst structural efficiency

For maximum stiffness (K), the compliance (C) can be minimized. For a structure with an applied displacement (U), the compliance (C) can be considered a direct measure of the stiffness (K)

$$C = \frac{1}{2} U^T F = \frac{1}{2} U^T K U = \frac{1}{2} \frac{u^2}{K},$$

$$\text{with } \frac{1}{2} u^2 = \text{constant}$$

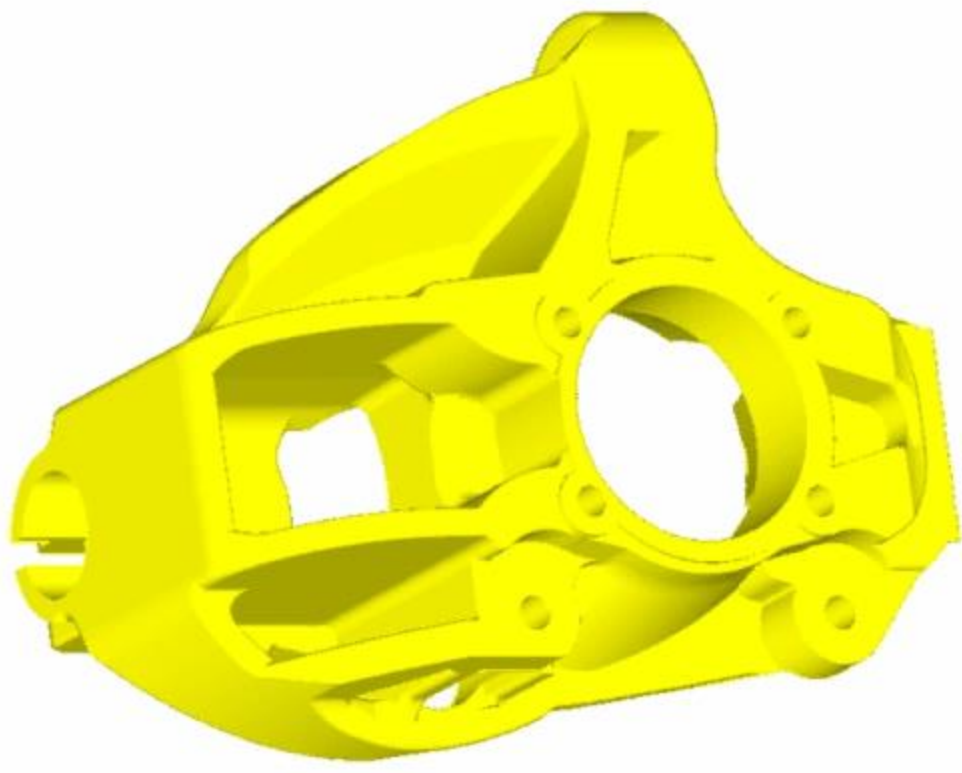
Full Hydrostatic Load + Gravity
100mm uniform thickness



CDTS DEVELOPED USING Altair's AWARD WINNING TECHNOLOGY

Altair Optistruct®:

Award-winning design synthesis technology



American Business Awards 2012



Company/Organization Awards Category Stevie® Award Winners

Companies of the Year –

Automotive & Transport Equipment: Ford Motor Co.

Computer Hardware: Apple Inc.

Computer Software:

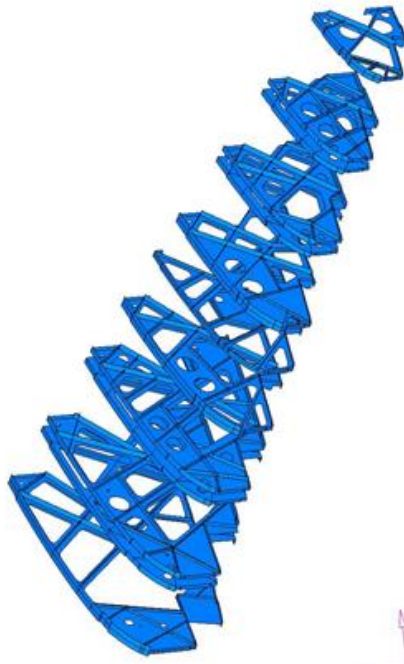
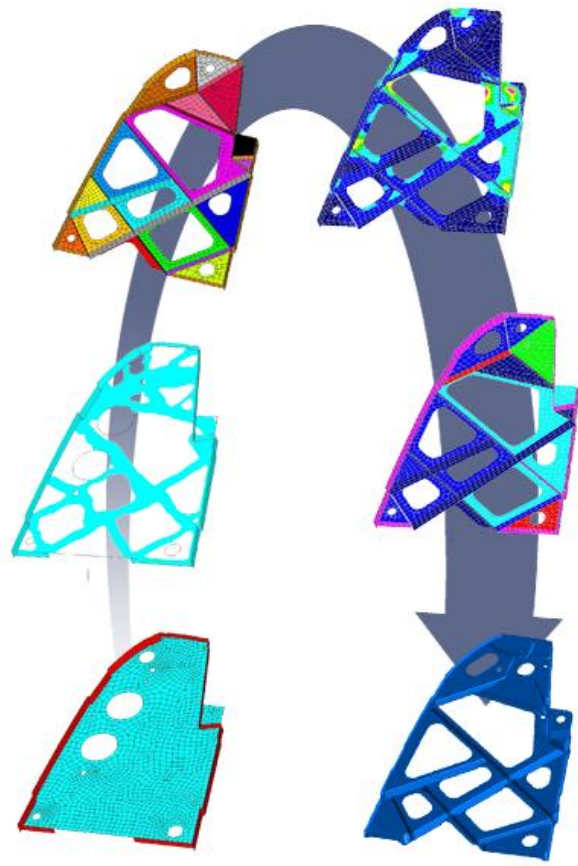
Altair

Aerospace and Defense: BE Aerospace

Telecommunications: Qualcomm



Industry Success - Leading Edge Rib Design for the AIRBUS A380



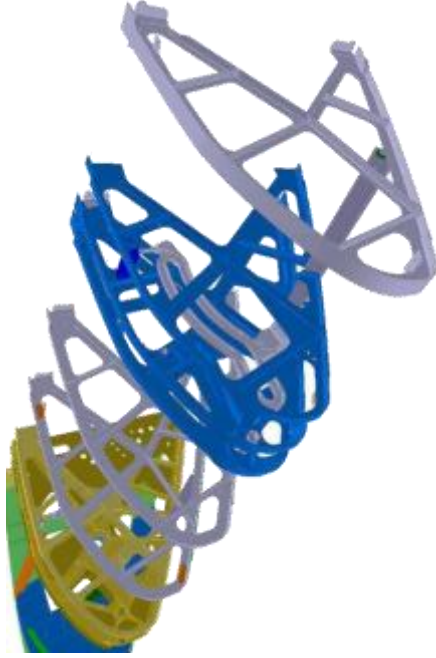
Results:
Mass Savings of 44% (500kg)
Deadline met: Ribs developed in 13 weeks

Aerospace Success Story



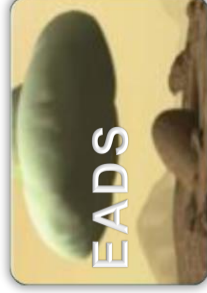
Topology, Size & Shape Optimization on the 787 Wing Structure

Met the target weight reduction: -12%
Quicker and more robust process development



“Boeing and partner Spirit AeroSystems are extensively using the OptiStruct optimization tool to design Fixed Leading Edge Wing Ribs. 50 unique rib designs have been created using the process and many are now being produced. The expected weight savings has been achieved.”

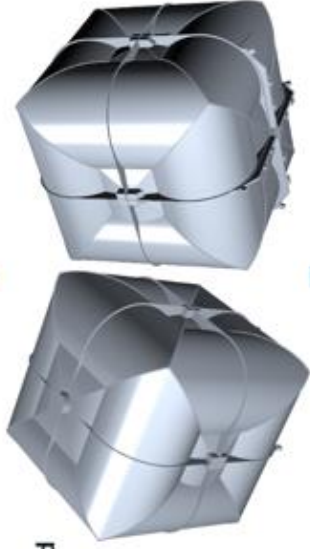
Stephen Amorosi, The Boeing Corporation, Seattle, WA



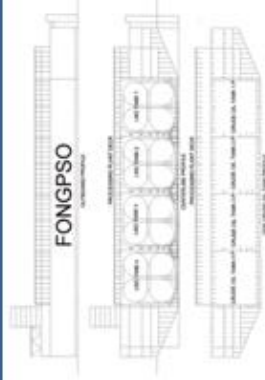
CDTS – Applications

Type B CDTS Tanks
>50,000 m³

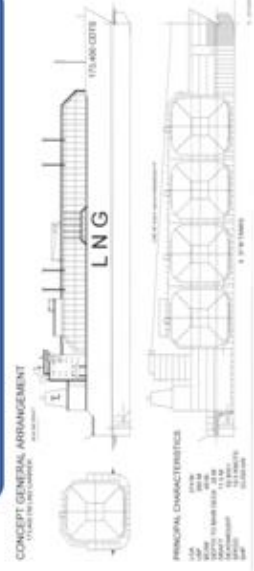
CDTS
cubic or cuboid



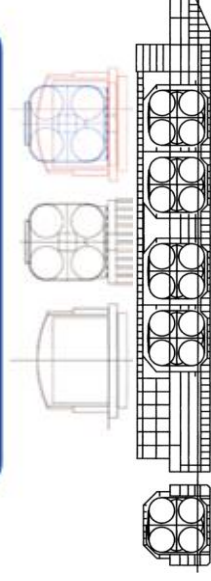
FLNG



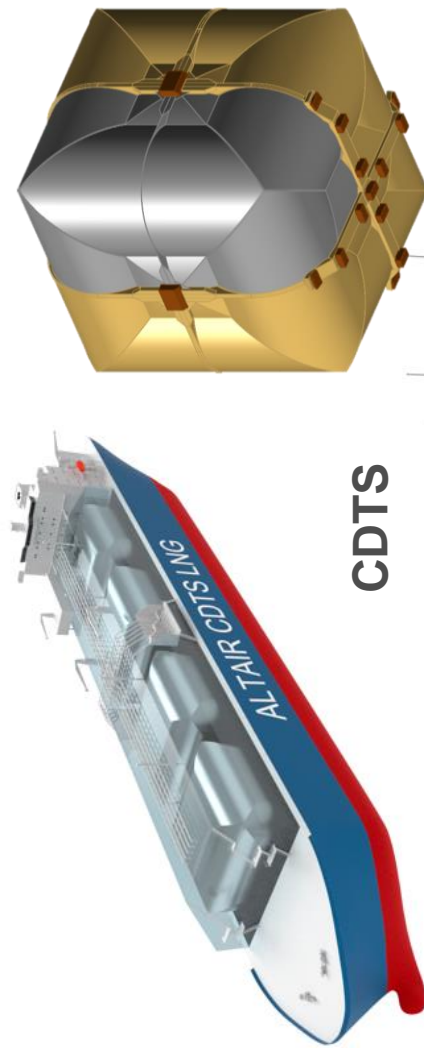
LNGC



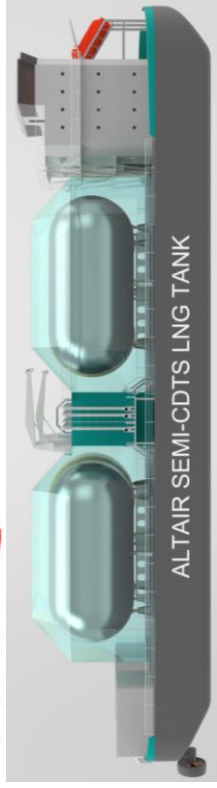
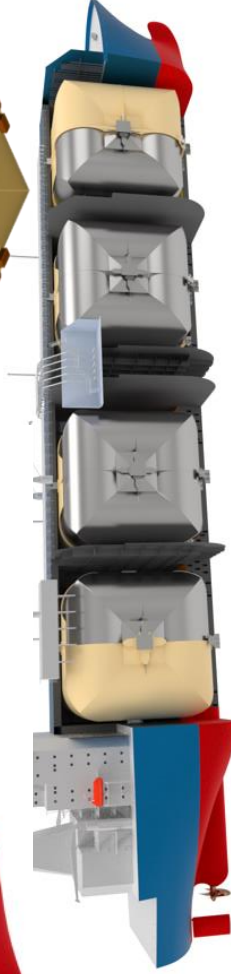
Land or Floating
Storage (FSU/FSRU)



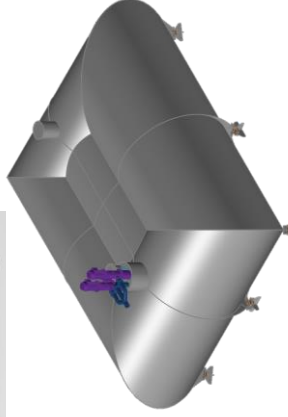
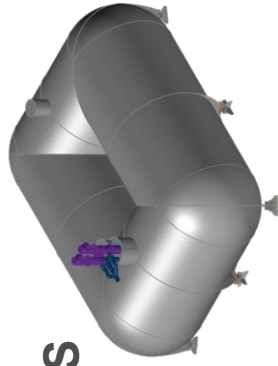
Approval-In-Principle (AIP) from ABS



CDTS



Semi-CDTS



Ref.: TASK#: T1333681
Project#: 3464039
Date: 30 April 2015

Certificate of Approval in Principle

As requested by:

Altair Product Design

ABS has reviewed documentation as specified in ABS letter dated 30 April 2015 for:

Cubic Donut Tank System (CDTS) for LNGC - Concept Design

and found the system to be satisfactory with respect to the intent of the following:

- 1- ABS Rules for Building and Classing Steel Vessels, Jan. 2014
- 2- ABS Guidance Notes on Review and Approval of Novel Concepts, Jun. 2003
- 3- ABS Guide for Building and Classing Liquefied Gas Carriers with Independent Tanks, Jan. 2010
- 4- International Code for the Construction and Equipment of Ships Carrying Liquefied Gases in Bulk (IGC Code), 1993 Ed. and new IGC code effective July 2016 notwithstanding any additional detailed analyses that may be required when the new IGC code comes into force

subject to compliance with the comments in the above letter and the Rules. All drawings, calculations, test reports, and certificates for components are to be found acceptable to ABS.

ABS Americas

ABS CORPORATE, Technology



Suresh Pisin,
Manager of Houston SED

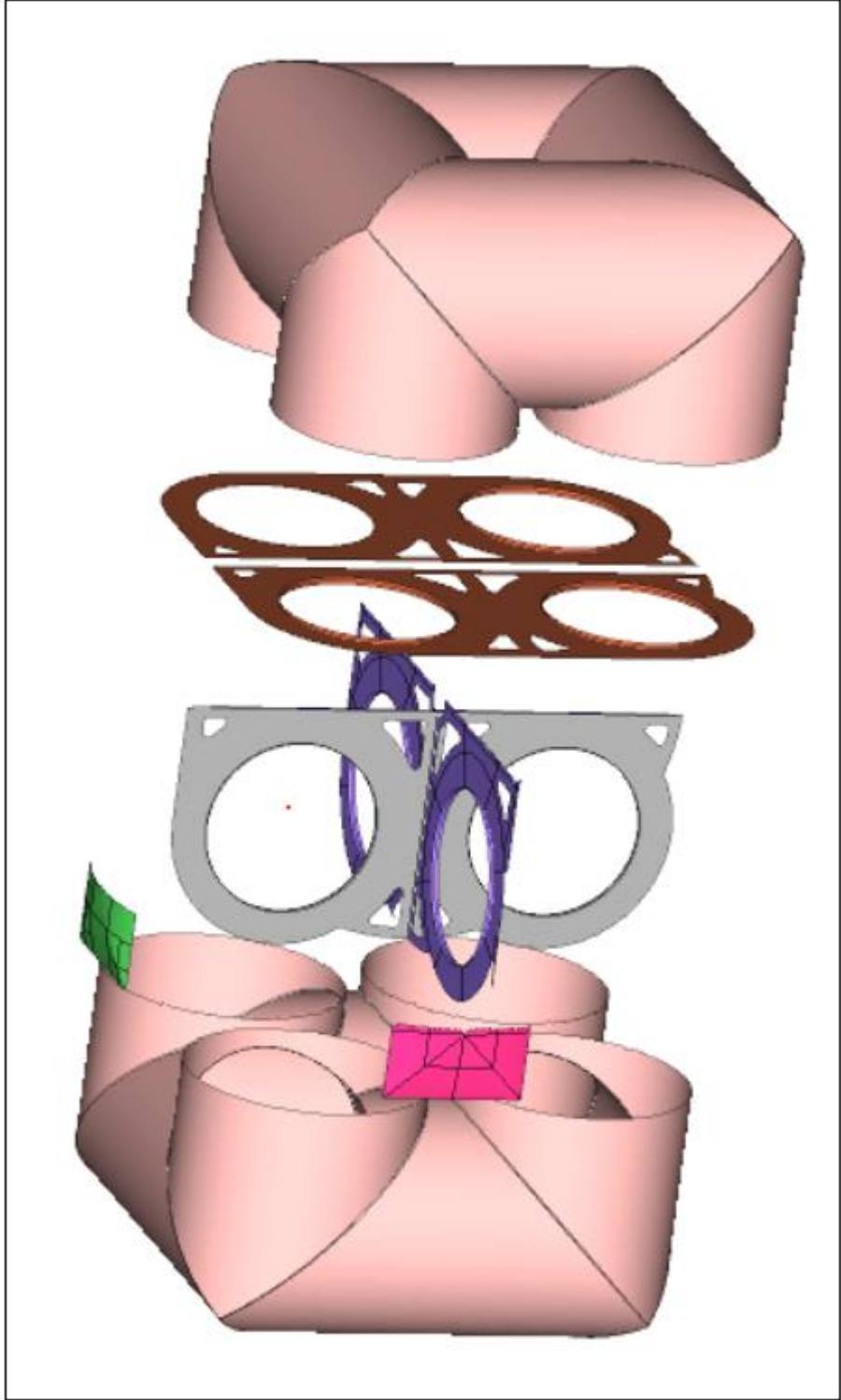
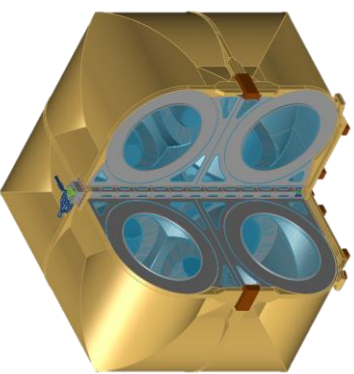
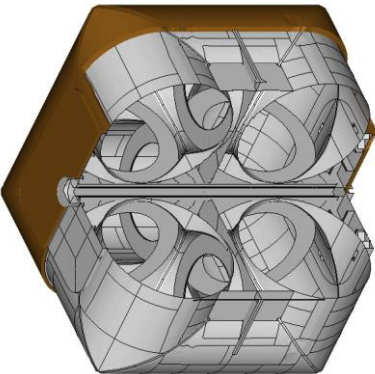


Yung S. Shin,
Head of Cargo Containment
Systems Group

Note: This certificate evidences compliance with one or more of the rules, Guides, standards or other criteria of American Bureau of Shipping or a statutory, industrial or manufacturer's standards and is issued solely for the use of the Bureau, its committees, its clients or other authorized entities. Any significant changes to the aforementioned product without ABS approval will result in this certificate becoming void. This certificate is governed by the terms and conditions in the ABS Rules.

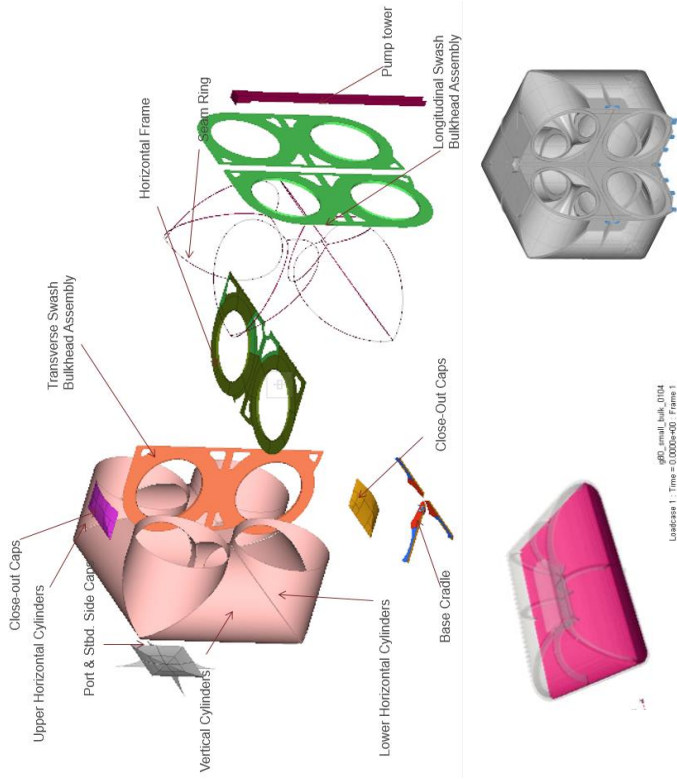
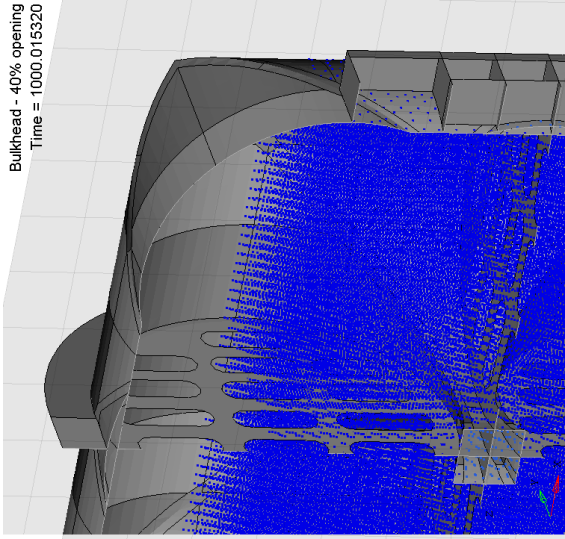
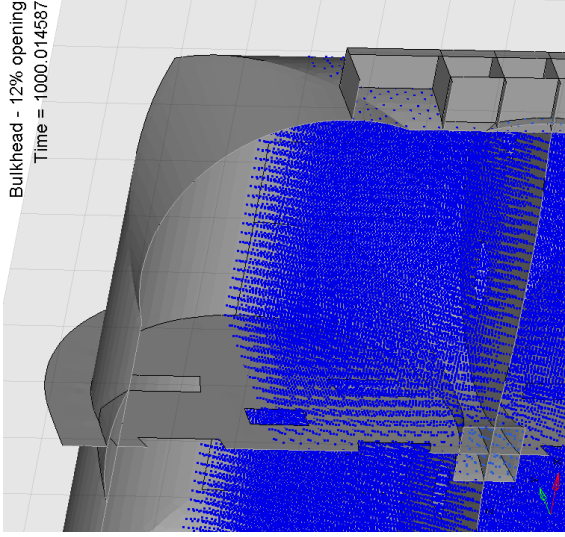


Altair



CDTs Exploded View

CDTS SLOSHING MITIGATION FEATURE

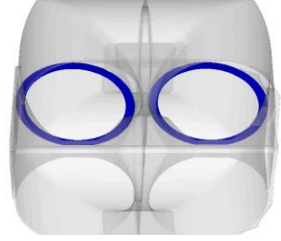
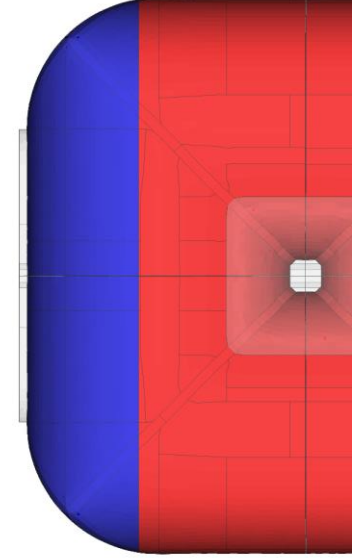
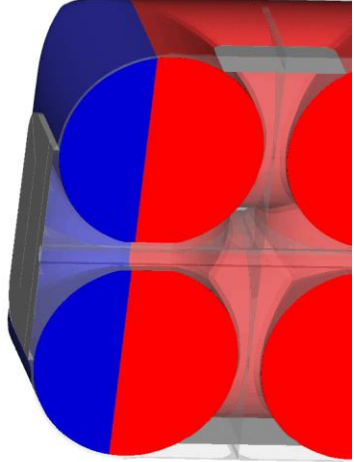


Contour Plot
Density (SI units value)
Loadcase 1
Min = 1.137E-09
Max = 5.022E-07
SOLID 59877

Contour Plot
Density (SI units value)
Loadcase 1
Min = 5.001E-07
Max = 1.142E-09
SOLID 59874

Loadcase 1 - Time = 0.000e+00 - Frame 1

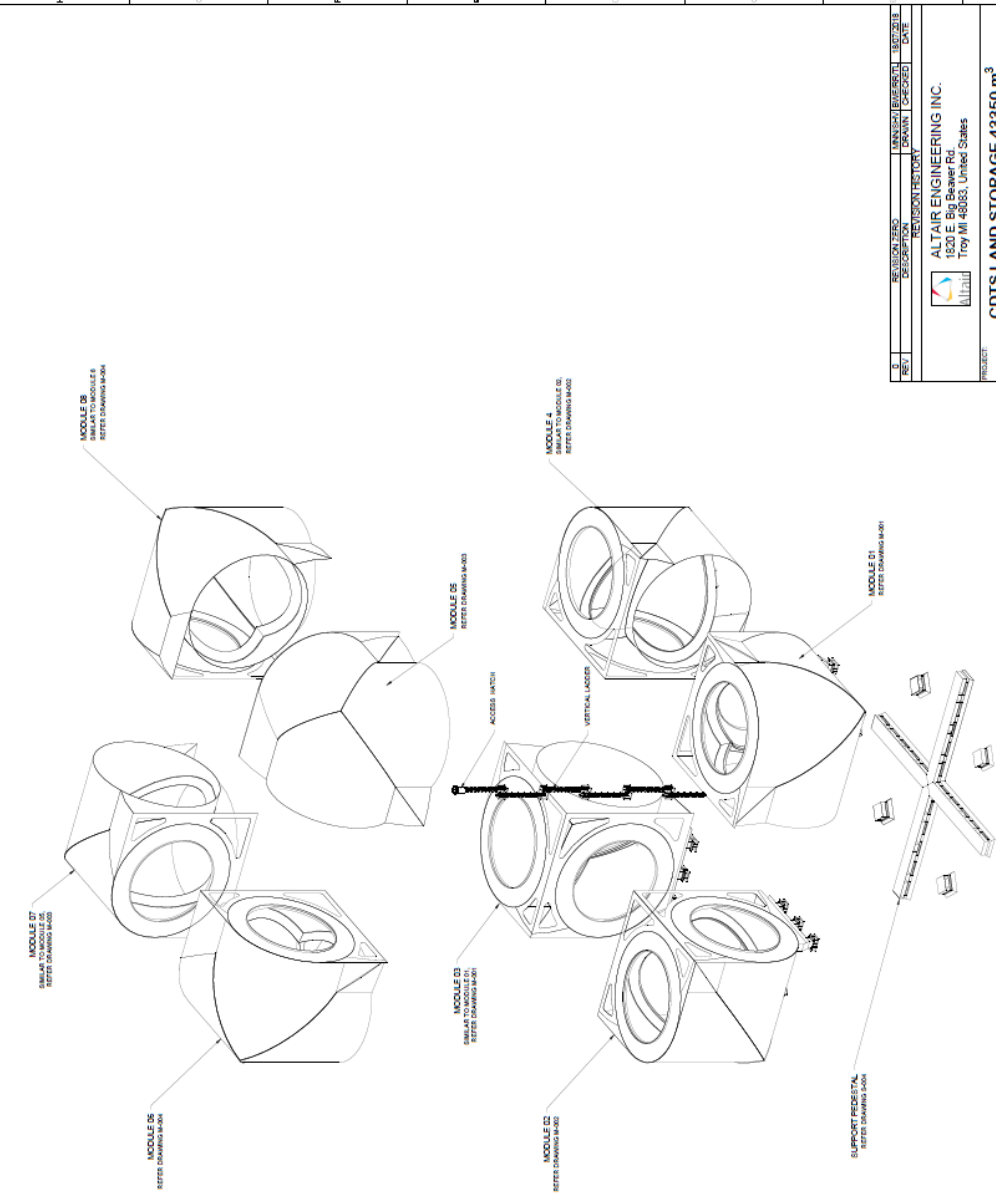
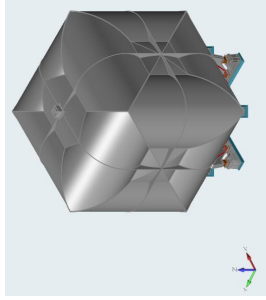
1. CDTS - sloshing_mitigation_004
Loadcase 1 - Time = 1000.0e+00 - Frame 1



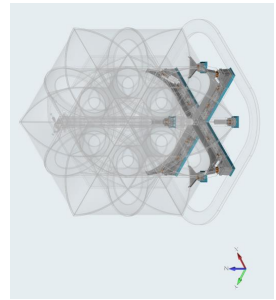
X
Z

X
Z

9Ni Single Containment CDTs



TANK MODULES EXPLODED VIEW



| REV | REVISION | ISSUED | DESIGNED | BY | DATE | APPROVED | DATE |
|-----|----------|--------|----------|-----|------|----------|------|
| 1 | REVISION | 1/2 | 1/2 | 1/2 | 1/2 | 1/2 | 1/2 |

| | | | | |
|--|-------|--------------|-------|-------|
| | | | | |
| ALTAIR ENGINEERING INC. 1830 E. Big Beaver Rd. Troy, MI 48063, United States | | | | |
| PROJECT: CDTs LAND STORAGE 43350 m ³ | | | | |
| TITLE: TANK ASSEMBLY | | | | |
| DRAWING NO. | SHEET | DRAWING SIZE | SCALE | UNITS |
| A-001 | 1/2 | A1 | 1:250 | mm |

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Conventional Cylindrical Containment Tanks



Figure 7 Comparison of roof platforms with and without side wall discharge (courtesy Cheniere and Covec [11])

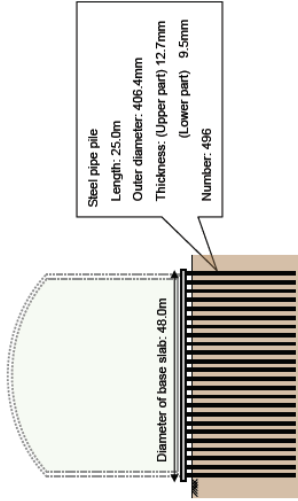


Figure 3.3. Specification of tank foundation

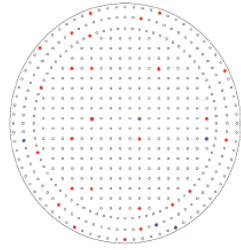


Figure 3.4. Framing plan of piles and the measured piles in corrosion survey

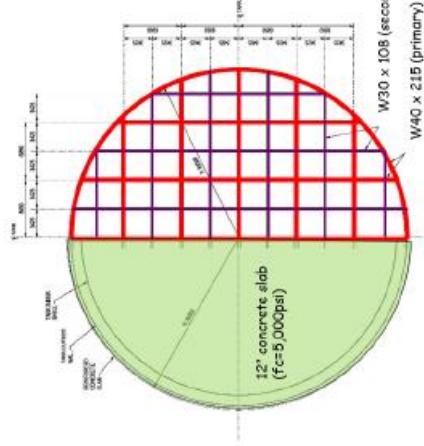


Figure 4 408 m³ 99%N₂ Steel Single Containment Modular LNG Tank General Arrangement

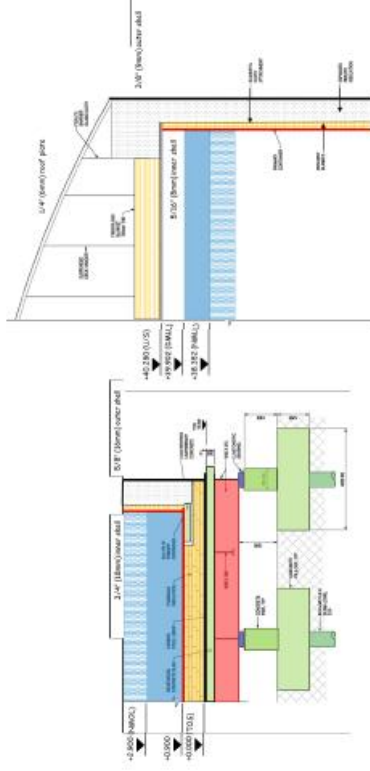
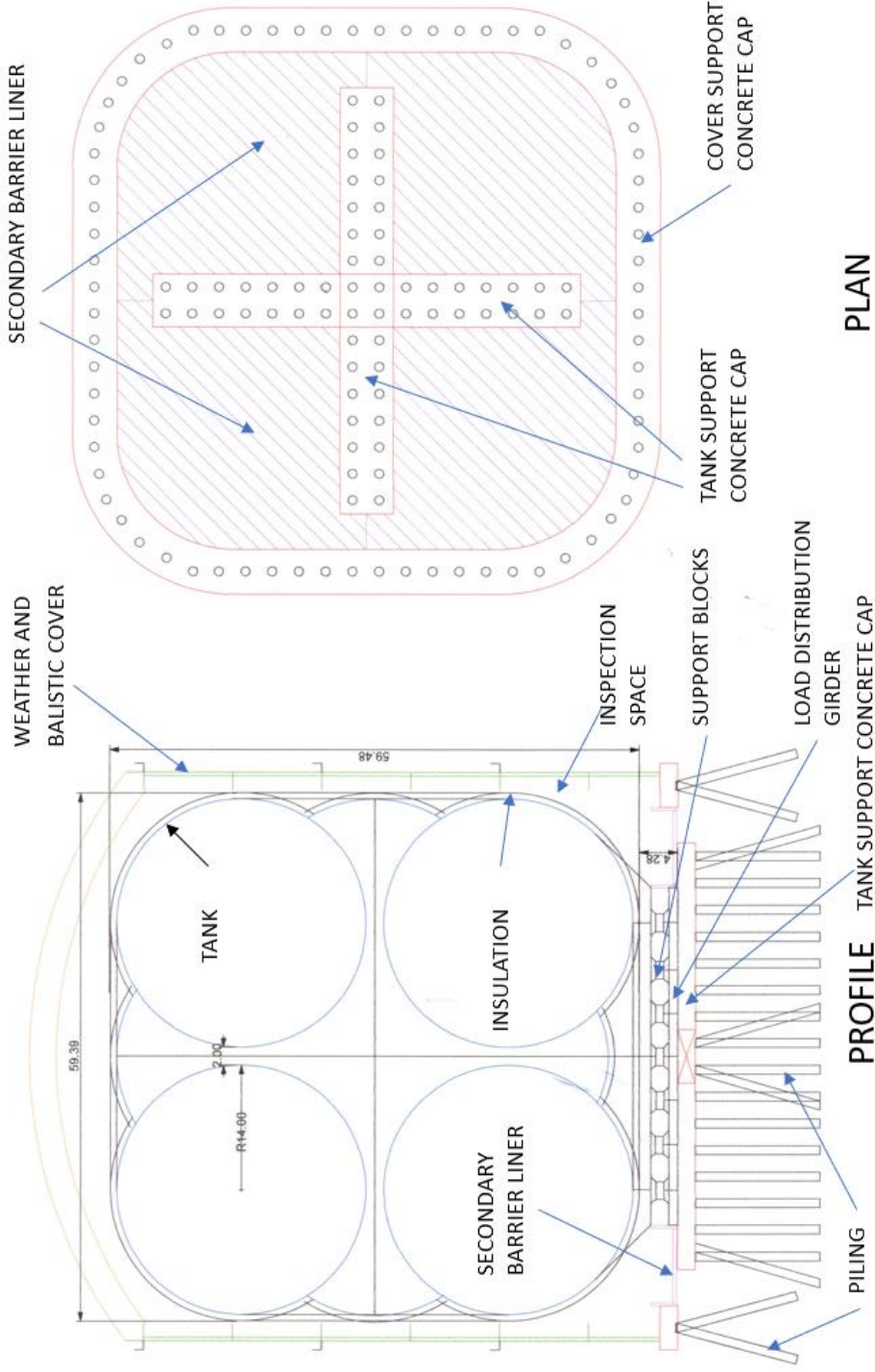


Figure 5 408 m³ 99%N₂ Steel Single Containment Modular LNG Tank Details

CDTS for Land LNG Containment

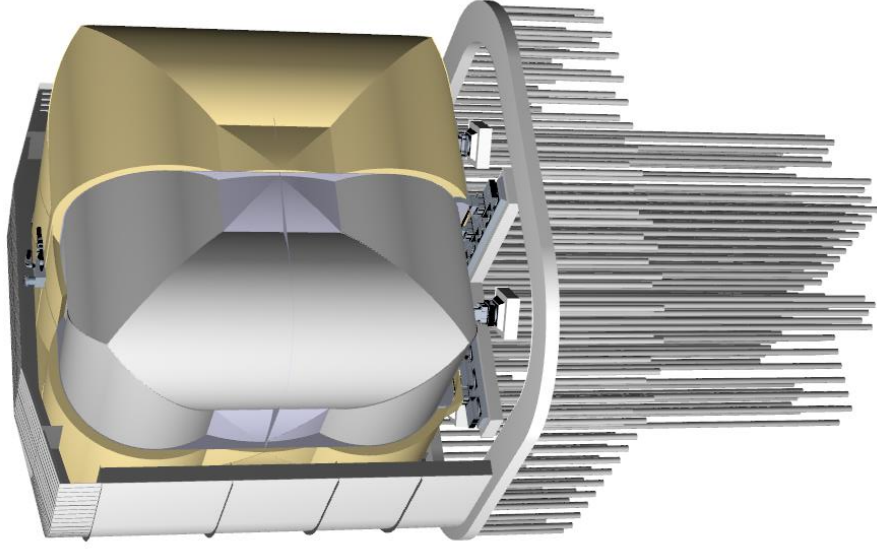
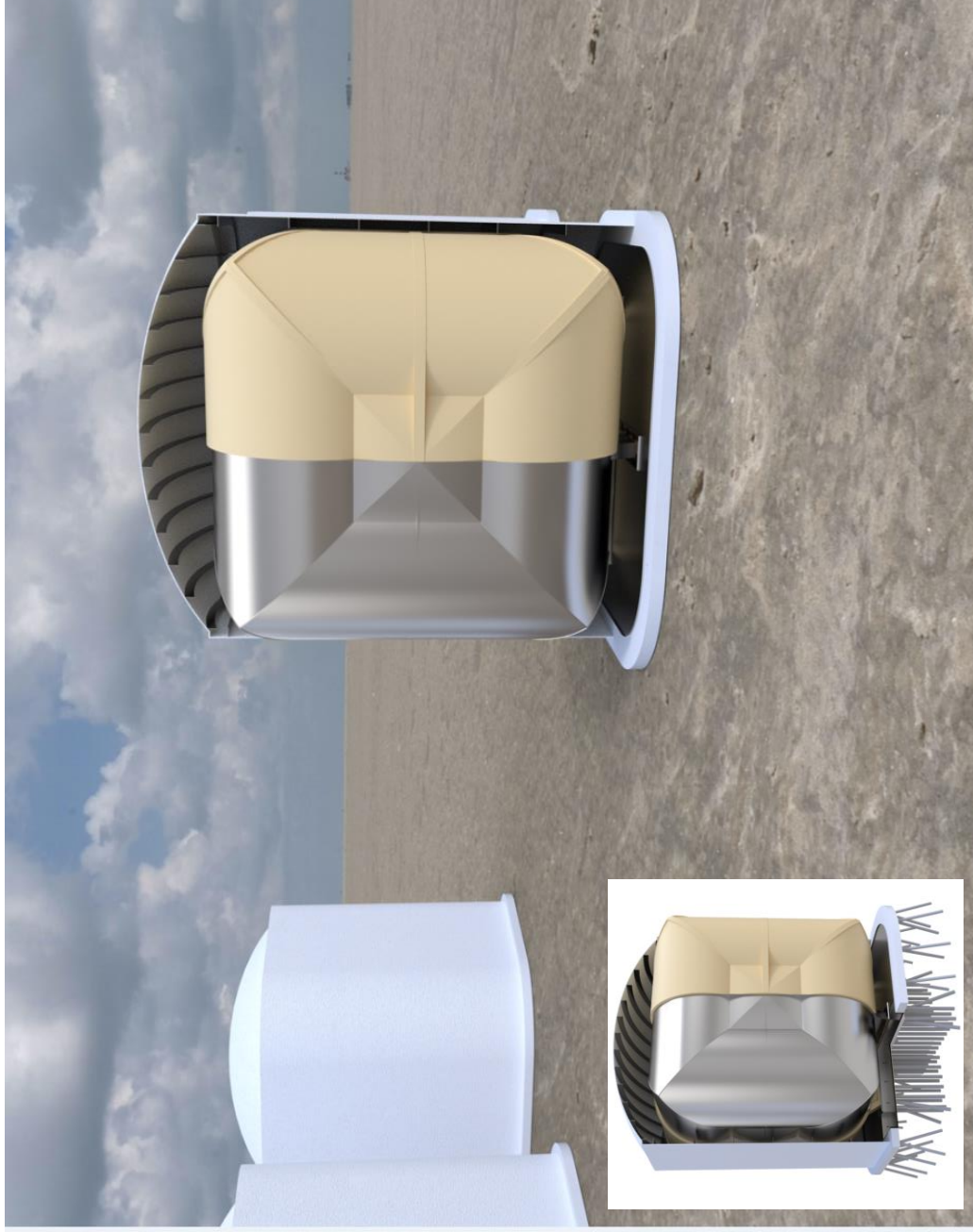
TL 4/8/2018

160 K CDTs LNG Land Storage Tank



TANK, COVER, CONCRETE FOUNDATION AND PILING CONCRETE STRIPS AND PILING

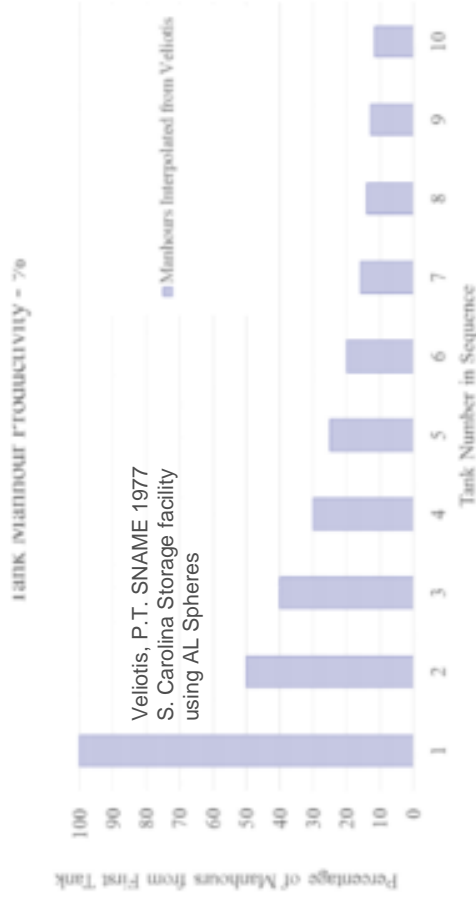
CDTS for Land LNG Containment



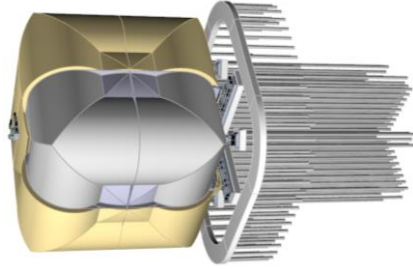
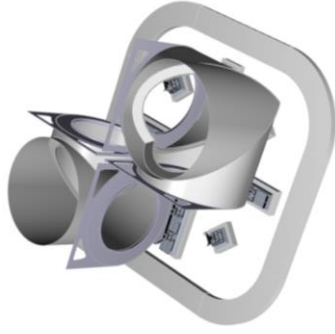
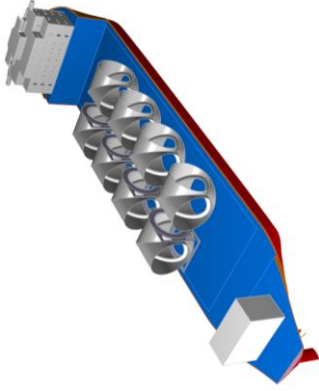
Benefits of Modularized Construction of CDTs Tanks

- Currently, most tank systems must be completely constructed on site, especially when they are large, as typically for land storage purposes
- Our self-standing tanks can be built at another site (by a third party company, perhaps specializing in constructing tanks), this is NOT possible for conventional tanks
- The proposed manufacturing method uses an assembly consisting of eight corners of the tank welded together leading to higher quality and productivity
- This enables CDTs tanks (40K CM Capacity) weighing a total of 2400t to be delivered as eight corners each weighing ~300 t or if lifting capacity at site is available, they can be delivered as a full tank

- The use of identical modular corners, built off-site as well as multiple smaller volume tanks to build the required storage volumes brings economies of scale to the tank farm with a much shorter time to build out and commissioning than a tank farm with few very large conventional tanks that must be built *in-situ*



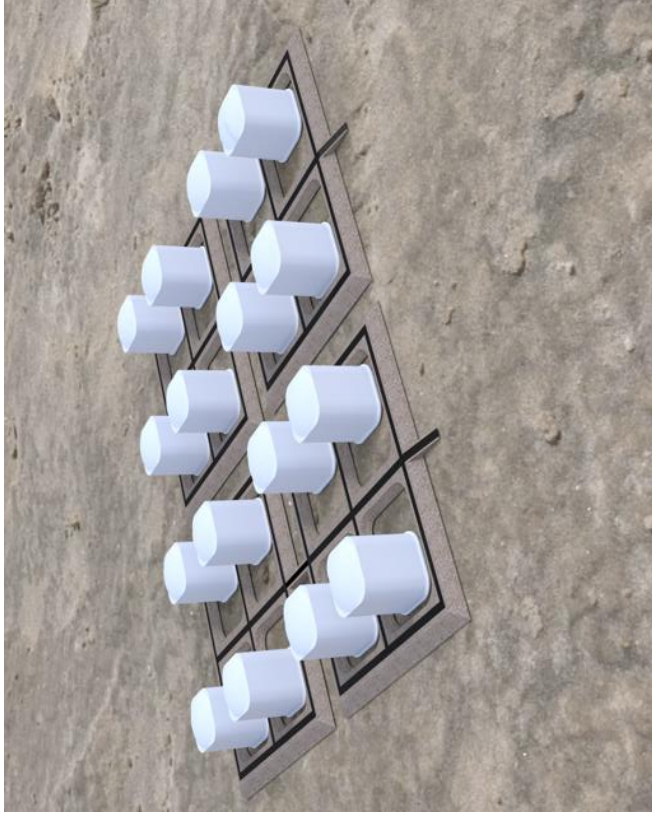
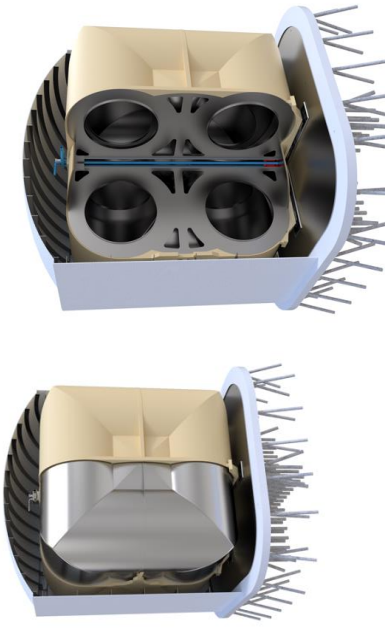
9Ni CDTs Land Storage Tank



- True Plug & Play
- Standardization of **Modules and Design**
- Dedicated Yard Leading to **significantly Higher Productivity & Quality since modular**
- Off-site Tank Pre-fab in Parallel to Foundation Construction
- On-site **commissioning of Tank only once** for all stake-holders together with other EPC partners
- **Can Ship in Modules as they are completed, more cost effective and logistically efficient**
- Reduced Man-Hours on-site compared to full containment concrete and **only have to transport 8 ~300t modules as they are completed at yard**
- **Total Weight of tank is expected to be under 3000t with higher safety margins than conventional land storage cylindrical containment tanks**

Regulatory Approvals

- Conformance (exceeds) to API 620/625 and NFPA59A
- OISD-STD-194 & CCOE-Nagpur can be met if Local Regulatory Authorities require conformance
- ABS Requirements (or equiv. for approval of modules at fabrication site)
- Our CDTs system was originally designed per IGC Code & ASME Section VIII



Specifications of CDTs Tanks

- Tank Type – Above Ground, Stand-alone Structural Single Containment
- Inner Tank – 9% Nickel Steel
- Roof – Integral with CDTs Tank
- Base – Integral with CDTs Tank
- Support – Extended Transverse & Longitudinal Frames on Lignostone Blocks
- Designed Seismic Loads: [Horizontal] - SSE 0.2g, OBE 0.1g; Vertical - $2/3$ * (Horizontal)
- Design Pressure Internal – 1 bar (0.1 Mpa)
- Design Vacuum – -0.005 bar (0.0005 Mpa)
- Design Temperature - -170 C
- Specific Gravity of LNG - 0.48
- Design BoR – 0.05%/day

Specifications of CDTs Tanks

- Tank Volume – 43,350 m³
- LNG Volume – 40,000 m³
- Tank Dimension – 37 m x 37 m x 37 m
- Max. Operating Level – 36.5 m*
- Min. Operating Level – 0.5 m*
- Insulation Type – 5 layer of PUF Blocks
- Insulation Thickness – 1100 mm
- Tank Height above Concrete – 2 m
- Overall Height 40 m

*needs to be confirmed with Gas Engineering Partner

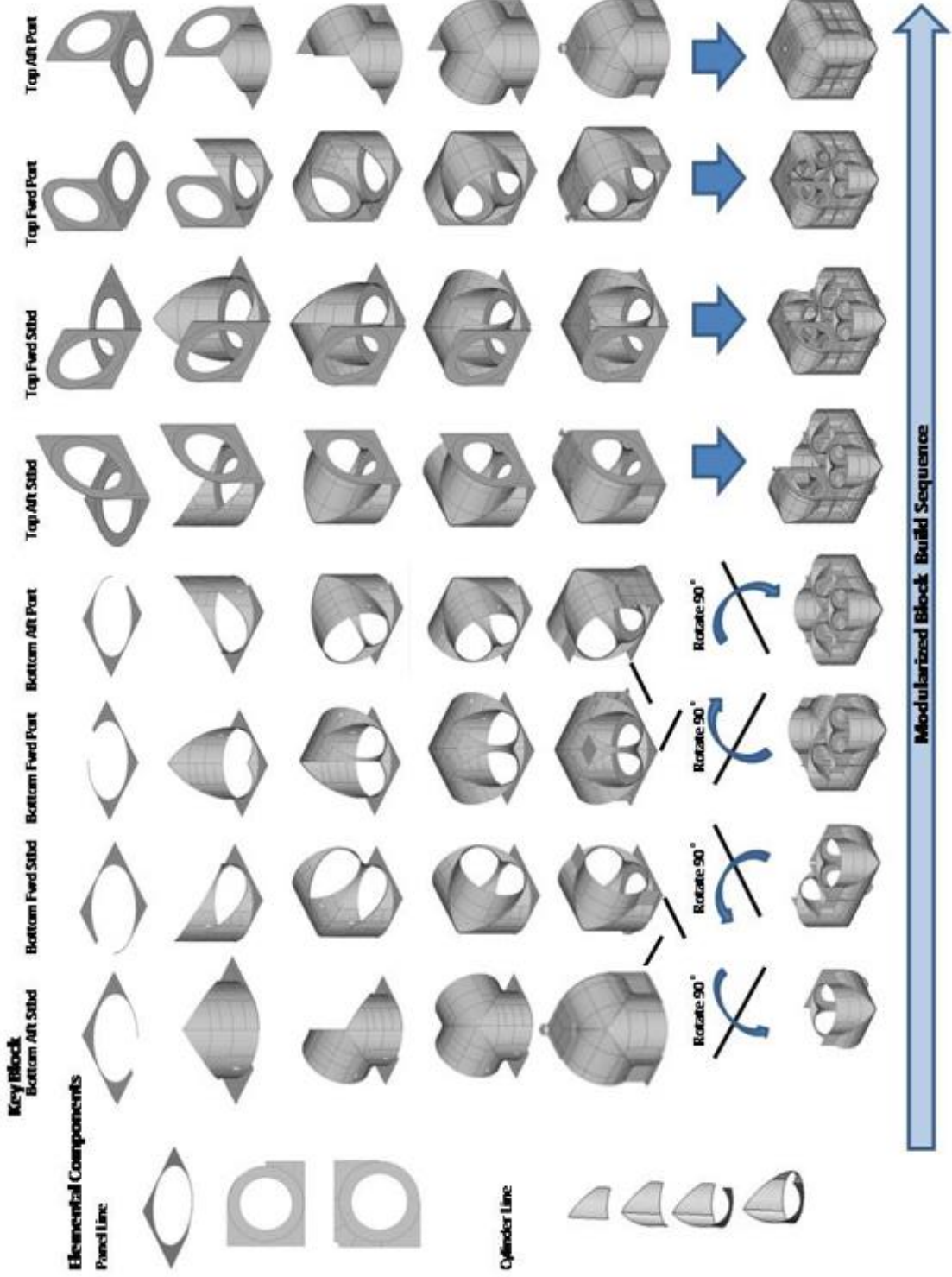
Specifications of CDTs Tanks

- Outer Tank – A36 Steel Enclosure
- Enclosure Dimensions – 40 m x 40 m x 43 m
- Enclosure Thickness – 0.75 mm
- Hydrostatic Test Load – 1.25 x full head of LNG
- 1 m of LNG = 0.48 m of H₂O
- Hydrostatic Test Load = 1.25 x 0.48 = 0.6 * Height of liquid head in H₂O
- Concrete Support Design Load – 3 times tank weight
- Limestone Support Load – 3 times Block Load
- Differential Settlement Perimeter – 1:500
- Differential Settlement Center to Edge – 1:300
- Planar Tilt Angle – 0.002 radians

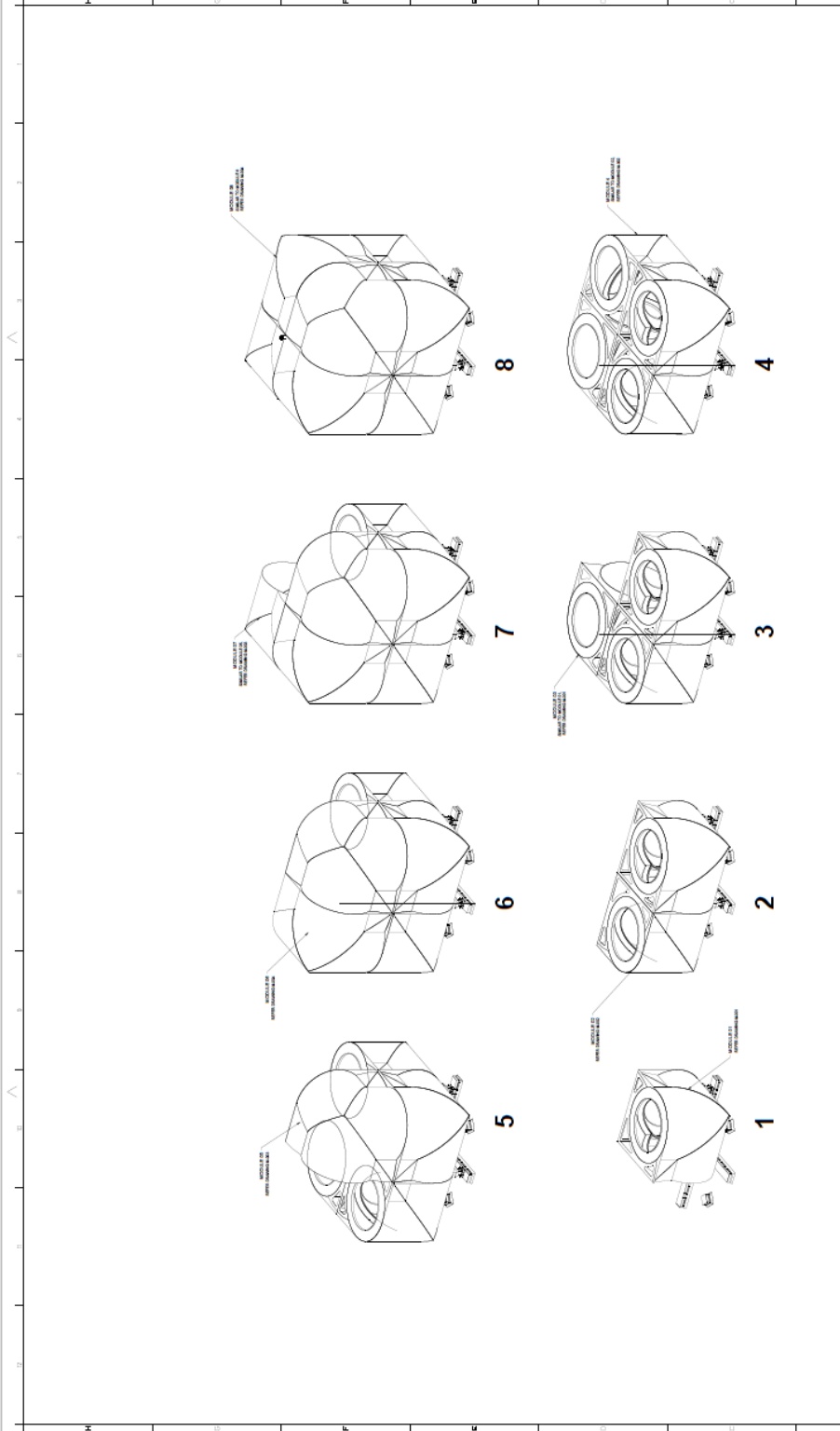
Preliminary Specifications for Concrete Base Slab

- G30 ~ G35 Concrete Slab on piles
- Pile Spacing and Depth (~25m) will depend on geo-mechanics and seismicity of site
- Slab height estimated at 500mm ~ 800mm
- Project Site Environmental Conditions may effect Design somewhat but not expected to be significant

CDTS Manufacturing Methodology



9Ni Single Containment CDTs



ASSEMBLY SEQUENCE

| | | | |
|--|-------------|----------------------------|----------|
| REV | DESCRIPTION | UNLESS OTHERWISE SPECIFIED | DATE |
| | | | |
| ALT AIR ENGINEERING INC. 1530 S. 10th Street Troy MI 48068, United States | | | |
| PRODUCT: CDTs LAND STORAGE 43350 m ³ | | | |
| TITLE: TANK ASSEMBLY | | | |
| COMPANY NO. | DRAWING NO. | SCALE | UNITS |
| A-001 | 2/2 | A1 | 1-400 mm |
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9Ni single Containment CDTs

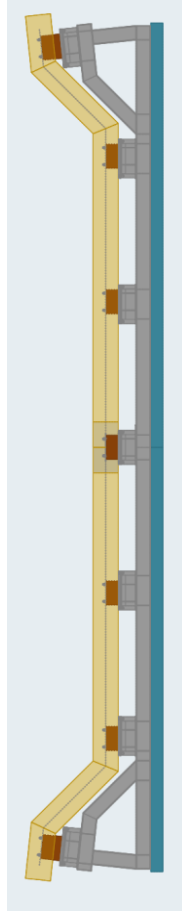
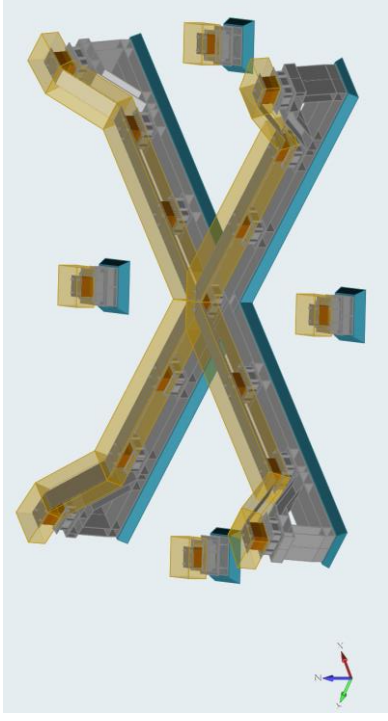
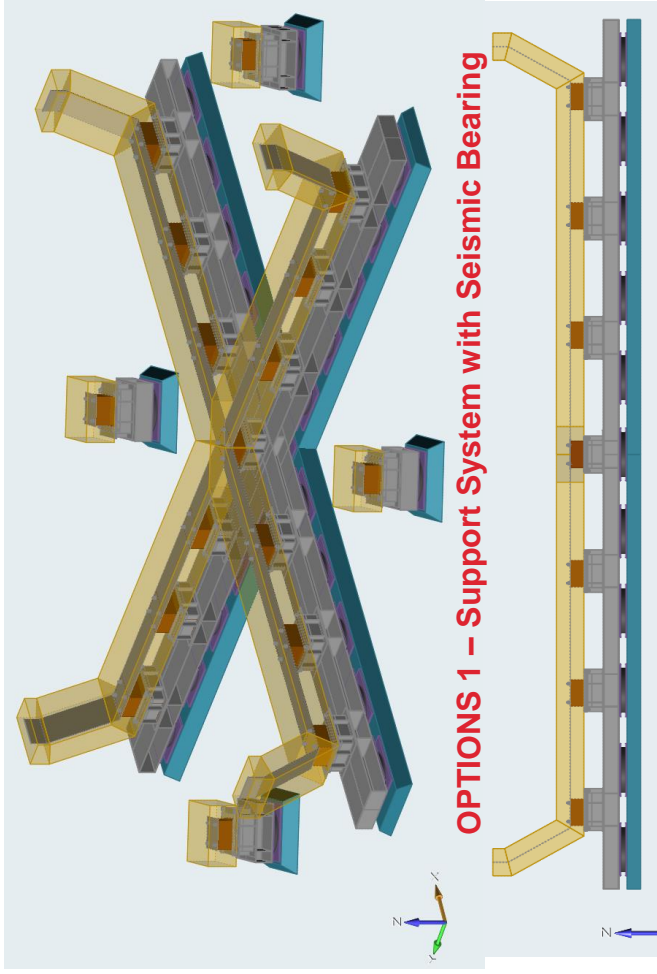


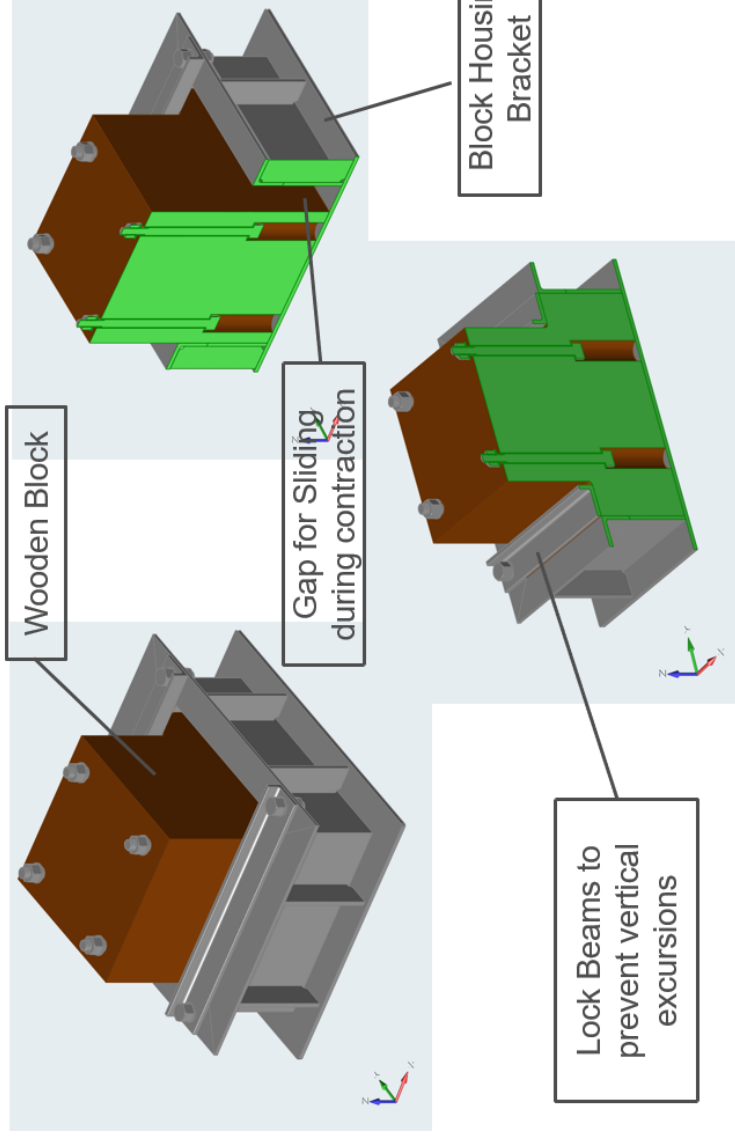
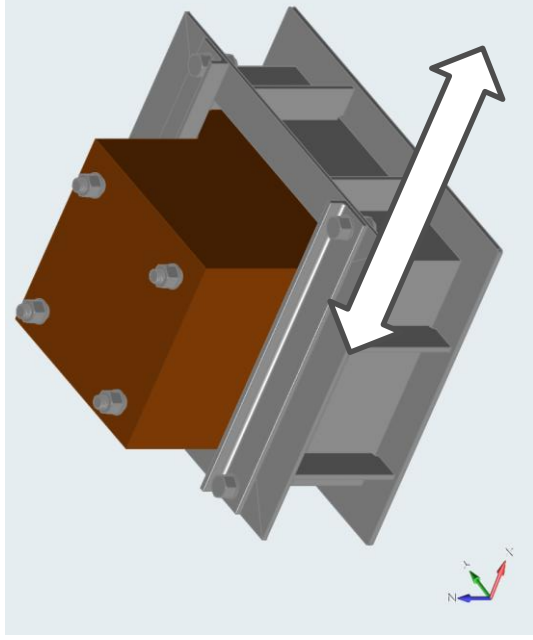
Figure 11. Para LING J204 130,000lbs with 216 Triple Pseudostatic bearing (courtesy of EPSC)



Figure 12. Jackson LING Terminal provided in elastomeric bearing.

Sliding Support Mechanism

- Limestone Blocks are attached to the CDTS Bottom Support via 4 bolts
- The blocks sit in support housing per our marine variant that allow excursions in one direction to accommodate contraction



Insulation System

5.2 Calculation of Heat & BOR

In ANSYS, the heat is calculated through the formula below

$$q_{total} = q_{qsz} \cdot 4$$

where q : Total heat loss

q_{qsz} : heat calculated by the quarter size model

BOR is calculated as below

$$BOR = \frac{q_{total} \cdot 3600 \cdot 24}{h_{fg} \cdot V \cdot \rho_m} \cdot 100\%$$

where q_{total} : Total heat loss

V : Total cargo volume of a tank (43350 m³)

h_{fg} : Latent heat of pure methane (511kJ/kg)

ρ_m : Density of pure methane (425kg/m³)

Results are summarized as below.

| Thickness of TiG PU panel [mm] | BOR target [/day] | Total heat loss [W] | Calculated BOR [/day] | Safety margin* |
|--------------------------------|-------------------|---------------------|-----------------------|----------------|
| 1000 | 0.05% | 51064 | 0.0469% | 6.27% |
| 700 | 0.08% | 77560 | 0.0712% | 11.03% |
| 580 | 0.10% | 96820 | 0.0889% | 11.15% |
| 380 | 0.15% | 146148 | 0.1341% | 10.58% |

*) Safety Margin = (BOR Target - Calculated BOR) / BOR Target

Table 3 Heat results summary

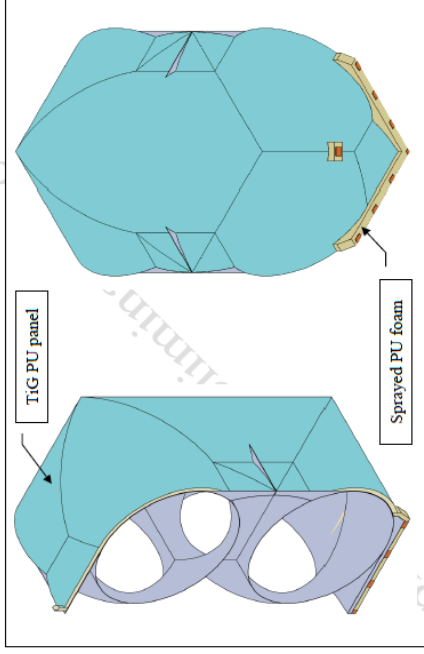


Figure 1 Cargo tank and insulation system

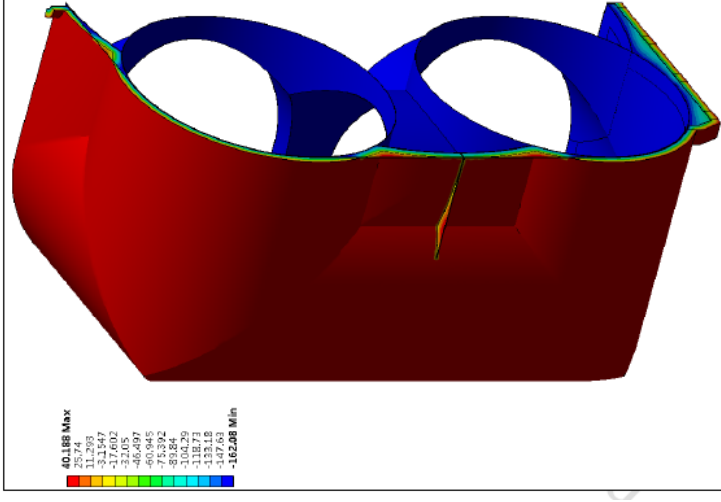


Figure 2 Temperature distribution in a typical case

4. Boundary Condition

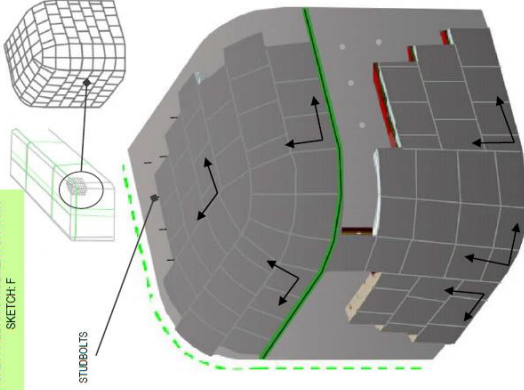
| Area | Type | Temperature [°C] | Heat transfer coefficient [W/m ² K] |
|-------------------|------------|------------------|--|
| Hold space | Convection | 40 | 5.8 |
| Bottom of support | Conduction | 40 | - |
| Inside Tank | Convection | -161.5 | 500 |

Table 2 Boundary condition

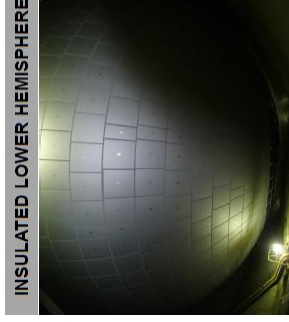
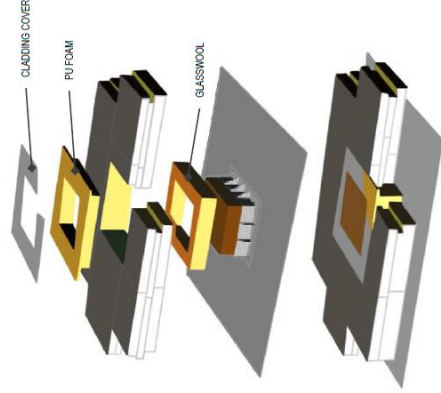
Radiation heat transfer is not considered.

Insulation System

TYPICAL PANEL ARRANGEMENT ON TANK SKETCH F

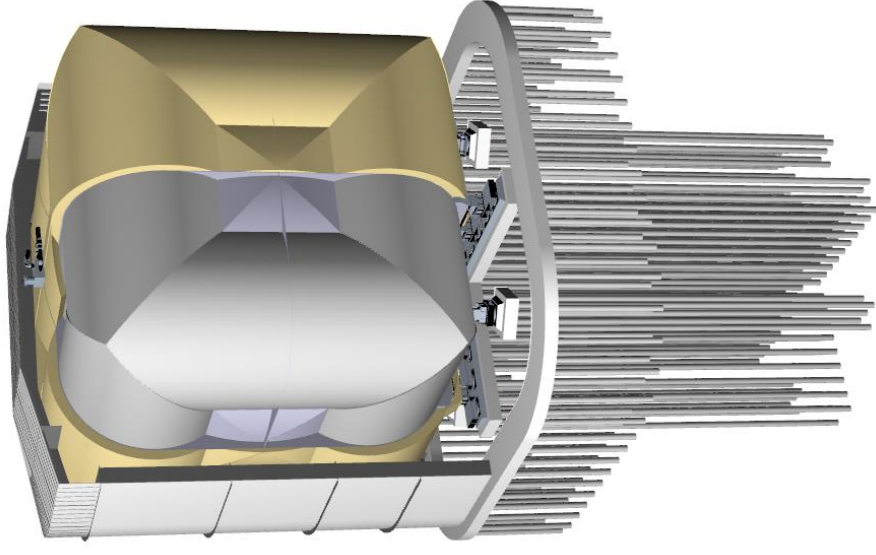
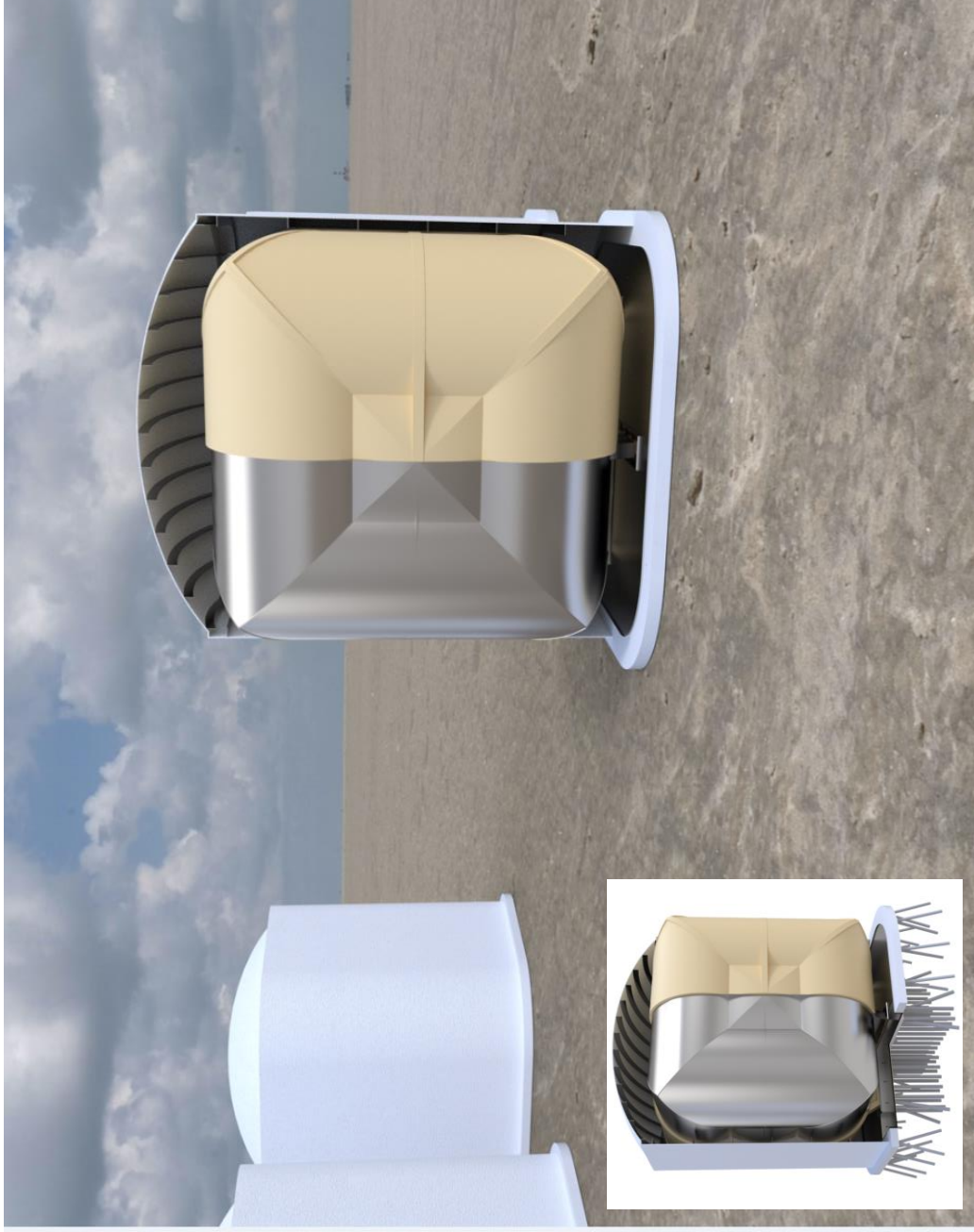


TYPICAL SUPPORT INSULATION ARRANGEMENT SKETCH G

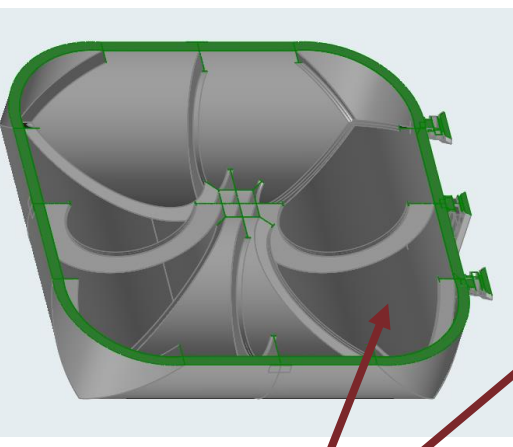
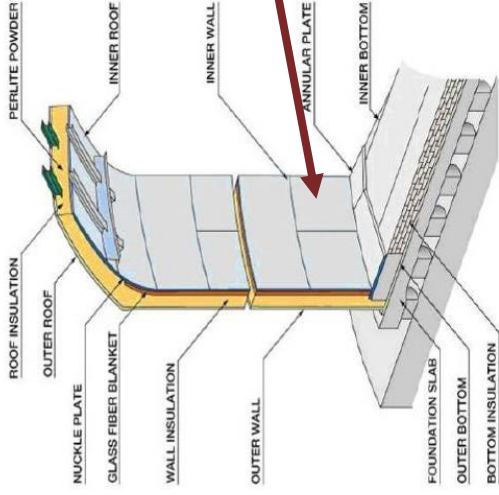


The entire TiG insulation system has been rigorously tested under cryogenic conditions under strict class (LR) control and verification. The system was dismantled and inspected while in fully frigid condition in order to discover any weakness or problems. The class could witness that the integrity of the system was fully satisfactory. This testing was completed in 2007 after a long testing program.

CDTS for Land LNG Containment



CDTS Tanks vs Cylindrical Tanks



$$\sigma_{\theta} = [Pr. \times \text{Dia.}] / (2t)$$

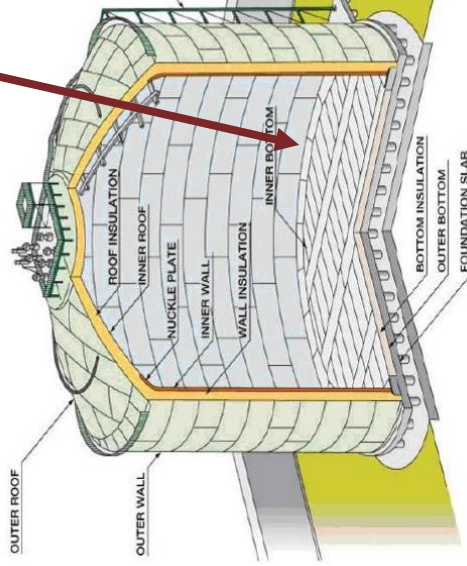
$$\sigma_a = 0.5 \times \sigma_{\theta}$$

350 MPa

200 MPa

40K Tank Comparison

| | Cylindrical 9Ni Single Containment | ALTAIR 9 Ni CDTS |
|------------------------------|--|------------------------|
| Inner Shell (t) | 640 | 2400 |
| Shell Thickness | | Tank Shell (t) |
| Top (mm) | 10 | 15 |
| Bottom (mm) | 25 | 30 |
| Base Support (t) | | 60 |
| Concrete (t) | 990 | Base Cradle (t) |
| Steel Grillage (t) | 212 | |
| Insulation | Perlite | PUF (aged) |
| Density (kg/m ³) | 130 | 43 |
| Thickness (m) | 1.275 | 1.0 |
| K (W/mk) | 0.047 | 0.0142 |
| Insulation (t) | | |
| Vertical Wall | 467 | |
| Roof | 50 | |
| Base | 502 | |
| Total Insulation | 1019 | 298 |
| Weight (t) | | |



SABINE PASS – 2 Storage Tanks Shut-Down due to Leakage

NATURAL GAS

Feds order partial shutdown at Cheniere LNG export site

Jenny Mandel and Mike Soraghan, E&E News reporters
Energywire: Monday, February 12, 2018



Tanks store liquefied natural gas at Cheniere Energy Inc.'s Sabine Pass LNG terminal. Roy Luck/Flickr

Federal regulators have ordered Cheniere Energy Inc. to shut down part of its liquefied natural gas export terminal in Louisiana after multiple leaks from storage tanks were discovered in late January.

The Pipeline and Hazardous Materials Safety Administration (PHMSA) announced Friday that it had ordered Cheniere to shut down two tanks at its Sabine Pass facility, which in 2016 was the first of several U.S. LNG export projects under development to start shipping gas.

PHMSA allowed the company to continue importing and exporting gas and use three other LNG storage tanks at the site.

PHMSA is investigating a Jan. 22 incident in which workers discovered that LNG had been leaking into a containment ditch around a storage tank. Further inspection revealed that natural gas vapors were leaking from 14 points around the base of a second LNG storage tank.

Sabine Pass has five LNG storage tanks; all were designed by Mitsubishi Heavy Industries Ltd. Three of the tanks were built by Matrix Service Inc. between 2005 and 2008 and were placed into service in 2008, while the other two were built by Zachry Industrial Inc. and put into service in 2009, according to PHMSA.

Plymouth LNG- 1 Storage Tank Shut-Down due to Leakage from Shrapnel Puncture

Aerial view taken shortly after the failure. Looking South toward Columbia River.



What happened at Plymouth LNG?

LNG is simply **natural gas** that has been refrigerated to -260 degrees Fahrenheit. At this temperature, natural gas becomes liquid and condenses to 1/600th of the space it occupied as a gas. Cryogenic refrigeration allows plant operators to store large quantities of natural gas in tanks that could not otherwise hold such a large volume. If liquid natural gas is not kept extremely cold, it turns back to a gas. When a utility needs to use the LNG it has stored, workers simply pipe LNG out of the refrigerated storage tank and return its temperature to normal.

Plymouth is the largest LNG storage facility in the Pacific Northwest, boasting two **14.6 million gallon** storage tanks. Shortly after 8:00 a.m. on March 31, 2014, gas processing equipment at Plymouth LNG exploded into a towering, **mushroom-shaped cloud**. Nearby residents **saw flames shoot into the air**, and people living **three to six miles** from the plant could feel the explosion. The blast sent **250 pounds of debris and shrapnel** flying as far as 300 yards, damaging buildings and equipment and puncturing one of the large LNG storage tanks.

Shrapnel injured four of the **fourteen** employees on duty, and a fifth worker was **hospitalized** for burns. Debris from the blast also **damaged the main rail line** on the north side of the Columbia River, which delayed more than 40 trains before BNSF Railway completed repairs on Tuesday afternoon. (Sightline has **previously calculated** that on a typical day, several **notoriously combustible** oil trains traverse the route that passes by the Plymouth LNG facility.)

In the hours that followed, 14.3 million cubic feet of gas spewed from **a large gash** in the storage tank and other damaged equipment on site. **Video and photos** show vaporized LNG escaping from a puncture low on the tank. Williams **says** the damaged tank was only one-third full.

Spill of LNG won't count as LNG spill

In addition to not being considered a threat to public safety, the Plymouth LNG spill is not even considered an LNG spill. The data retrieved from PHMSA's website states that even though 14,270 barrels (599,340 gallons) of LNG spilled, no LNG was lost. When Sightline contacted PHMSA about the apparent error in the report, an agency official responded that in fact no LNG was spilled at all. The official clarified that **evaporated** natural gas was spilled, not **liquid** natural gas.

Aerial view taken shortly after the failure. Fires still burning. Perlite insulation leakage from the penetrated outer LNG-1 storage tank. Control room lower left.



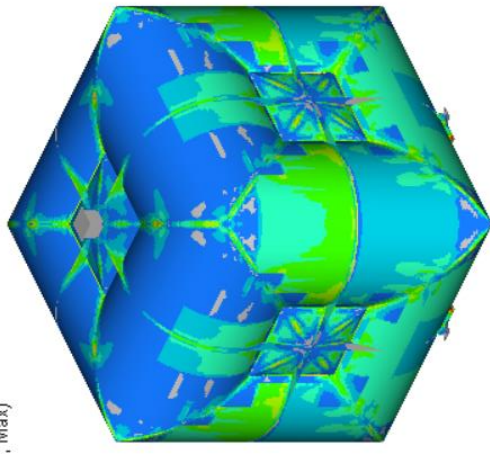
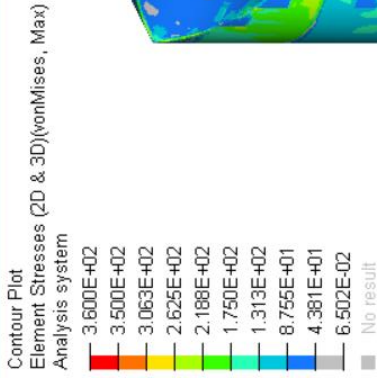
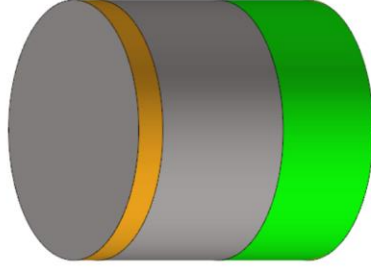
Tank Technology Selection Study For the Hong Kong LNG Terminal

- Because much on an in-ground is covered with soil, tank inspection and monitoring is difficult and possible problems may go unnoticed. When problems do occur, it is much harder to repair them. For example, the in-ground tanks in Yung-An (Taiwan) have been leaking for years, but due to the difficulty in pinpointing the leak location and accessibility, have elected not to try to repair the leak.

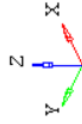
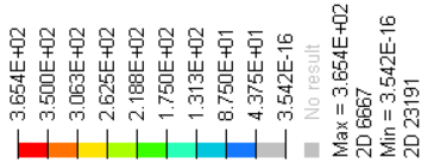
9Ni Single Containment CDTs vs Cylindrical

Loading

1. Hydrostatic load (25% margin)
2. gravity load
3. pneumatic load (25% margin)

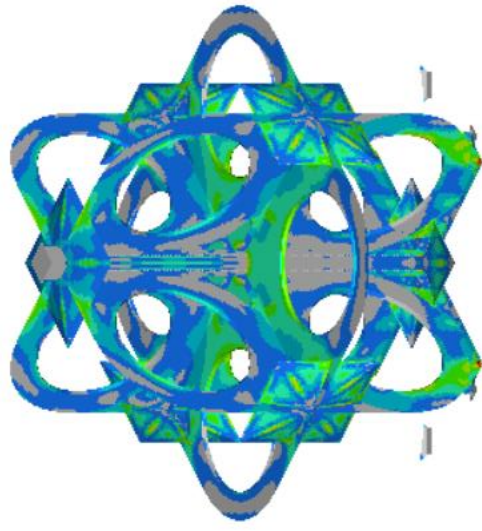
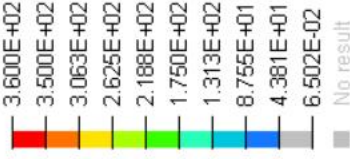


Contour Plot
Element Stresses (2D & 3D)(vonMises, Max)
Analysis system



Z

Contour Plot
Element Stresses (2D & 3D)(vonMises, Max)
Analysis system





Altair

HyperWorks®

**CDTS 40K m³ :
Land Storage Tank Stress Analysis**



Altair

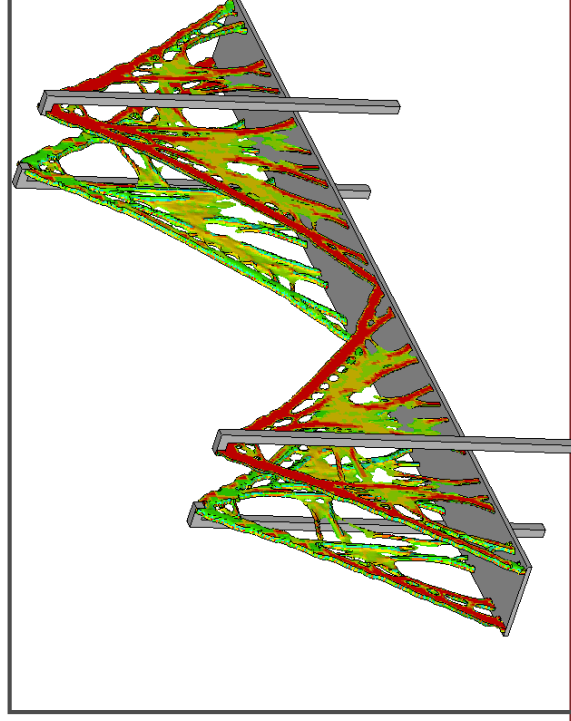
**Eng Ban-Wee, Principal Naval
Architect, Altair Engineering, Inc**

Concept Level Optimization Types

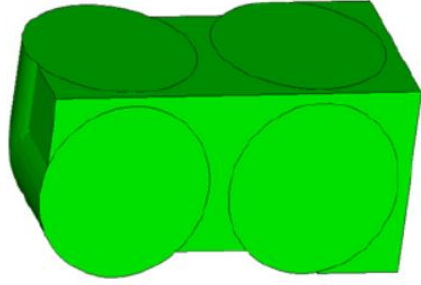
Topology Given a design envelope, topology optimization finds the optimum material placement within that space according to the constraints and objective

Topography Given a shell structure, topography optimization creates a bead pattern from the elements that meets the constraints and objective

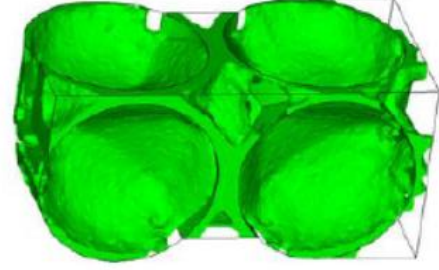
Free Size Given a shell structure, free size optimization finds the optimum thickness on an element-by-element basis that meets the constraints and objective



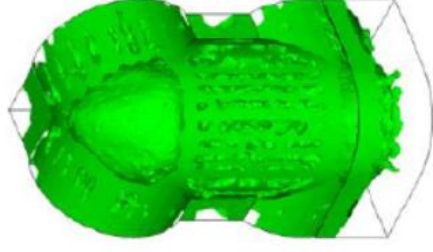
Optimization process for CDTs



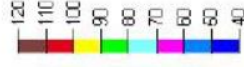
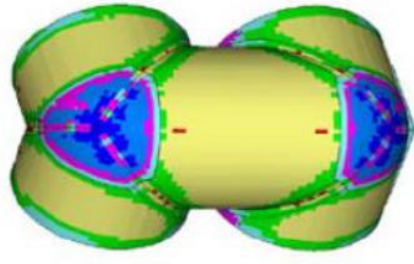
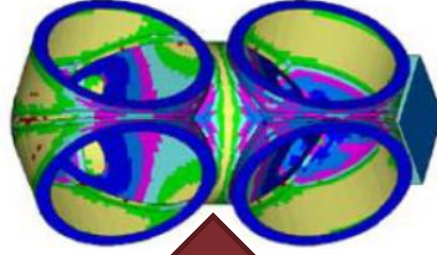
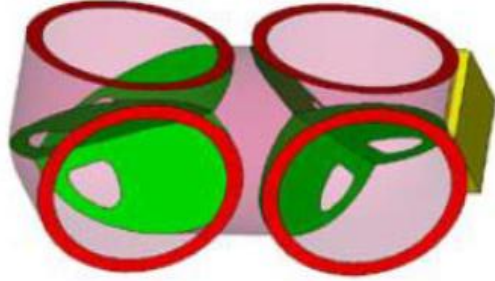
Design space



Load path from Optimization



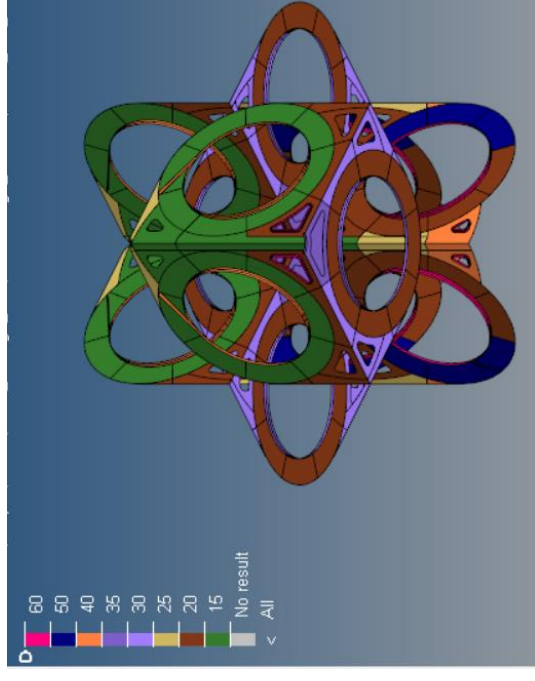
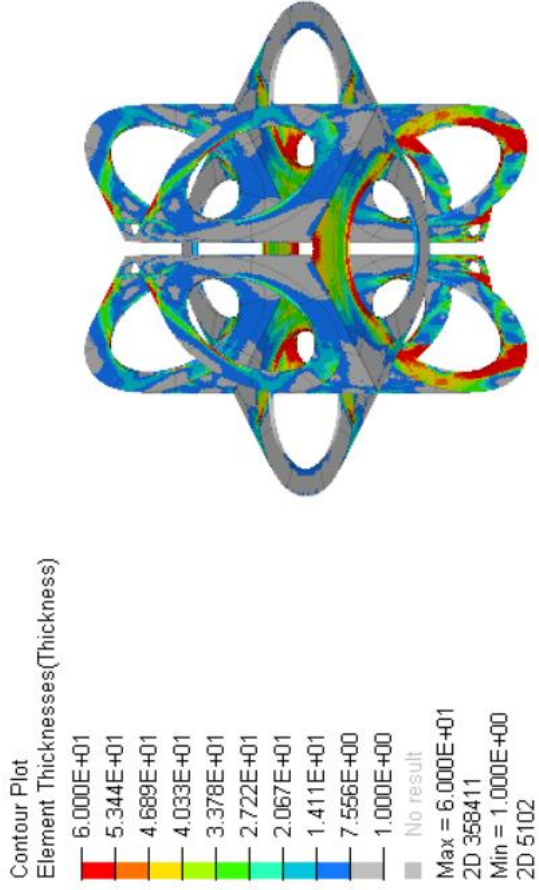
Load path from Optimization



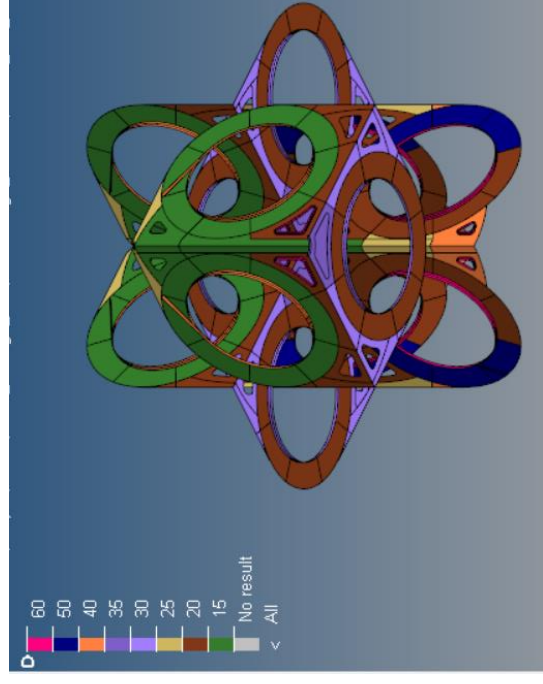
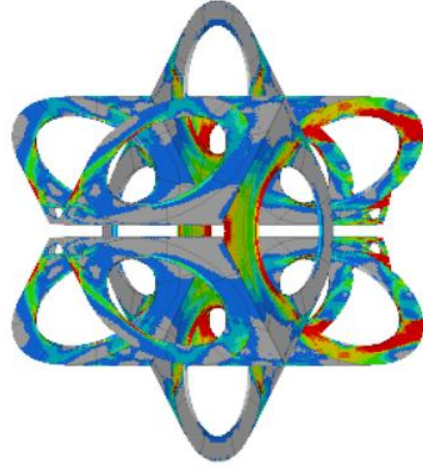
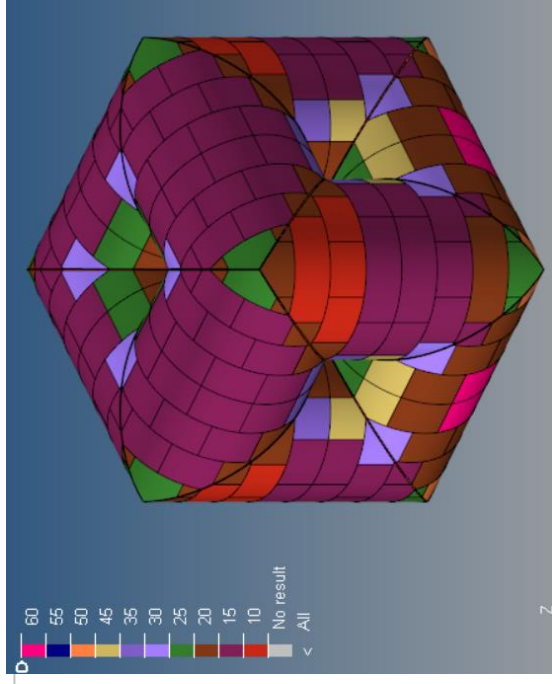
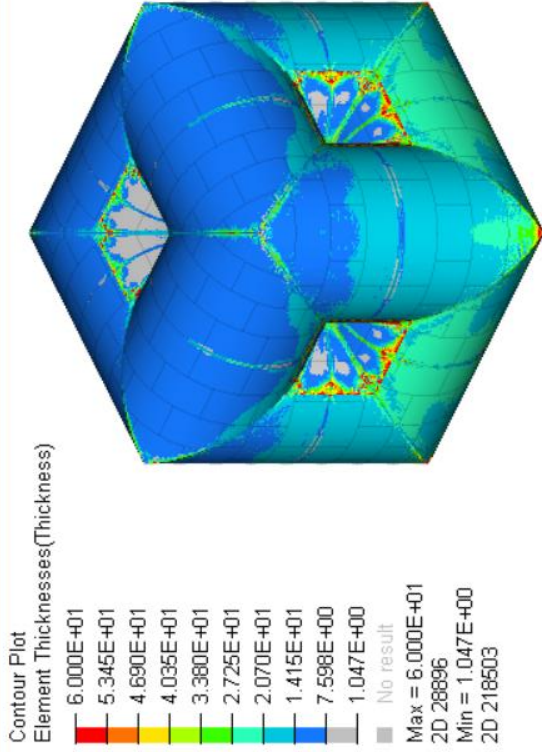
Free size thickness

Optimization process for land storage tank

- **Constrain the mass and stress of the structure**
- **Objective is maximum the stiffness(rigidity)of the structure**



Optimization Process

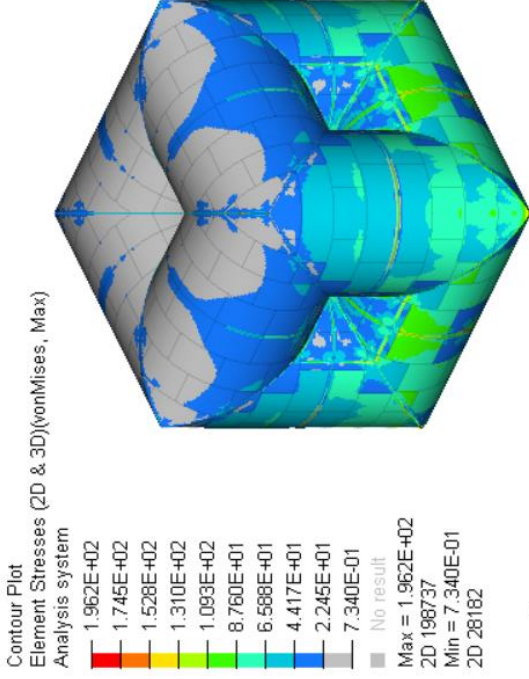
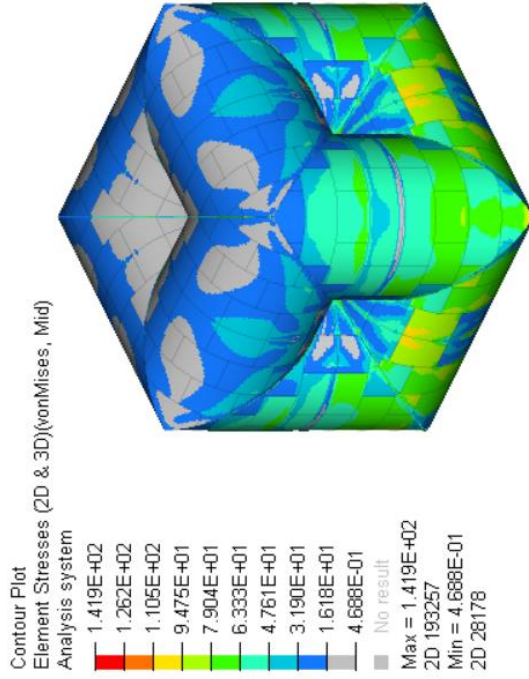


Stress criteria :

- Using ASME pressure vessel code for the design standard

| | IGC Stress Allowables | Nominal | Local |
|--|-----------------------|---------|-------|
| Allowable membrane Stress (MPa) | | 212 | 318 |
| normal pressure loading or plate structures under in-plane loading) | | | |
| Allowable Total Stress (MPa) | | 318 | 318 |
| (i.e., structural segments that are subjected to membrane and bending loads) | | | |

API Rules 75% of min yield@586 = 440 Mpa

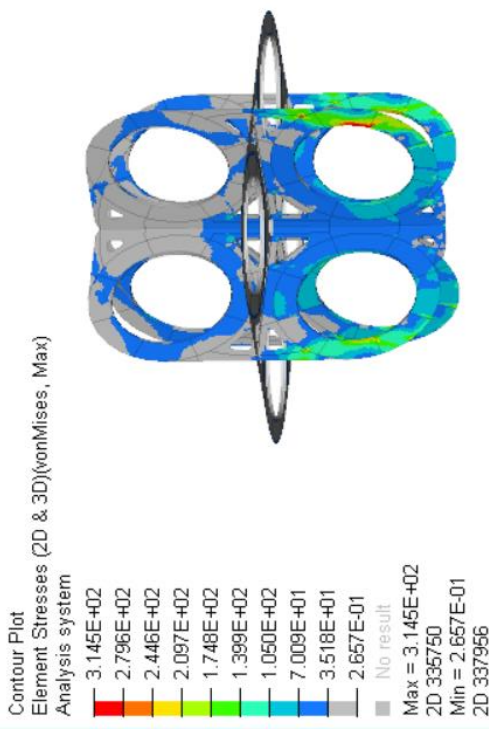
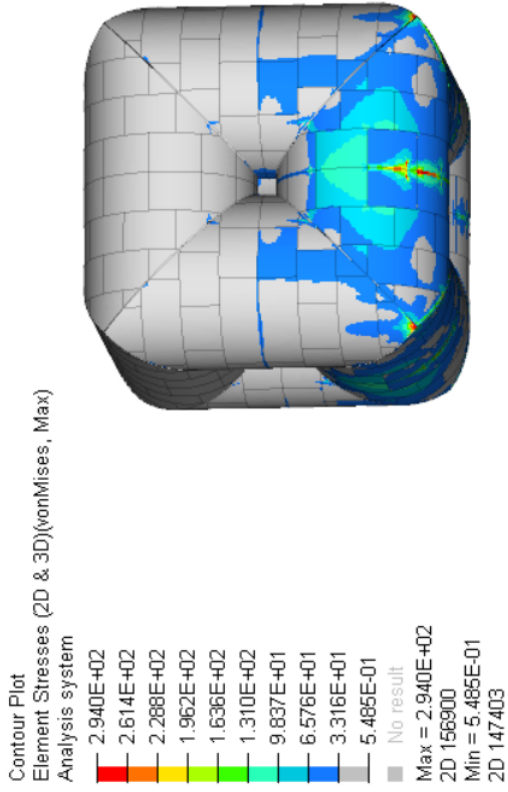


Membrane stress

Von mises stress

Load combination f:

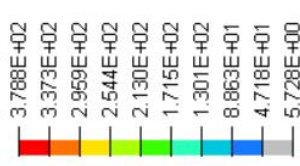
- Seismic load + storage liquid force



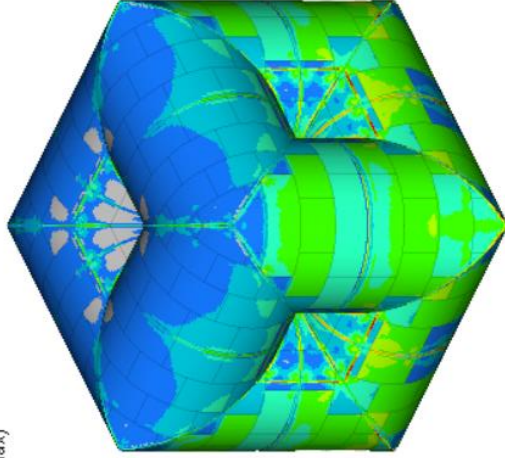
Load combination g:

- hydrostatic test + dead load

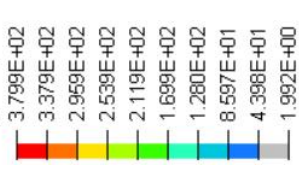
Contour Plot
Element Stresses (2D & 3D)(vonMises, Max)
Analysis system



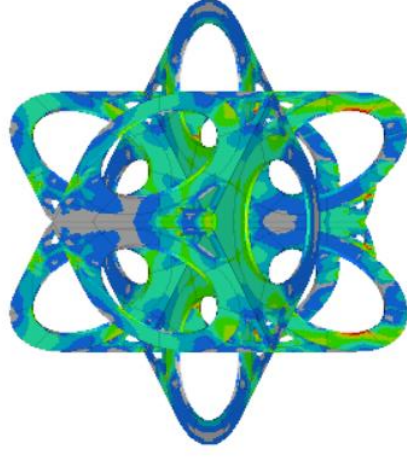
Max = 3.788E+02
2D 155422
Min = 5.728E+00
2D 218988



Contour Plot
Element Stresses (2D & 3D)(vonMises, Max)
Analysis system



Max = 3.799E+02
2D 336548
Min = 1.992E+00
2D 9131278

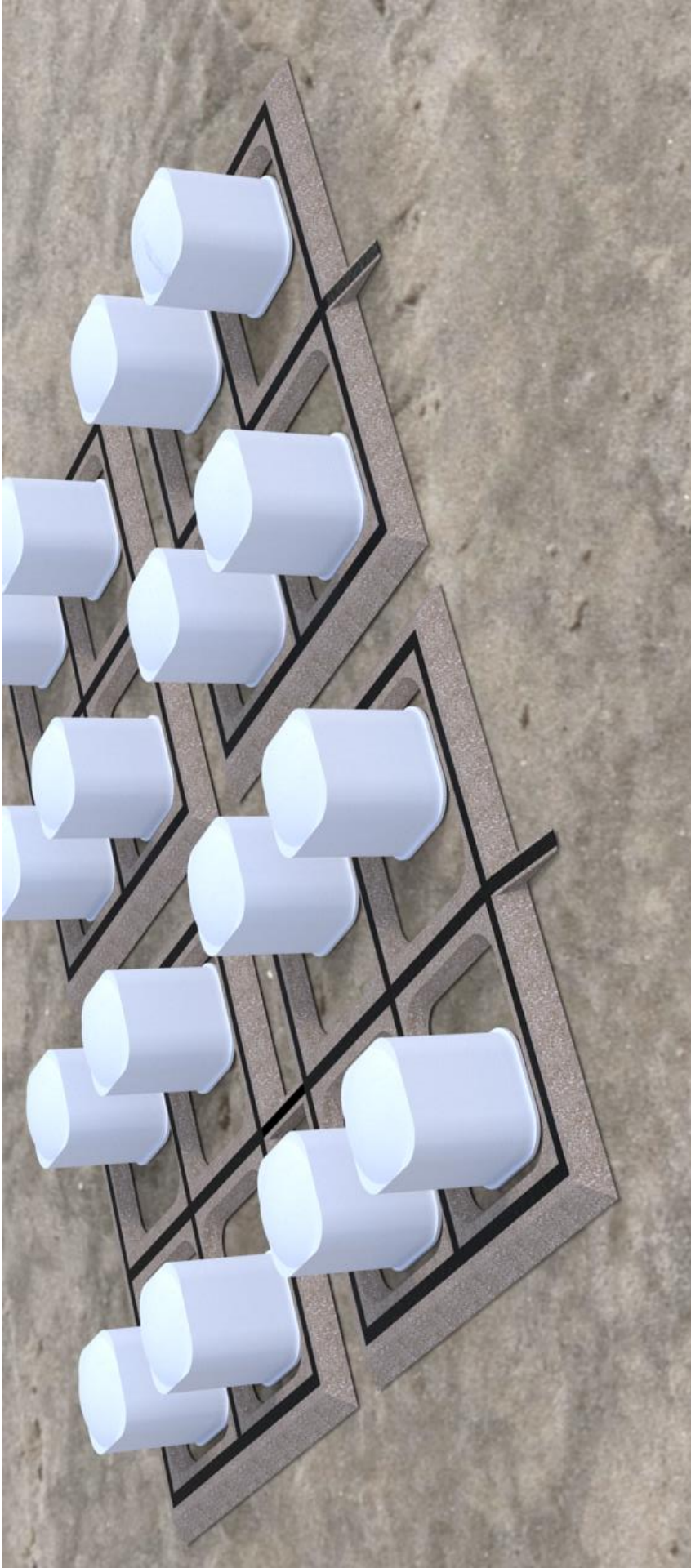


Von Mises Stress summary

| Load | Tank shell stress (MPa) | Bulkhead stress (MPa) |
|---|-------------------------|-----------------------|
| a) $D_L + P_g + P_I$ | 175 | 221 |
| b) $D_L + W_L + 0.7P_g$ | 40 | 66 |
| c) $D_L + W_L + 0.4P_v$ | 80 | 91 |
| d) $D_L + P_v + 0.4(L_r \text{ or } S)$ | 183 | 144 |
| e) $D_L + 0.4P_v + (L_r \text{ or } S)$ | 76 | 75 |
| f) $D_L + 0.7P_g + P_I + E + 0.1S$ | 294 | 315 |
| g) $D_L + H_t$ | 379* | 380* |
| h) $D_L + L_s$ | 39 | 64 |
| i) $D_L + L_p + P_g + P_I$ | 175 | 221 |

*using >75% of yielding stress

| | IGC Stress Allowables | Nominal | Local |
|--|-----------------------|---------|-------|
| Allowable membrane Stress (MPa) | | 212 | 318 |
| normal pressure loading or plate structures under in-plane loading) | | | |
| Allowable Total Stress (MPa) | | 318 | 318 |
| (i.e., structural segments that are subjected to membrane and bending loads) | | | |



CDTS FABRICATION, ERECTION & OUTFITTING AND PROCESS SYSTEMS

SHIVARAJH • Sr Project Engineer • July 2018

CONTENTS

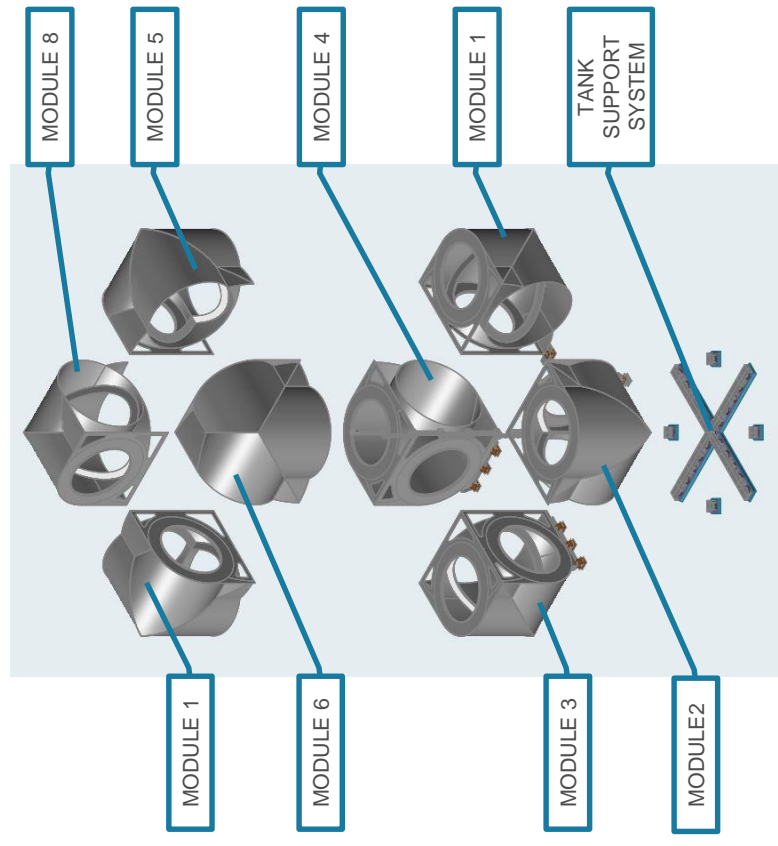
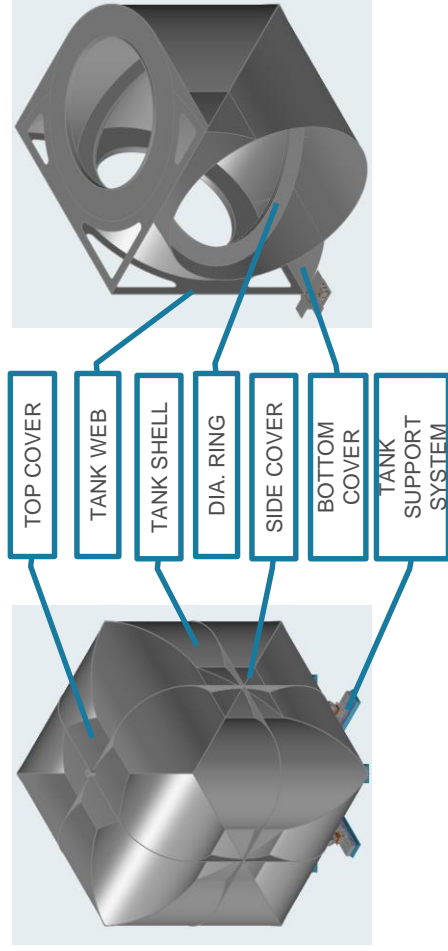
- **CDTS MODULAR ASSEMBLY**
 - TANK PARTS & MODULES
 - MODULE FABRICATION
 - TANK ERECTION
- **INSULATION SYSTEM**
 - CDTS INSULATION
 - TI CALLENBERG FOR INSULATION
 - INSULATION SYSTEM
 - INSULATION INSTALLATION
- **PROCESS FOR LAND STORAGE**
 - SEQUENCE OF OPERATION
 - PROCESS FLOW DIAGRAM



CDTS MODULAR ASSEMBLY

TANK PARTS & MODULES

- **CDTS comprise of eight (8) modules**
- **Identical / Mirror to each other**
- **Enables modules fabricated at yard and erected on site**



MODULE FABRICATION

- TOP MODULES



- BOTTOM MODULES





TANK ERECTION

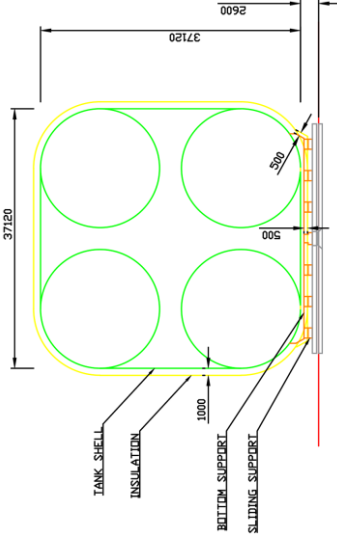
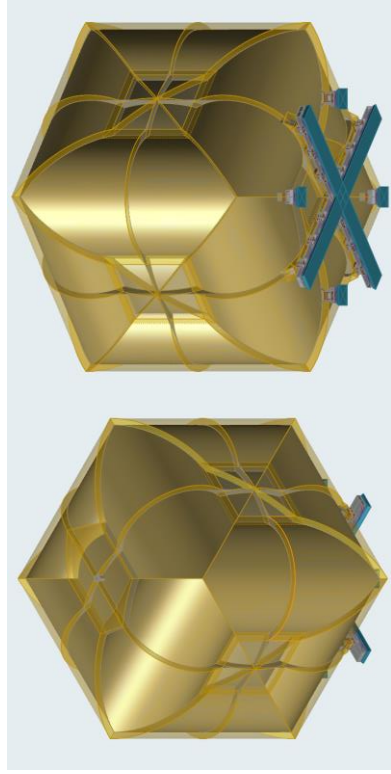


Altair

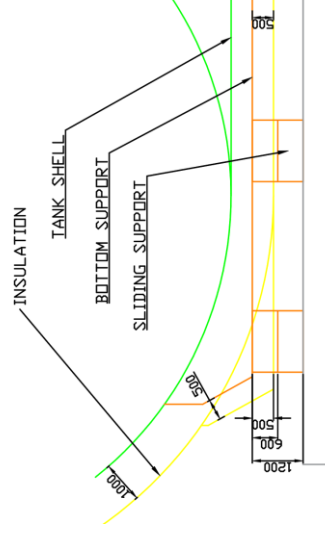
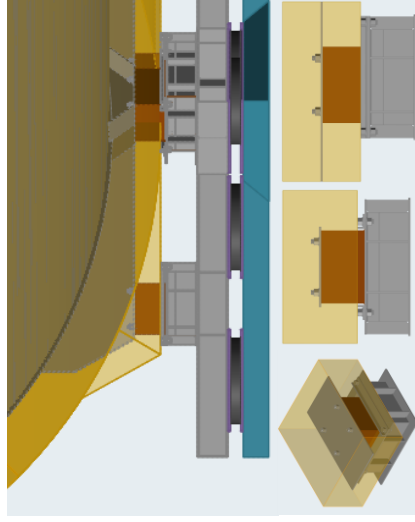
INSULATION SYSTEM

CDTS INSULATION

• TANK INSULATION



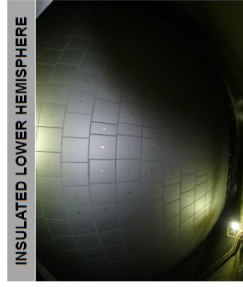
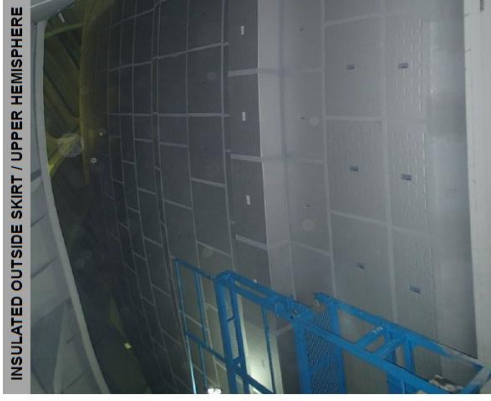
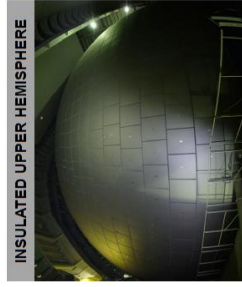
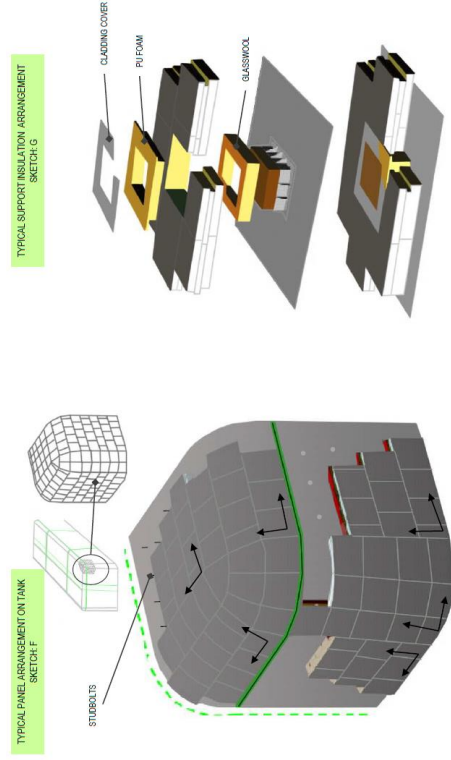
• SUPPORT



• INSULATION DETAILS

- BoR target : 0.05%/day
- Insulation System : PUF system
- Insulation density : 43 kg/m³
- Tank volume: 43,000 m³
- The tank surface : 7819 m²

TI CALLENBERG FOR INSULATION



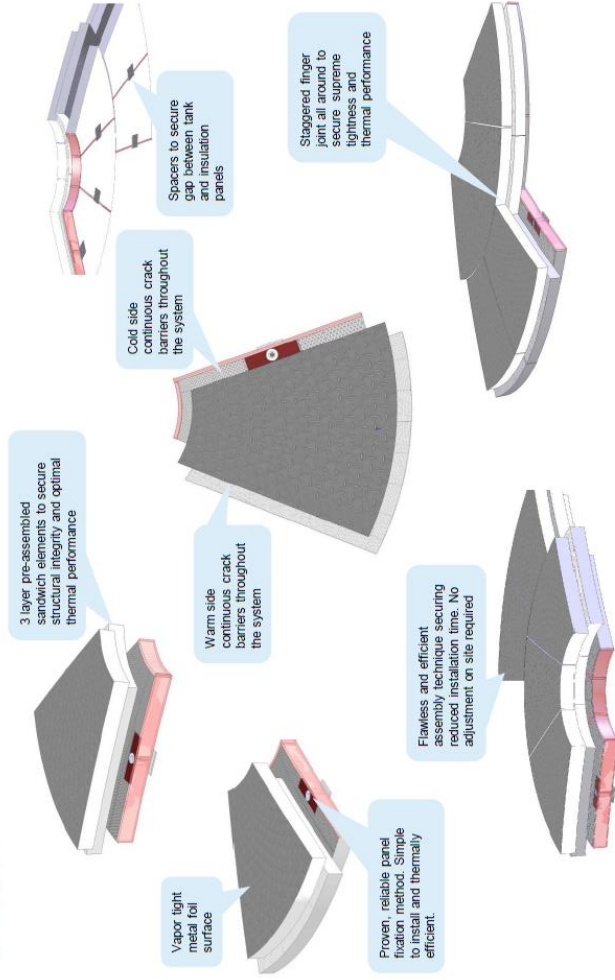
The entire TIG insulation system has been rigorously tested under cryogenic conditions under strict class (LR) control and verification. The system was dismantled and inspected while in fully frigid condition in order to discover any weakness or problems. The class could witness that the integrity of the system was fully satisfactory. This testing was completed in 2007 after a long testing program.

INSULATION SYSTEM



TIG INSULATION SYSTEM BASIC DESIGN

A COMPLETE, PREFABRICATED AND TAILOR MADE CRYOGENIC INSULATION SOLUTION WITH PROVEN TRACK RECORD. THE SYSTEM IS EASY AND EFFICIENT TO INSTALL BASED ON A TRANSPARENT INSTALLATION TECHNIQUE WHICH SECURES HIGH QUALITY.

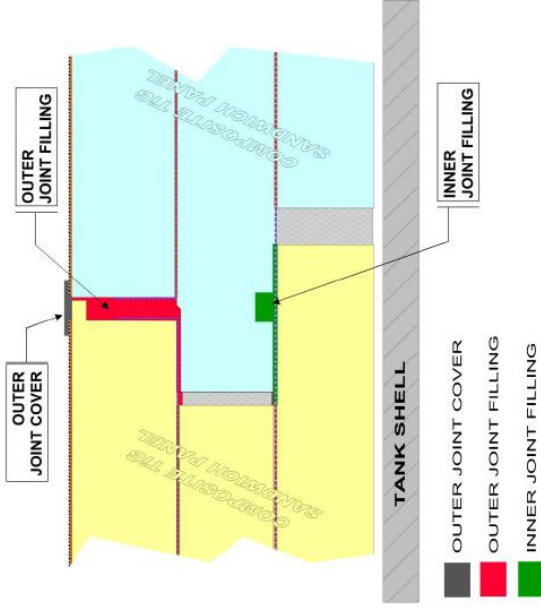


Part of Wilhelmssen Maritime Services, a With. Wilhelmssen group company

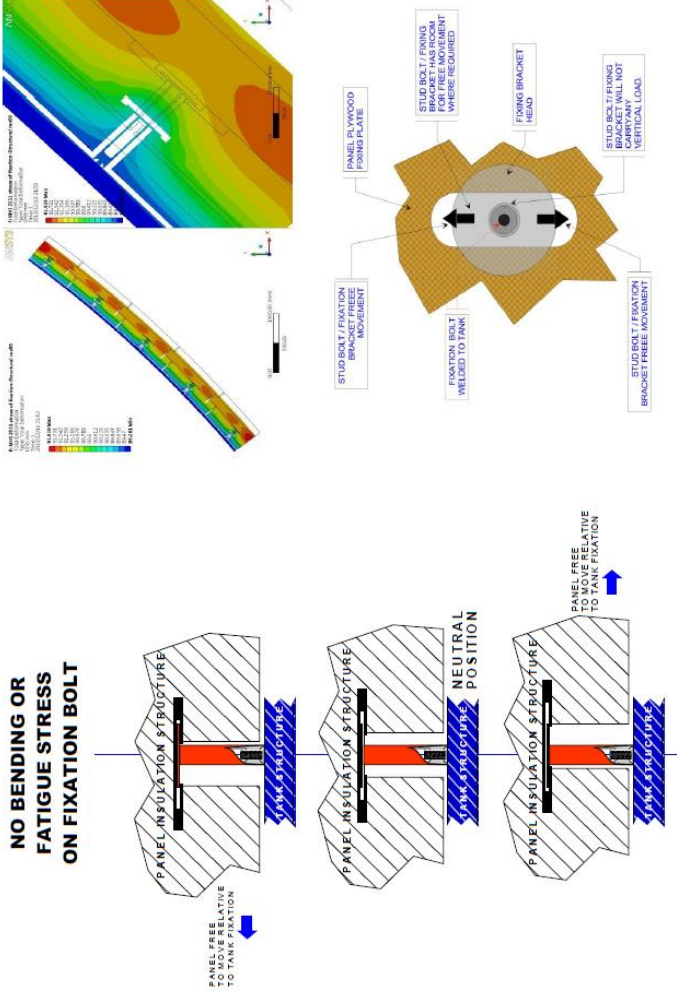
INSULATION SYSTEM (CONT')

TIG SYSTEM PROVEN PANEL JOINT FILLING TECHNOLOGY FOR IMPROVED INSULATION SYSTEM TIGHTNESS AND ENHANCED THERMAL EFFICIENCY

TIG PANEL STAGGERED TONGUE AND GROOVE JOINT DESIGN SECURES SUPERIOR TIGHTNESS AND THERMAL EFFICIENCY



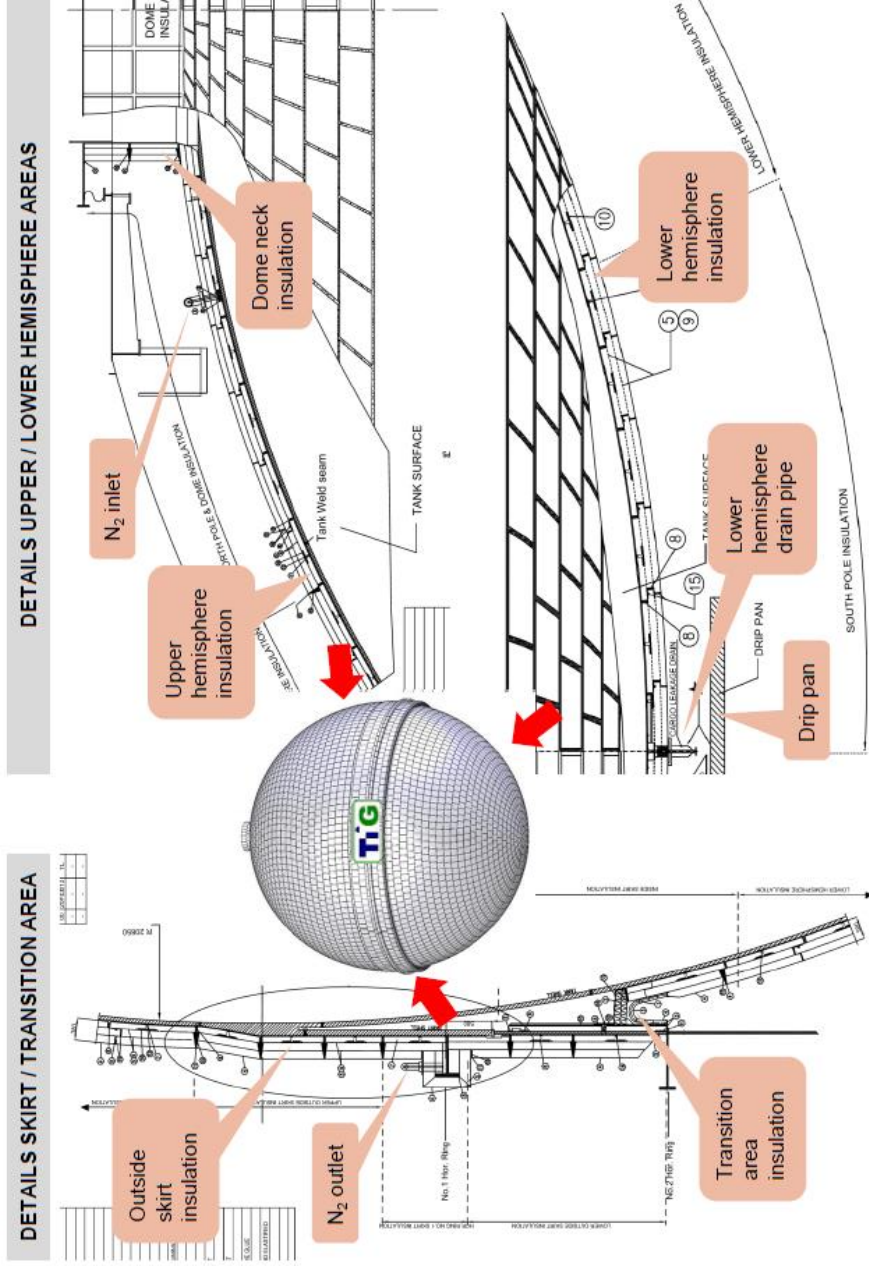
TIG SYSTEM PROVEN FIXATION METHOD TO AVOID FATIGUE PROBLEMS



INSULATION SYSTEM (CONT')



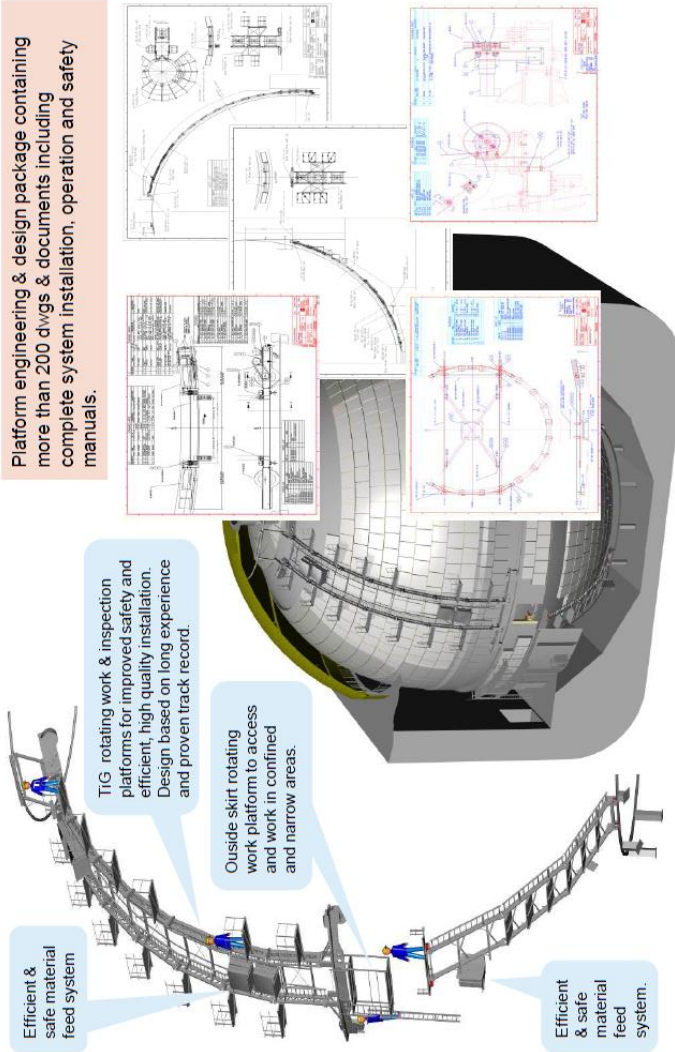
TiG INSULATION SYSTEM – A COMPLETE INSULATION SOLUTION FOR MOSS DESIGN



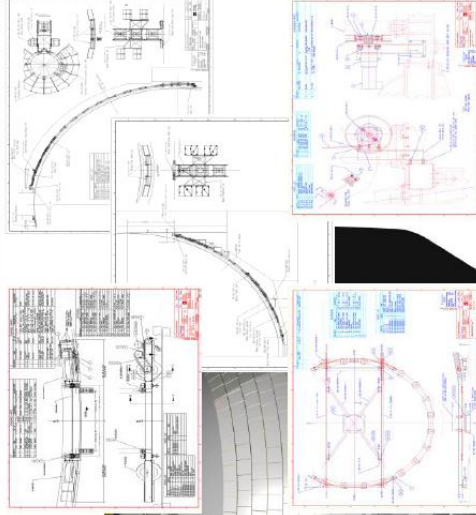
INSULATION INSTALLATION



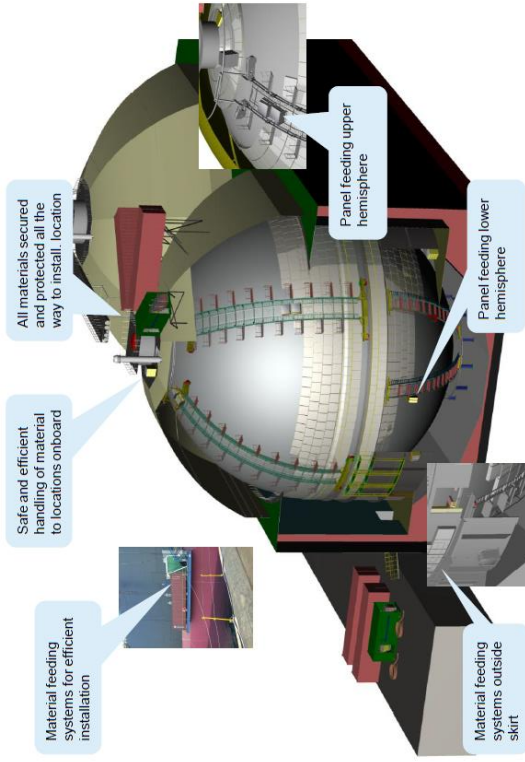
ROTATING WORK & INSPECTION PLATFORMS INCLUDING MATERIAL FEEDING SYSTEM, TAILOR MADE TO DELIVER HIGH QUALITY WORK SAFELY AND EFFICIENTLY IN CONFINED SPACES.



Platform engineering & design package containing more than 200 dwgs & documents including complete system installation, operation and safety manuals.



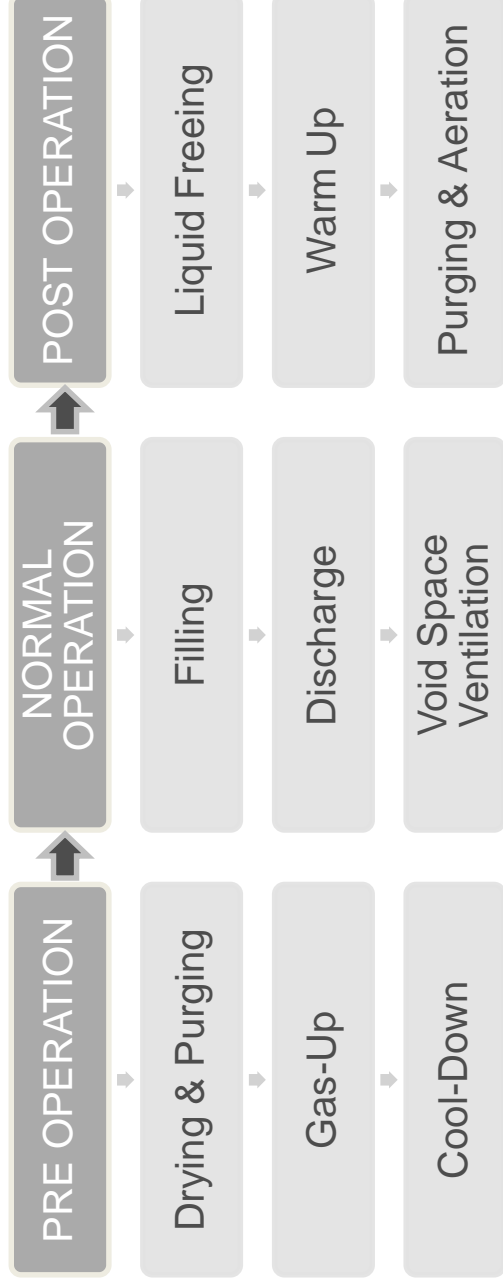
COMPLETE MATERIAL FEEDING / HANDLING SOLUTIONS FROM SHORE STORAGE TO VESSEL AS WELL AS ONBOARD LOGISTICS





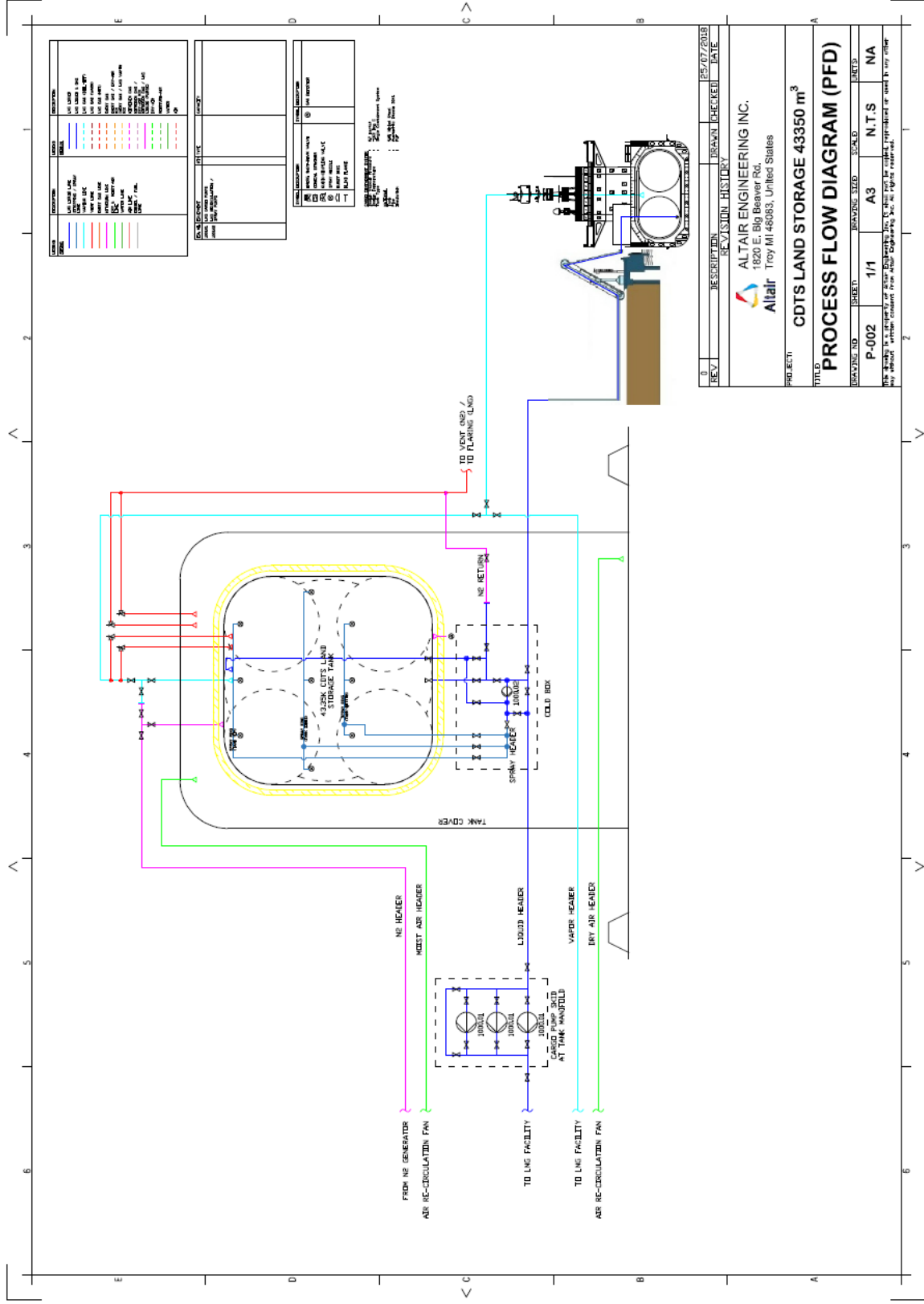
PROCESS FOR LAND STORAGE

SEQUENCE OF OPERATION





PROCESS FLOW DIAGRAM



| REV | DESCRIPTION | DRAWN | CHECKED | DATE |
|-----|-------------|-------|---------|------------|
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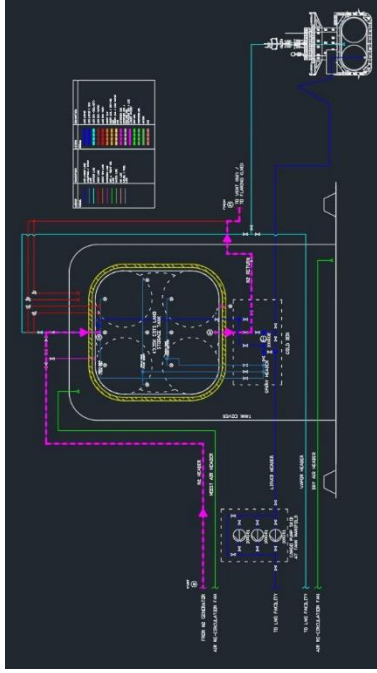
ALTair ENGINEERING INC.
 1820 E. Big Beaver Rd.
 Altair Troy MI 48063, United States

PROJECT: CDTs LAND STORAGE 43350 m³
 TITLE: PROCESS FLOW DIAGRAM (PFD)
 DRAWING NO: P-002
 SHEET: 1/1
 SCALE: A3
 N.T.S.
 NA

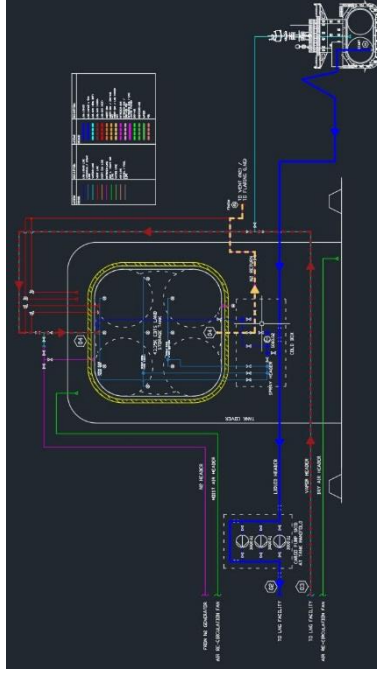
NOTES:
 1. THIS DRAWING IS THE PROPERTY OF ALTair ENGINEERING INC. IT SHALL NOT BE COPIED, REPRODUCED OR USED IN ANY OTHER MANNER WITHOUT THE WRITTEN CONSENT FROM ALTair ENGINEERING INC. ALL RIGHTS RESERVED.

PROCESS FLOW DIAGRAM (CONT')

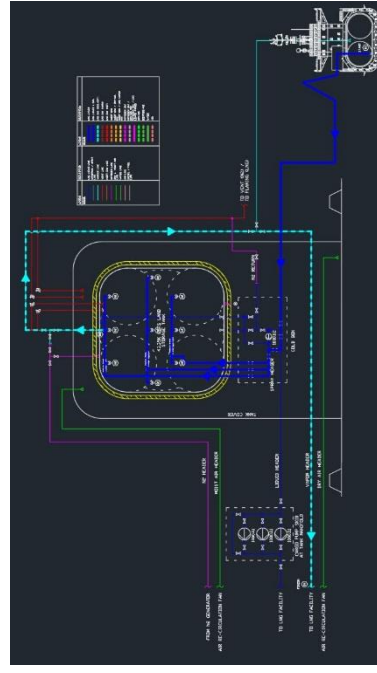
- 01 - N2 Purging



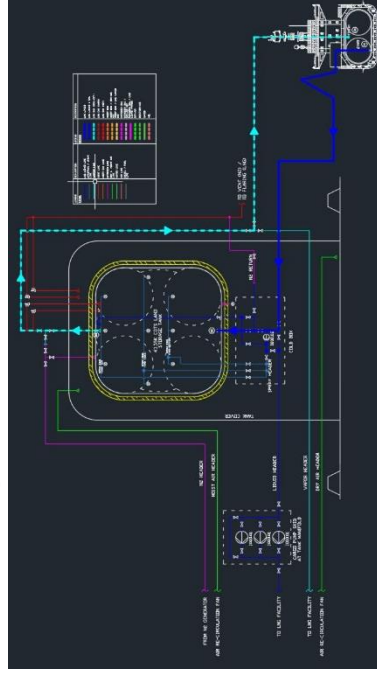
- 02 - Gas Up



- 03 - Cool Down

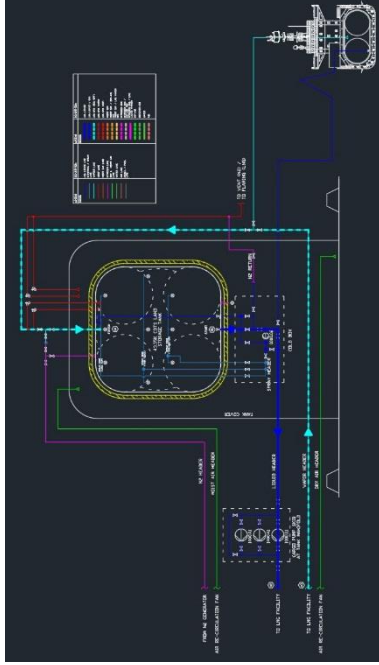


- 04 - Filling

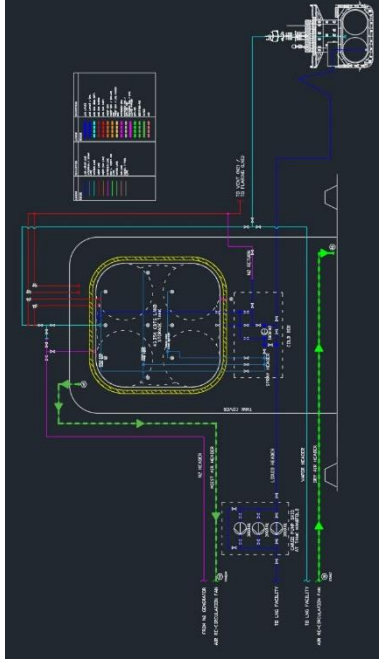


PROCESS FLOW DIAGRAM (CONT')

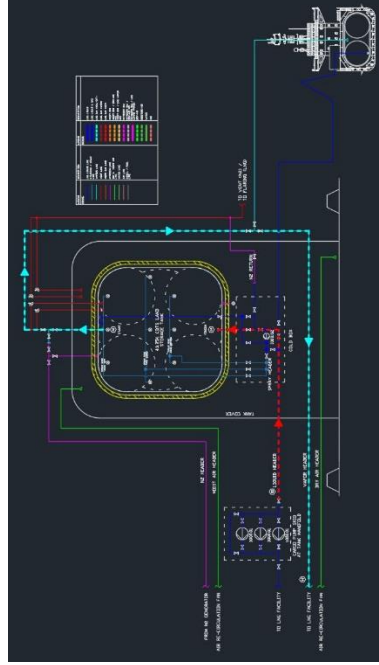
- **05 - Discharge**



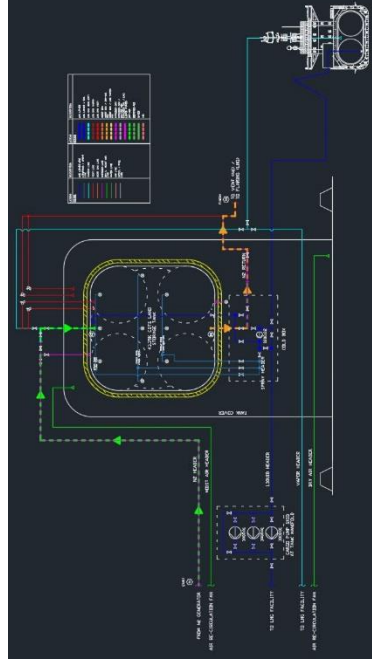
- **06 – Void Space Ventilation**



- **07 – Warm Up**



- **08 – Purging / Aeration**





Appendix C.

Multi-Effect Distillation Desalination

Refineries, power plants and other industries need high purity water. The thermal desalination process uses energy to evaporate water and subsequently condense it again. Waste heat powering thermal desalination is a most efficient and viable solution.

Low Temperature [70° C.] -- Multi-Effect Distillation is a low-pressure steam process. The LT-MED approach achieves exceptional thermal efficiency and reliability – a multi-effect process in which a spray of seawater is repeatedly evaporated and then condensed, with each effect at a lower temperature and pressure. This process multiplies the quantity of pure water that can be produced using a given quantity of energy, resulting in a significant cost reduction.

PROPERLY DESIGNED LT-MED's KEY BENEFITS

- Safe and reliable continuous operation
- Lower operation and maintenance costs
- Eco-friendly solutions to minimize impact on the environment
- Fast installation time
- Low temperature process minimizes desalination costs
- Large pitch design delivers reliable, non-clogging wetting operations
- An on-line ion trap prevents heavy metal ions from entering the plant
- Use large wetting areas in heat transfer tubes to prevent scaling and fouling
- Use rubber grommets to seal heat transfer tubes with electrical insulation to protect against galvanic corrosion
- Use non-erosive titanium condenser components to extend lifecycle

Process of Multiple Effect Distillation plant:

The steam enters the plant and is used to evaporate heated seawater. The secondary vapour produced is used to generate tertiary steam at a lower pressure.

The primary steam condensate is returned to the boiler of the power station since it is of extremely high quality that is needed for turbine steam production.

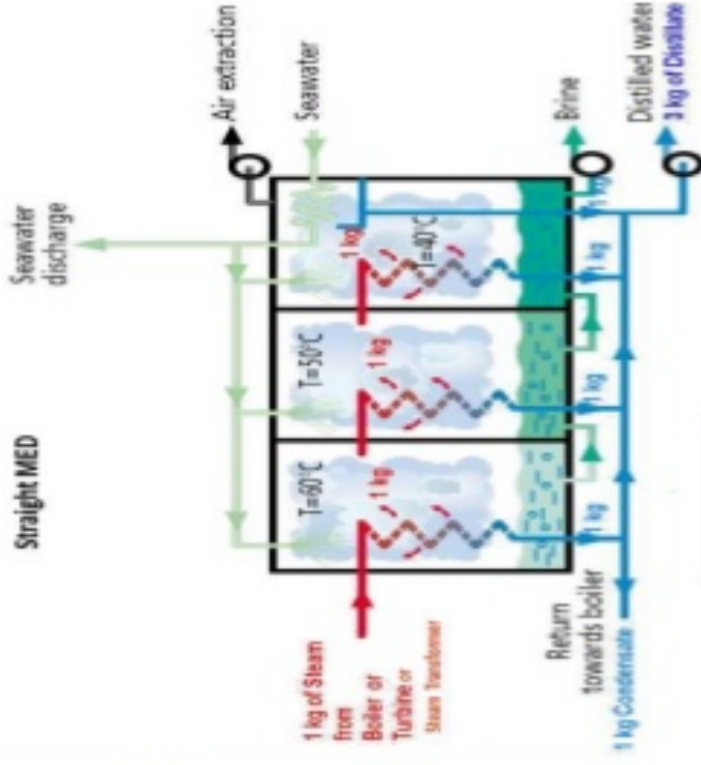
The MED technique is based on double-film heat transfer. Latent steam heat is transferred at each stage by steam condensation through the heat transfer surfaces to the evaporated falling film of seawater.

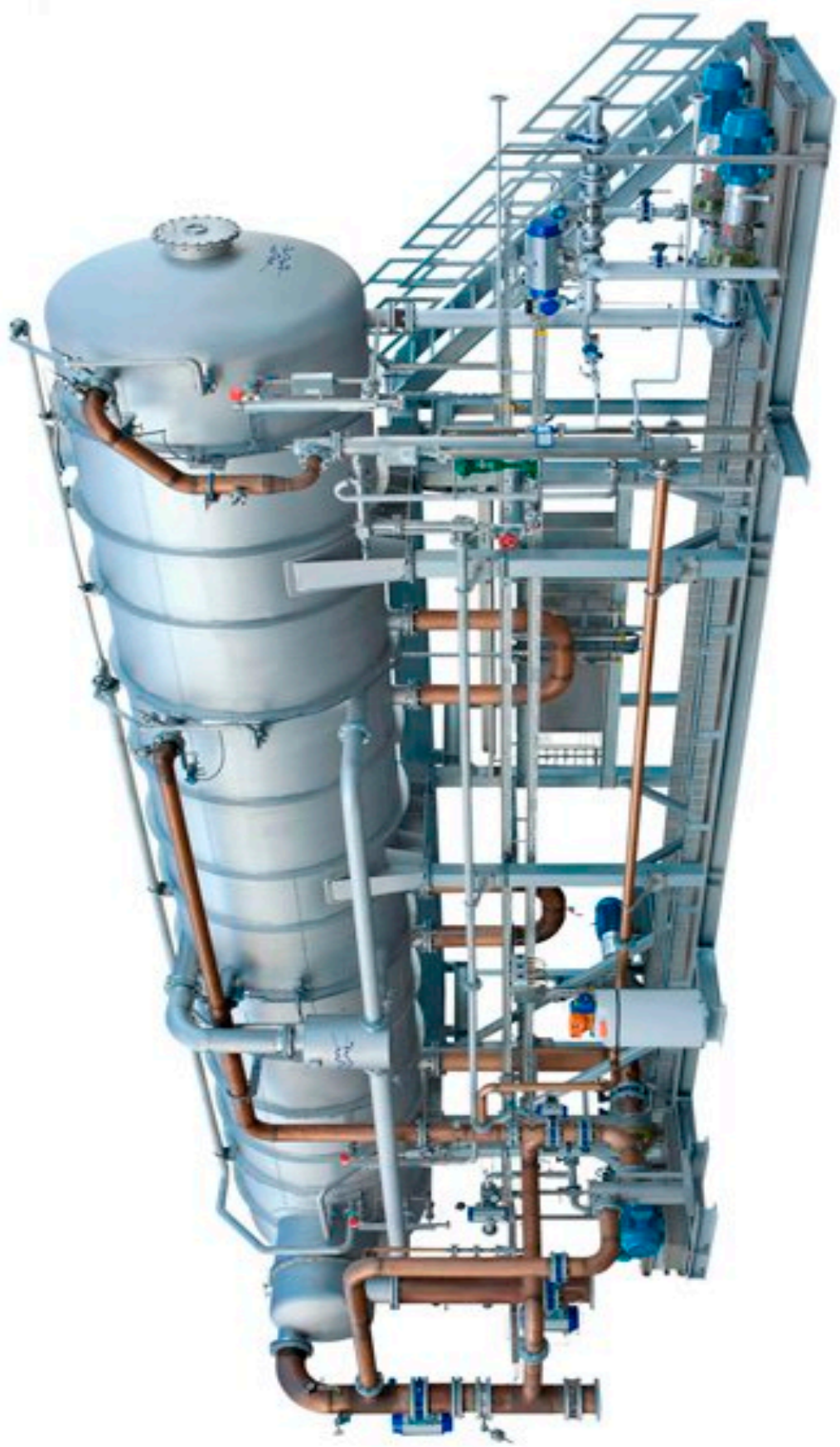
The process is repeated up to 16 times in existing plants between the upper possible temperature and the lower possible cooling water.

A compressor is used to maintain the gradual pressure gradient inside the vessel by removing the accumulated non-condensable gases together with the remaining water vapour.

The pressure gradient along the MED effects is dictated by the saturation pressure of the feed steam and the saturation pressure of the condensing steam exiting the last stage.

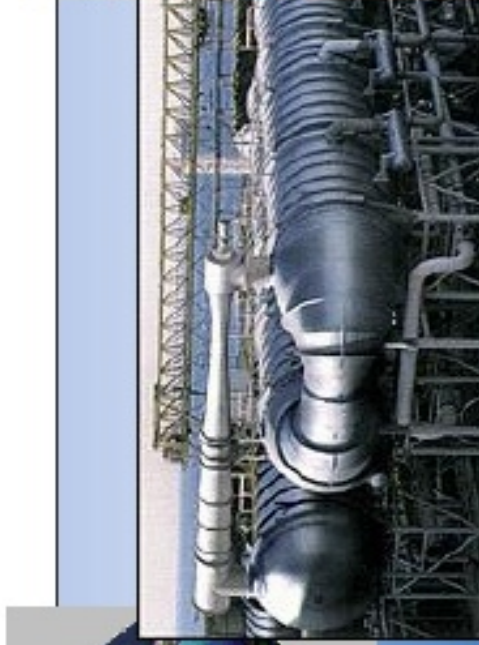
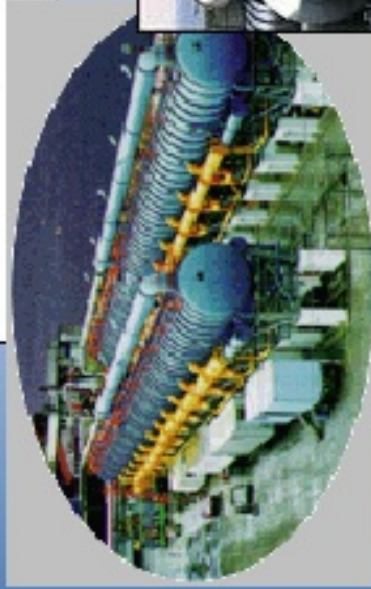
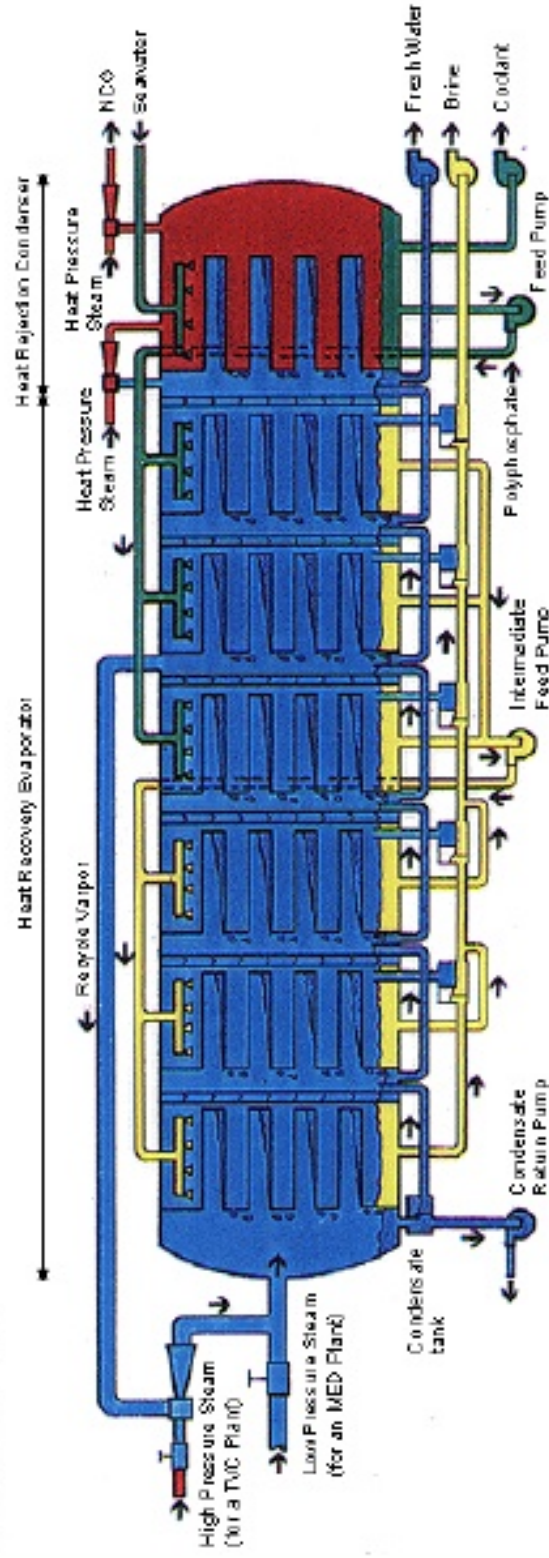
It is condensed by cooling with seawater. Typical pressure gradients of 5-50 kPa across the system (less than 5 kPa/stage) are typical.





Multi Effect Distillation - Horizontal Tubes - IDE Design

MED and TVC process schematic





Appendix D.

Cost Plus Basis

| at 321 MW CCGT plant plus RLNG & LT-MED facilities | | |
|--|------------|----------------|
| CAPEX | | \$US |
| 321 MW CCGT with flow acceleration & RLNG; LT-MED | | 477,608,908 |
| Total power (MWh) delivered at 80% efficiency | | |
| (386 MWh at 80% eff) | 2,705,088 | |
| Gas consumption (NG MSCF.y) | 14,406,346 | |
| Effective NG cost \$ per MSCF | 8.17 | 117,667,426 |
| OPEX | | |
| Cost of NG consumed \$ per kWh | 0.0435 | 117,667,426 |
| Effective cost of LT-MED desalination system \$ per kWh | 0.0819 | 747,338 |
| O&M (\$2.25 per MWh) | 2.25 | 6,086,448 |
| Mgt & Engineering (\$2.50 per MWh) | 2.50 | 6,762,720 |
| Other OH (insurance, administration,...) per MW | 0.50 | 1,352,544 |
| Distribution fees (\$1.00 per MWh) | 1.00 | 2,705,088 |
| Total OPEX per kWh | 0.0500 | 135,321,564 |
| Amortization (5%, 10 yrs) loan & cost per kWh | 0.0140 | 37,972,093 |
| Effective cost of power production per kWh | 0.0641 | 173,293,657 |
| Developers Margin per kWh | 0.0200 | 54,101,760 |
| All in service cost per kWh | \$ 0.0841 | \$ 227,395,417 |
| Proposed tariff | \$ 0.1000 | \$ 270,508,800 |
| Margin | \$ 0.0159 | \$ 43,113,383 |
| | 19% | 19% |
| An array of three 60MW aeroderivatives fed into one steam turbine | | |
| that generates 321.9MW plus 20% more with Flow Acceleration Heat Exchanger | | |
| equaling 386MW for the price of 321MW of fuel | | |